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1 **Microencapsulation of blackberry pulp with arrowroot starch and**
2 **gum arabic mixture by spray drying**

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29 **Microencapsulation of blackberry pulp with arrowroot starch and** 30 **gum arabic mixture by spray drying**

31 Abstract: This research work aimed to obtain blackberry pulp powder by spray
32 drying and, by an experimental design, evaluated the effect of inlet air
33 temperature (100–150°C) and blackberry pulp solids:arrowroot starch/gum
34 Arabic solids ratio of 1:0.5–1:2 on the physicochemical properties of the
35 powders. Arrowroot starch and gum Arabic present T_g values above 100°C;
36 hence it was possible to employ them as carriers in blackberry pulp spray drying
37 in order to increase T_g of the system. Powder yield and solubility increased with
38 increasing blackberry pulp solids:arrowroot starch/gum Arabic solids ratio of
39 1:0.5-1:2, whereas hygroscopicity decreased. Yield, solubility and hygroscopicity
40 of the powders increased and water activity decreased, with increasing inlet air
41 temperature. The powders presented low moisture content and water activity.
42 Temperature of 143°C and blackberry pulp solids:arrowroot starch/gum Arabic
43 solids ratio of 1:1.78 were the optimal conditions to obtain high yield and
44 blackberry powders that are soluble in water and less hygroscopic.

45 Keywords: glass transition temperature; process yield; moisture content; average
46 size; hygroscopicity; solubility.

47 **Introduction**

48 *Rubus fruticosus* or blackberry, belonging to the Rosaceae family, grows abundantly in
49 regions of cold weather, in the north of Europe, Australia, part of Asia, North America
50 and South America (Ferrari et al., 2012; Gomar et al., 2014).

51 The fruits are highly appreciated by consumers, not only for the combination of
52 their appealing color and desirable flavor and taste, but also for their high nutritional
53 value (D'Agostino et al., 2015). In addition to high contents of fibers, vitamins, and
54 essential minerals, blackberry is an important source of phenolic compounds, such as
55 phenolic acids, tannins and anthocyanins, which have high antioxidant capacity (Elisia
56 et al., 2007; Hager et al., 2008; Machado et al., 2015). Its consumption has been
57 associated with benefits for human physical and mental health (antioxidant, anticancer,

58 anti-inflammatory and anti-neurodegenerative activities) (Dai et al., 2007; Tavares et
59 al., 2012; Zia-Ul-Haq et al., 2014).

60 However, blackberry is one of the most perishable berries because of its thin and
61 fragile skin and high respiration and transpiration rates, which limit its consumption in
62 the fresh form (Ferrari et al., 2012; Joo et al., 2011). During postharvest period, there
63 are fast changes in the blackberry's physicochemical and nutritional properties, such as
64 mass loss, texture alteration and microbiological deterioration. Most blackberries
65 destined for fresh markets became unmarketable after 2 or 3 days when held at 0°C due
66 to decay (Hardenburg et al., 1986; Joo et al., 2011). About 60% of its production is lost
67 if processed improperly (Romero and Yépez, 2015).

68 For this reason, spray drying is an alternative for the processing of blackberry,
69 since the powder obtained is easier to handle, package and transport than the fruit itself,
70 and also provides a high-quality product with prolonged shelf life (Santana et al., 2016).

71 More specifically, spray drying is a technological process in which a fluid
72 product is transformed into a powder by atomizing it into a hot gas stream (Gharsallaoui
73 et al., 2007). The feed flow rate, the inlet and outlet air temperatures, atomizer speed,
74 feed concentration, feed temperature and inlet air flow rate are process parameters of
75 spray drying that influence physicochemical properties of the powders produced (Ré,
76 1998; Chegini and Ghobadian, 2005). Different parameters can be controlled during
77 spray drying process in order to obtain desired characteristics in the final product (Daza
78 et al., 2016).

79 However, some intrinsic drawbacks, such as stickiness, hygroscopicity and low
80 solubility may occur. In addition, the adhesion of droplets to the drying chamber walls
81 decreases the process yield (Santana et al., 2016). The sticky behavior of juices or fruit
82 pulp powders is attributed to the presence of low molecular weight sugars and organic

83 acids in their composition, which have low glass transition temperatures (Bhandari and
84 Datta, 1997; Saavedra-Leos et al., 2012; Araujo-Díaz et al., 2017).

