EVALUATION OF A NEW SUSTAINABLE CONTINUOUS SYSTEM FOR PROCESSING BOVINE LEATHER

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Abstract

The aim of the present work is to evaluate a new sustainable continuous system for processing bovine leather. By means of a prototype described in the international patent WO 2010/070571 (A2) of the technological centre AIICA, a dehydration process for bovine hides is carried out. What is obtained through this new process is a dehydrated leather with the optimal physical and chemical characteristics that will allow its subsequent tanning by immersion processes in aqueous solutions of chemical products. When compared to existing traditional processes, there are economic and environmental advantages resulting from the use of this new system. More specifically, the new process results in reductions of 30.6% in water use, 50.2% in chemical use and 16.4% in process time. In addition, a reduction of 27.3% in wastewater and a reduction of 47.5% of thermal energy consumption are obtained. However, this new system presents an increase in electricity consumption of 63.03% and an increase in gaseous emissions of 75% due to the use of acetone in the dehydration process and the 0.5% losses of acetone during the process.

In order to better assess the environmental impact of this new tanning system, life cycle analysis methodology has been chosen to perform calculations on the global warming potential (CO2 equivalent emissions) and the energy consumption comparing both traditional and new tanning processes.

Keywords

Dehydration; leather; tannage; global warming potential

1. Introduction

The chrome tanning method is the most widely used and represents the 90% of world production, thanks to its ease of use and good properties given to the skin: durability, hydrothermal resistance, touch, fullness, etc. However, the use of chromium is a controversial issue because of its toxicity and persistence in the environment that represent some of its chemical forms.
A great variety of projects have been carried out in order to minimize this impact: recycling of pickle-tanning floats (Morera et al., 2011), recovery and treatment of chrome floats (Kanagaraj et al., 2008), high exhaustion of such floats (Bacardit et al., 2008; Thanikaivelan et al., 2004; Legesse et al., 2002), management of solid waste containing chrome (Hu et al., 2011), and the use of other tanning agents to substitute chrome (Ollé et al., 2001; Saravanan, 2003; Taylor et al., 2011).

The present work is based on the knowledge acquired in two previous studies (AIICA, 2010; Ollé et al., 2013a; Ollé et al., 2013b). In these mentioned studies, a prototype to obtain a new collagenic material by dehydration was developed and the best process for obtaining dehydrated bovine hides was studied. Once the optimum process was established, a dehydration system for bovine hide at industrial stage was designed, which allows for a dry and very porous substrate to be obtained, which facilitates the application of tanning agents, dyes and fats by immersion in aqueous solutions.

Indeed, dehydration technologies based on the use of solvents have been developed since the beginning of the twentieth century. However, a proper system for the recovery of the solvent used is yet to be determined. Also, further research is needed to determine whether the dehydrated hide is in the optimum condition to be subsequently stabilized and transformed into finished leather (Teliba et al., 1993; Chagne et al., 1993, Silvestre et al., 1994).

In the present work, a process of tanning by immersion of dehydrated bovine leathers with the aim of minimizing the negative effect of the tanning pollution was studied. Specifically, the processing of 1000 kg of raw salted hide generates approximately 22 m$^3$ of residual effluent with high concentrations of pollutants, plus approximately 730 kg of solid waste and 40 kg of emissions. Another parameter to take into consideration is the low efficiency of the chemical processes which take place during the process of tanning. An excess of tanning products is needed in order to stabilize 1000 kg of raw hide, that is, approximately 60 kg of chrome salts or more than 450 kg of vegetable extracts (European IPPC Bureau, 2009; International Union Environment of IULTCS, 2008).

It is expected through the design of the new continuous system to obtain a reduction of the process time, a reduction of the chemicals used and a reduction of the water consumption compared to those of the conventional process.

2. Material and methods
2.1. Material
The tests were carried out using hides split at 2.5 mm. In order to finish the preparation before dehydration, the hides were delimed using 1.5% of a commercially available carboxylic acid and were bated using 0.7% of enzymes of 1000 LVU/g. The pH of the hides is 8.5; the hides are negatively charged since the ionised groups of collagen in this pH are carboxyl groups. In order to reach the isoelectric point of the hide, a neutralisation has to be carried out using 0.5% of formic acid, correcting the pH with NaHCO₃ if it goes below 5.0. The pH obtained is 5-5.5, which is the point at which the ionisation of the pelt is the lowest. In this condition, the water present in the hide is less likely to create hydrogen bonds and it is then easier to move the water towards the external medium of solution.