85 Alternatively, high molecular weight encapsulating agents are added to pulps or
86 fruit juices prior to the drying process in order to increase the glass transition
87 temperature of the system and to reduce such problems (Araujo-Díaz et al., 2017). Gum
88 arabic, maltodextrins, starches, gelatin, methyl cellulose, gum tragacanth, alginates,
89 pectin, silicon dioxide, tricalciumphosphate, glycerol monostearate and mixtures of
90 some of them are some examples of encapsulating and coating agents used in spray
91 drying (Igual et al., 2014). Among polysaccharides, starches are being widely studied
92 as potential encapsulating agents due to their low cost, abundance and renewability,
93 besides the advantage of existing in various forms, depending on the source of the raw
94 material (Sartori and Menegalli, 2016), which can generate exceptional functional
95 properties when compared to conventional encapsulating agents. Arrowroot starch has
96 not been used as an encapsulating agent. However it, presents a great potential for
97 application for being multifunctional, non-toxic, biodegradable, blood-compatible,
98 bioactive, besides having a high digestibility (Hoover, 2001; Winarti et al., 2015; Wu
99 and Liao, 2017). Due to its high digestibility, gelling and thickener ability, arrowroot
100 starch (Hoover, 2001; Villas-Boas and Franco, 2016) has been widely used in
101 preparation of bakery products, as in confection of biscuits, cakes, creams and sweets
102 (Leonel et al., 2002).

103 However, arrowroot starch cannot be easily thermal processed, which limits its
104 application in industries. Thus, to increase the functionality of arrowroot starch, it is
105 blended with other polymers to make biocomposites, creating a biomaterial with more
106 functional applications (Wu and Liao, 2017). The mixture of arrowroot starch with gum
107 Arabic has a great potential for use as encapsulating agent, since gum Arabic presents

108 many desirable characteristics of a good wall material for drying encapsulating
109 techniques, such as increasing glass transition temperature, imparting high solubility,
110 low viscosity and good emulsifying properties to feed dispersions (Ramírez et al.,
111 2015).

112 This study aimed to produce powdered pulp from blackberry by spray drying
113 using mixture of gum Arabic and arrowroot starch as encapsulating agent, in order to
114 evaluate the impact of drying conditions on the physical properties of spray-dried pulp.

115

116 **Materials and methods**

117

118 ***Materials***

119 *Blackberry fruits*

120 Frozen fruits of blackberry (*Rubus fruticosus*), cv Tupy, were acquired from "Agro
121 Monte Verde Eirelli", company of Cambuí – MG, Brazil, and used in this research
122 work. Pulp was obtained by grinding blackberry fruits in a blender, previously thawed
123 in refrigerator (8°C) for 24 h. Then, the pulp was sieved to remove seeds, homogenized
124 and packed in polypropylene bottles and coated with aluminium foil to protect against
125 photodegradation. The samples were stored in freezer at $-40 \pm 3^\circ\text{C}$ until drying. Pulp
126 soluble solids content was 9°Brix, determined with a manual refractometer with a 0–
127 90°Brix range and 0.2°Brix resolution (Reichert, Model AR200, USA). The pulp
128 presented total solids content of 10.3 g/100g of pulp.

129

130 *Carrier agent*

131 The encapsulating agents used were gum Arabic Instantgum® (colloids Naturels, São
132 Paulo, Brazil) containing $14.00 \pm 0.10\%$ of moisture content, $1.38 \pm 0.16\%$ of proteins,

133 0.37±0.02% of lipids, 3.70±0.10% of ash and 80.46±0.00% of carbohydrates
134 (A.O.A.C., 2006), and arrowroot starch containing 15.24±0.19% of water, 0.40±0.03%
135 of protein, 0.12±0.01% of fat, 0.33±0.01% of ash and 83.91±0.00% of carbohydrates
136 (A.O.A.C., 2006). The arrowroot starch was extracted according to the methodology
137 developed by Cruz and El Dash (1984). Arrowroot rhizomes used in the extraction of
138 the starch were obtained in the Faculty of Agronomy, Federal University of Grande
139 Dourados, Mato Grosso do Sul, Brazil, in 2014. All other reagents used for the analyses
140 presented analytical grade.