2.2. Dehydration process
The prototype consists of a wash drum, two collection tanks for the final floats, a tank to recover the condensed solvent and a tank for feeding solvent. As for the recovery of acetone in the final floats, a distiller is coupled to a cooling tower, which also collects the recovered gas emissions. The prototype is made of stainless steel and is appropriately equipped with pumps and valves for the processing of solvents. Fig. 1 shows the prototype as seen from different perspectives. And Fig. 2 shows a picture of the prototype.

Next is a brief description of the units in prototype (1):

- Stainless steel machine (2) with wash drum (2a) with variable rotation speed, of 360 L capacity,
Pneumatic valves, full automation of wash process times and subsequent spin cycles to replace the sammying operation. The final floats are collected by the different tanks of the device depending on the concentration of acetone.

- Distillation column (3) to separate the solvent from the rest of the float (fat + water + leather fibres + dissolved salts)

- Condensation unit (6) with a cooling system

- Tank to collect the final floats (4) comprised of different compartments: (4a) tank to collect the solvent condensed during the process of acetone distillation; (4b) collection of centrifugation float and sammying float; (4c) collection of the last wash float with solvent to recirculate it through a first float application; (4d) feed tank

- Heating units (7) and (9)
- Circulation nozzle (5) of final wash float with acetone
- Nozzle (5a) to circulate the final recovery wash float into the system
- Drum solvent feed nozzle (8)
- Nozzle (10) to circulate solvent vapours into the condensation unit

The working parameters for bovine hides into the prototype are described in Table 1. The drying parameters can be seen in Table 2.

2.3. Tanning and post-tanning by immersion of dehydrated hides

In this stage, a tanning and post-tanning processes on dehydrated pelts were carried out by means of a roller machine at industrial scale as it can be seen in Fig. 3.

A solution of 10% of chromium salt with a basicity of 45ºSch is prepared. The solution is deposited in the immersion compartment of the roller machine. The speed of the rollers is 4.4 m/mm and the speed of the conveyor is 3.3 m/mm. The process time of tanning by immersion is 13 seconds. In order to obtain a good tannage, two applications were performed.

After tannage, a solution is prepared with 10% of synthetic retanning product, 2% of dyestuff, 3% of soya lecithin, 2% of sulfonated beef tallow and 4% of oxisulfated marine oil. The solution is deposited in the immersion compartment of the roller machine. The speed of the rollers is 4.4 m/mm and the speed of the conveyor is 3.3 m/mm. The process time of post-tanning by immersion is 13 seconds. In order to obtain a good post-tannage, two applications are performed.

Once the tannage and post-tannage by immersion is finished, the hides are dried for 12-14 hours.

2.4. Characterization of the leathers obtained

The following tests were carried out on the leather batch that has been dehydrated, tanned and post-tanned through immersion and finished:
2.5. Analysis of the environmental impact

In order to carry out a study of the feasibility of the new system, a basic material and energy balance calculation was performed. More specifically, water supply, chemical products consumption, electricity and thermal energy consumption, solid wastes and wastewater obtained, as well as gaseous emissions were compared.

Apart from the basic material and energy balance calculation, life cycle analysis (LCA) methodology has been chosen to perform a more reliable and quantifiable environmental comparison between both traditional and new tanning processes. In order to achieve this goal, calculations on the global warming potential (GWP) and the energy consumption comparing both production systems are presented in this work.

LCA is a recognized tool to make decisions, since it allows evaluating the environmental impact of a particular management system. It also allows comparing its impact with those of other management systems. LCA methodology is regulated by the ISO 14040 and 14044 (ISO-14040, 2006; ISO-14044; 2006) international standards. The GaBi 4 software from PE International (PE International, 2009) has been used to perform this LCA analysis.

In comparison with the basic material and energy balances, LCA approach takes also into consideration the production of the chemicals used as well as the emissions they generate. This wider view of the process, allows a more detailed environmental evaluation, quantitatively measuring the effect of the chemicals and energy used.
3. Results and discussion

3.1. Characterization of the leathers obtained

The aim at this stage is to assess whether the leathers processed with this new system present better properties than the traditional ones. Table 3 shows the physical and chemical tests carried out on the tanned leathers.

As can be seen in Table 3, leathers tanned with the new system gave similar results like those for the traditional one. Dehydrated leathers showed slightly lower values in shrinkage temperature but present high values in tensile strength (IUP 6) and in tear load (IUP 8). This is due to the fact that the dehydration process confers to the hide a rubbery state.

3.2. Analysis of the environmental impact

The aim of the second part of this study is to assess whether the dehydrated hides at industrial level and tanned and post-tanned by immersion presents an environmental advantage versus the traditional one, that is if using this new system a reduction of process water, chemicals and process time can be obtained.

The subsequent figures present the basic material and energy balance calculation, i.e. in water (Fig. 5), chemical use (Fig. 6), process time (Fig. 7), electricity consumption (Fig. 8) and thermal energy (Fig. 9).

As can be seen in the process flow chart (Fig. 4), the dehydration process consists in removing water content from the neutralised leather in order to obtain a dry and porous collagen substrate. It is through this process that products by immersion can be applied. These new immersion processes allow the chemical products to readily diffuse in such a manner that the subsequent processes will be shorter when compared to the traditional process, also requiring less chemicals and amount of water (see Fig. 5, 6 and 7).

Fig. 5 shows that the main reduction in water use is obtained during the pickling, tannage and post-tannage processes as these are not required in the new system. A total reduction in water consumption of 30.6% is obtained.

Fig. 6 shows that the main reductions in chemical use are obtained once again during the processes of pickling, tannage and post-tannage according to the new proposed system. Chemical use is reduced by
50.2%.

Fig. 7 shows that the main reduction in process time is once again obtained during the processes of pickling, tannage and post-tannage. Process time is reduced by 16.4%.

Fig. 8 shows the comparison in electricity consumption. Electricity consumption is increased by 63.03%. As can be seen, the main disadvantage of the new system is the high electrical energy consumption in the dehydration; this is due to the 5% of losses in acetone. This is a parameter that has to be improved in further investigations.

Fig. 9 shows thermal energy consumption in the new system, more specifically, a reduction by 47.5% is produced. This improvement in thermal energy consumption is due to the tannage and post-tannage by immersion in which the drying is shorter.

In addition, a balance in wastes was performed, i.e. in solid wastes, in wastewater, and gaseous emissions.

There is no significant reduction in production of solid waste. However, it must be taken into account that the production of dehydrated waste from shavings and trimmings of dehydrated leather is different from that of the conventional process since it doesn’t contain any chrome and can be reused as collagen.

The production of waste water is reduced by 27.8%. Although with the new system an increase of 75% in gaseous emissions is obtained. The cause of this increase is due to the use of acetone and its 0.5% loss during dehydration.

3.3. Analysis of the environmental impact according to Life Cycle Analysis methodology

Based on LCA methodology, GWP and energy consumption are calculated in this work to environmentally compare the traditional and proposed tanning systems.

Comparative results for GWP and energy consumption are shown in Figure 10, showing a clear preference for the proposed system for GWP whereas better results for the traditional system for energy consumption.

Reduction of GWP was expected according to the material and energy balances presented. However, higher energy consumption in the new system has not been presented in the basic energy balance, where conversely, a reduction in the new process energy consumption has been detected. The acetone
production is the cause of this GWP results, being acetone the major contributor to energy consumption in the new tanning process. Thus, a sensitivity analysis on this particular chemical is needed to assess its effect to the results.

Fig. 11 shows the contribution of acetone to GWP and also to energy consumption of the proposed system. Acetone production is clearly the responsible for the high energy consumption in the new tanning process.

According to these results, a reduction in the use of acetone during the process will affect positively on the results. In the current results, a 5% loss for each of the 5 baths with acetones is considered. If the 5% acetone losses of the prototype used could be reduced to a 2%, the energy consumption of the new process would be slightly lower than the one of the traditional process. At the same time, this reduction would make the GWP even lower; lowering the CO$_2$ equivalent emissions from the initial 27% reduction to a 57% reduction (see Fig. 12). This proposal should be achieved by the improvement of the prototype, mainly its sealing and the inlet and outlet circuits.

4. Conclusions

The dehydrated hides can be transformed into stabilised leather by immersing the hides in an aqueous solution of chemical products after a short period of application. The quality and the properties of the leathers manufactured with the new system are similar to those obtained with the traditional one.