141

142 ***Methods***

143 *Differential Scanning Calorimetry (DSC) of carrier agents*

144 The thermal properties of arrowroot starch and gum Arabic (powder) were studied using
145 a Differential Scanning Calorimeter (DSC1, Mettler Toledo, Schwerzenbach,
146 Switzerland). Aliquots of 10 mg of the samples were weighed in a microanalytical scale
147 (MX5-Mettler Toledo, Schwerzenbach, Switzerland), in an aluminum pan (40 µl). For
148 reference, an empty aluminum pan was used. The samples were submitted to heating
149 program between 25 and 100°C at a rate of 10°C/min, in an inert atmosphere (50
150 mL/min of N₂). When temperature reached 100 °C, samples were held for 10 minutes at
151 this temperature. After this first scan, the measurement cells were cooled with liquid
152 nitrogen to 25°C, followed by a second heating sweep between 25 and 270°C at rate of
153 10°C/min in an inert atmosphere (50 mL/min of N₂). The glass transition temperature
154 (T_g) was calculated as the baseline inflection point, caused by the discontinuity of
155 specific heat of the sample.

156

157 *Experimental Design*

158 Drying experimental runs were conducted following an experimental design using
159 mixture of arrowroot starch/gum Arabic (1:1, weight/weight) as encapsulating agent. A
160 central composite design – including 4 factorial runs, 4 experimental runs in axial
161 conditions and 3 repetitions of central point, totalling 11 runs – was developed (**Table**
162 **1**) to study the effects of dryer inlet air temperature (100–150°C) and blackberry pulp
163 solids:arrowroot starch/gum Arabic solids ratio of 1:0.5–1:2 (weight/weight) on the
164 powder properties. The response variables considered were drying process yield,
165 moisture content, water activity, hygroscopicity, solubility and particle size.

166

167 *Microcapsule production*

168 The solution of encapsulating agents and blackberry pulp was prepared in mixer type
169 homogenizer at room temperature for 5 minutes. The solutions obtained were diluted in
170 water in a ratio of 1:2 (weight/weight) to facilitate spraying, due to its high viscosity.
171 The total solids contents of the spray feed solutions are presented in Table 1 and were
172 determined from the determination of the dry weight obtained by drying in a vacuum
173 oven at 60 °C until obtaining constant weight (A.O.A.C., 2006).

174 The resulting homogenized solutions were immediately fed into laboratory spray
175 dryer (Model B191, Büchi, Flawil, Switzerland) equipped with a drying chamber
176 (diameter of 110 mm and height of 435 mm) and dual fluid atomizer nozzle with an
177 orifice of 0.5 mm in diameter, using the following process conditions: airflow of 19
178 m³/h; pressurized air flow of 0.6 m³/h; feed mass flow of 0.2 kg/h. Three drying
179 repetitions were performed for each test. The resultant powder was stored in
180 polyethylene packages in desiccators until its characterization.

181

182 *Powder characterization*

183

184 *Drying process yield.* Drying process yield was determined by the ratio between
185 powder solids mass and feeding solids mass of blackberry pulp.

186

187 *Moisture content and water activity.* The powder's moisture content was gravimetrically
188 obtained by vacuum oven at 60°C until constant weight, in triplicate (A.O.A.C., 2006).
189 Water activity (A_w) was determined by direct reading at 25°C, using a water activity
190 meter (Aqualab, Decagon Devices, USA). All determinations of A_w were carried out
191 from three independent preparations, in triplicate.

192

193 *Microstructure.* Electronic Scanning Electron Microscope with X-ray Dispersive
194 Energy Detector (SEM) bench (model of MEV: Leo 440i, model of EDS: 6070, Leo
195 440i - LEO Electron Microscopy/Oxford- Cambridge, England) was used to observe the
196 morphological characteristics of the powder samples. Powder sample was placed on
197 double-sided carbon adhesive tape adhered to stub, submitted to application of a gold
198 layer (model K450, Sputter Coater EMITECH, Kent, United Kingdom) and observed in
199 scanning electron microscope operated at 20 kV.

200

201 *Hygroscopicity of blackberry powders.* Hygroscopicity was determined according to
202 methodology proposed by Cai and Corke (2000), with some modifications.
203 Approximately 1 g of each powder sample was placed in a hermetic container at 25°C,
204 with a saturated NaCl solution, to create a 75.7% relative humidity atmosphere. The
205 samples were weighed, in triplicate, after seven days and the hygroscopicity was

206 determined and expressed in g of adsorbed water per 100 g of dry solid (100 g g⁻¹).

207

208 *Solubility of the blackberry powders.* Solubility was determined according to the
209 method described by Eastman and Moore (1984), cited by Cano-Chauca et al. (2005).