When assessing the environmental impact of the new system, consumption of chemical products, water and process time with the new system in respect to the conventional process, there are reductions of 30.6% in water use, 50.2% in chemical use and 16.4% in process time. In addition, a reduction of 27.3% in wastewater and a reduction of 47.5% of thermal energy consumption are obtained. However, this new system presents an increase in electricity consumption of 63.03% and an increase in gaseous emissions of 75% due to the use of acetone in the dehydration process and the 0.5% losses of acetone during the process. Based on these results, the proposals of improvements in the prototype have been presented to reduce the losses of acetone during the process.

LCA-based environmental evaluation show better results for GWP in the new proposed system compared to traditional tanning process. However, energy consumption is higher in the new tanning process due to the acetone losses detected in the prototype used in the tanning tests. A reduction in the acetone losses would lower the energy consumption impact from the new system to the level of the traditional system. A further reduction in the acetone losses would clearly make the proposed tanning process energetically preferable to the traditional system.
5. Acknowledgments

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6. References


International Union Environment of the IULTCS, 2008. IUE 6: Pollution values from tannery processes under conditions of good practice.


PE INTERNATIONAL. GaBi Software. Leinfelden-Echterdingen: Institut für kunststoffprüfung und Kunststoffkunde; 2009.


WO 2010/070571 A2 –Procedure of the tanning of skins, material obtained during said procedure and device–.
Figure 4
Figure 5

<table>
<thead>
<tr>
<th>Process</th>
<th>Conventional Process (m³ of water/kg of raw hide)</th>
<th>New Process (m³ of water/1000 kg of raw hide)</th>
</tr>
</thead>
<tbody>
<tr>
<td>Soaking, liming</td>
<td>17</td>
<td>0</td>
</tr>
<tr>
<td>Deliming</td>
<td>17</td>
<td>0</td>
</tr>
<tr>
<td>Neutralization-Dehydration</td>
<td>3.5</td>
<td>0</td>
</tr>
<tr>
<td>Pickel</td>
<td>0</td>
<td>0.8</td>
</tr>
<tr>
<td>Tannage</td>
<td>1</td>
<td>0.4</td>
</tr>
<tr>
<td>Retannage-Dyeing</td>
<td>0</td>
<td>0.05</td>
</tr>
<tr>
<td>Finish</td>
<td>0</td>
<td>0.05</td>
</tr>
</tbody>
</table>

Legend:
- Blue: Conventional Process
- Red: New Process
Figure 8

- Conventional Process (kWh/t of raw hide)
- Dehydration Process (kWh/t of raw hide)
Figure 9

- Conventional Process (kWh/t of raw hide)
- Dehydration Process (kWh/t of raw hide)

<table>
<thead>
<tr>
<th>Process Type</th>
<th>Conventional Process</th>
<th>Dehydration Process</th>
</tr>
</thead>
<tbody>
<tr>
<td>Chemical processes</td>
<td>816</td>
<td>163.2</td>
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<tr>
<td>Mechanical processes and drying</td>
<td>675.2</td>
<td>405.12</td>
</tr>
<tr>
<td>Finishing</td>
<td>280</td>
<td>280</td>
</tr>
</tbody>
</table>
Figure 10
Figure 11
Figure 12

The bar chart compares the Global Warming Potential (GWP, CO2 equivalent) and energy consumption for New and Traditional methods. The GWP values are 44% for New and 99% for Traditional. The energy consumption values are both 100%.
<table>
<thead>
<tr>
<th>Float</th>
<th>Acetone (%)</th>
<th>Time (min)</th>
<th>Speed (rpm)</th>
</tr>
</thead>
<tbody>
<tr>
<td>1</td>
<td>200</td>
<td>60</td>
<td>15</td>
</tr>
<tr>
<td></td>
<td>5</td>
<td>200</td>
<td></td>
</tr>
<tr>
<td>2</td>
<td>200</td>
<td>60</td>
<td>15</td>
</tr>
<tr>
<td></td>
<td>5</td>
<td>200</td>
<td></td>
</tr>
<tr>
<td>3</td>
<td>200</td>
<td>60</td>
<td>15</td>
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<tr>
<td></td>
<td>5</td>
<td>200</td>
<td></td>
</tr>
<tr>
<td>4</td>
<td>200</td>
<td>60</td>
<td>15</td>
</tr>
<tr>
<td></td>
<td>5</td>
<td>600</td>
<td></td>
</tr>
</tbody>
</table>