210 The method consists in adding 1 g of sample to a vessel containing 100 mL of distilled
211 water, operating with high-speed magnetic stirring – level 4 of magnetic stirrer for 5
212 minutes, followed by centrifugation at 3000 g for 5 minutes. Aliquot of 25 mL of
213 supernatant was removed and kept in the oven at 105°C until constant weight. The
214 solubility was calculated by weight difference.

215

216 *Particle size distribution.* The particle size distribution (d 0.1, d 0.5, d 0.9, µm) was
217 determined by a particle size analyzer based on laser diffraction (Mastersizer 2000,
218 Malvern Instruments, UK). The mean diameter was determined based on the diameter
219 of a sphere with equivalent volume (De Brouckere Mean Diameter, D[4.3]). The surface
220 mean was determined based in volume/surface mean (also called the Sauter mean,
221 D[3.2]). Samples were analyzed in triplicate with dispersion in 99.5% ethanol.

222 *Statistical analysis*

223 The results of variable response of the experimental design were evaluated using
224 Statistica 9.0 software. Significant differences between mean results were
225 evaluated by analysis of variance (ANOVA) and Tukey test at 5% level of
226 significance, using SAS software (Cary, NC, USA).

227

228 **Results and discussion**

229

230 *Differential Scanning Calorimetry (DSC) of the carrier agents*

231 One of the difficulties of spray drying of sugar-rich food products, such as pulps or fruit
232 juices, is the high chemical affinity between water molecules and the low molecular
233 weight sugars contained in the pulp or juice (Araújo-Díaz et al., 2017). As a
234 consequence, the overall glass transition temperature (T_g) of the system decreases,
235 observing processing problems of fruit pulp powders obtained by spray drying, such as
236 stickiness, hygroscopicity and low solubility. In addition, the adhesion of droplets to the
237 drying chamber walls decreases the process yield (Santana et al., 2016).

238 Encapsulating agents may be employed as improver in the spray drying process
239 of pulps or fruit juices, with the main function of increasing T_g of the system, since
240 these agents are characterized by high molecular weight, low viscosity and T_g in the
241 range of 100–188°C (Araújo-Díaz et al., 2017; Saavedra -Leos et al., 2015). The quality
242 of the powder is closely linked with the choice of encapsulating agent. Thus, knowledge
243 of the glass transition temperature behavior of the polymeric materials supports its
244 choice as an encapsulating agent and helps to understand its performance in processes
245 such as dehydration, evaporation, and conservation.

246 Glass transition temperature (T_g) is a value referring to a temperature range that,
247 during the heating of a polymeric material, allows the amorphous chains to acquire
248 mobility (Schlemmer et al., 2010). T_g is an important information obtained from DSC
249 curves. Differential scanning calorimetry (DSC) is a commonly employed analytical
250 technique for analysis and characterization of amorphous solid dispersions. This
251 technique has proven to be a highly versatile technique for understanding the glass
252 transition temperature (T_g), relaxation, and crystallization behavior of polymeric
253 material (Bechgaard et al, 2018). Phase transitions in foods are often a result of changes
254 in composition or temperature during processing or storage. The DSC curves of
255 arrowroot starch and gum arabic are shown in Figure 1. According to Araújo-Díaz et al.
256 (2017), for any substance or compound to be used as an encapsulating agent, it must
257 present a T_g value above boiling temperature of water (approximately 100°C).
258 Considering that carbohydrate polymers, arrowroot starch and gum Arabic present T_g
259 values above 100°C , hence, they can be employed as encapsulating agents in spray
260 drying blackberry pulp.

261 The thermogram of arrowroot starch, with moisture content of 15.24% (dry
262 base), presented in Figure 1A, showed T_g of 118.19°C , with the beginning of this
263 transition at about 116.52°C and the end at about 118.20°C . The endothermic peak
264 around 140°C observed in thermogram (**Figure 1A**) of arrowroot starch was attributed
265 mainly to evaporation of water present in starch.

266 The thermogram of potato starch with moisture content of 3.7% w/w (RH 11%)
267 showed T_g of 161.72°C , while for the same sample with moisture content of 18.8%
268 w/w (RH 75%) T_g of 141.91°C (Chuang et al., 2016). The T_g presented by starch
269 depends heavily on moisture content of amylose and amylopectin, molecular

270 interactions between starch and low molecular weight co-solutes and the inherent
271 characteristics of the used measurement protocol (Perdomo et al., 2009).