Table 1. Working parameters for bovine hides
<table>
<thead>
<tr>
<th>Parameter</th>
<th>Conditions</th>
</tr>
</thead>
<tbody>
<tr>
<td>Temperature</td>
<td>25ºC</td>
</tr>
<tr>
<td>Drying time</td>
<td>60 min</td>
</tr>
<tr>
<td>Rotation speed</td>
<td>25 rpm</td>
</tr>
<tr>
<td>Pressure</td>
<td>Atmospheric</td>
</tr>
</tbody>
</table>

Table 2. Drying parameters for bovine hides
### Table 3

<table>
<thead>
<tr>
<th>Test</th>
<th>New System</th>
<th>Traditional System</th>
</tr>
</thead>
<tbody>
<tr>
<td>Tensile strength (N)</td>
<td>200.9</td>
<td>146.5</td>
</tr>
<tr>
<td>Tear load (N/mm)</td>
<td>71.6</td>
<td>34.3</td>
</tr>
<tr>
<td>Distension of grain (mm)</td>
<td>10.8</td>
<td>11.2</td>
</tr>
<tr>
<td>Strength of grain (kg)</td>
<td>25.2</td>
<td>23.2</td>
</tr>
<tr>
<td>Shrinkage temperature (°C)</td>
<td>93</td>
<td>108</td>
</tr>
<tr>
<td>Flex resistance (#cycles)</td>
<td>100000</td>
<td>100000</td>
</tr>
<tr>
<td>Dry rub fastness (100 cycles)</td>
<td>3-4</td>
<td>3-4</td>
</tr>
<tr>
<td>Wet rub fastness (25 cycles)</td>
<td>3-4</td>
<td>3-4</td>
</tr>
<tr>
<td>Dry adhesion (N/cm)</td>
<td>23.5</td>
<td>23.9</td>
</tr>
<tr>
<td>Determination of matter soluble in dichloromethane (%)</td>
<td>11.6</td>
<td>10.7</td>
</tr>
<tr>
<td>Water soluble organic matter (%)</td>
<td>0.5</td>
<td>0.5</td>
</tr>
<tr>
<td>Water soluble inorganic matter (%)</td>
<td>0.9</td>
<td>1.0</td>
</tr>
<tr>
<td>Chromium oxide content (%)</td>
<td>3.0</td>
<td>3.2</td>
</tr>
<tr>
<td>Determination of pH</td>
<td>3.7</td>
<td>3.5</td>
</tr>
</tbody>
</table>

**Table 3. Physical and Chemical Tests**
List of abbreviations
Click here to download Data File: List of abbreviations.docx
List of captions
Click here to download Data File: List of figure captions.docx
Figure 5 B/W

<table>
<thead>
<tr>
<th>Process</th>
<th>Conventional Process</th>
<th>New Process (m3 of water/1000 kg of raw hide)</th>
</tr>
</thead>
<tbody>
<tr>
<td>Soaking, liming, deliming, dehydration</td>
<td>17</td>
<td>0</td>
</tr>
<tr>
<td>Pickel</td>
<td>17</td>
<td>0.8</td>
</tr>
<tr>
<td>Tannage</td>
<td>3.5</td>
<td>0</td>
</tr>
<tr>
<td>Retannage, dyeing, felting, liquorifying</td>
<td>1 0.8</td>
<td>0.05 0.05</td>
</tr>
<tr>
<td>Finishing</td>
<td>7.4</td>
<td>0.05</td>
</tr>
</tbody>
</table>

(m3 of water/kg of raw hide)
Figure 6 B/W

- Conventional process (kg of chemicals/1000 kg raw hide)
- New process (kg of chemicals/1000 kg raw hide)
Figure 9 B/W

- Chemical processes: 816 kWh/t of raw hide
- Mechanical processes and drying: 675.2, 405.12 kWh/t of raw hide
- Finishing: 280, 280 kWh/t of raw hide

Conventional Process (kWh/t of raw hide)
Dehydration Process (kWh/t of raw hide)
Figure 11 B/W

The bar chart shows the GWP (CO2 equivalent) and energy consumption (MJ) for Acetone and Others. Acetone contributes 18% to GWP and 82% to energy consumption, while Others contribute 96% to GWP and 4% to energy consumption.