272 For gum Arabic with moisture content of 14% (dry base), the thermogram
273 showed Tg of 125.8°C, with the beginning of this transition at around 124.16°C and the
274 end at around 125.97°C (**Figure 1B**). A similar endothermic peak for gum Arabic was
275 reported by Mothé and Rao (2000) at about 90°C. According to the authors, this peak
276 appeared due to the melting of crystallites during heating of gum Arabic with lower
277 moisture content (0–40%).

278

279 Insert Figure 1 here

280

281 *Experimental design*

282 The experimental data for process yield (Y), moisture content (M), water activity (Aw),
283 hygroscopicity (H) and solubility (S) were determined using 11 combinations of the
284 independent variables, as shown in **Table 1**.

285 The results were fitted using a second-order regression model. The codified
286 regression coefficients, F-values, p-values and coefficients of determination (R^2) are
287 presented in **Table 2**. Nonsignificant terms, at confidence level of 95%, were eliminated
288 and the predictive models were tested for adequacy and accuracy of fit by ANOVA.
289 When calculated F-value (F_c) was greater than the tabulated F-value (F_t), the variation
290 was explained by the regression and not by residues. Thus, the regression was
291 significant, and the model could be considered predictive. **Figure 2** shows the response
292 surfaces generated by the proposed models.

293

294 Inserts Table 1 and 2 here

295 Insert Figure 2 here

296

297 ***Process yield***

298 According to **Table 1**, the experimental process yield values for blackberry pulp spray
299 drying using arrowroot starch and gum Arabic mixture as encapsulating agent ranged
300 between 28.77 and 56.95%. These values were similar to those obtained for spray
301 drying of açai of 34.3–55.7% (Tonon et al., 2008), for jussara pulp of 33.88 to 76.55%
302 (Santana et al., 2016), for beetroot juice ranged between 41.31% and 54.63% (Bazaria
303 and Kumar, 2016). Eldridge et al. (2014) demonstrated a recovery of 61.3% of
304 blackberry powder contained at 6.3:1 (w/w) mannitol:blackberry extract.

305 Blackberry is a fruit rich in sugars of low molecular weight such as glucose,
306 fructose and sucrose (Kafkas et al., 2006), which have low T_g value: 32°C, 14.5°C, and
307 45°C, respectively (Saavedra-Leos et al., 2012). The T_g of the pulp was influenced by
308 the present sugars, which makes difficult the drying process. In this work, it was not
309 possible to obtain powdered blackberry pulp without addition of encapsulating agent,
310 because the pulp behaved as syrup, sticking to the walls of dryer and obtaining a caked
311 product instead of a dry powder. Without carrier, pomegranate juice formed a hard glass
312 film on spray dryer chamber walls in dehydration process (Yousefi et al., 2011).

313 With incorporation of encapsulating agent in blackberry pulp before drying
314 process, it was possible to obtain powder, but at smaller ratios of arrowroot starch/gum
315 Arabic solids in relation to the total blackberry pulp solids, a large powder deposit was
316 still observed in the walls of drying chamber and cyclone. This same behavior was
317 reported by Igual et al. (2014) and Santana et al. (2016) during drying of lulo pulp and
318 jussara pulp, respectively. Retention of product on the chamber wall is undesirable

319 (Santana et al., 2016). Process yield corresponds to product recovery and is mainly
320 determined by the powder collection efficiency (Wang and Langrish, 2009).

321 The blackberry pulp drying process yield was significantly ($p < 0.05$) influenced
322 by inlet air temperature of the dryer and blackberry pulp solids:arrowroot starch/gum
323 Arabic solids ratio, which presented quadratic negative effect and positive linear effect,
324 respectively (**Table 2**).

325 The highest yields were obtained when higher blackberry pulp solids:arrowroot
326 starch/gum Arabic solids ratio and inlet air temperature were used, as shown in **Figure**
327 **2A**. The experimental run 8 and the central point runs presented the highest drying
328 process yield values (53.17–56.95%), which were significantly different ($p < 0.05$) from
329 results of other experimental runs. This behavior indicates that addition of encapsulating
330 agent to blackberry pulp before spray drying was sufficient for a possible increase of
331 glass transition temperature of system. Increased blackberry pulp solids:arrowroot
332 starch/gum Arabic solids ratio favored blackberry pulp drying, reducing stickiness of
333 powders encapsulation by encapsulating agents, consequently decreasing adherence of
334 solids in drying chamber, which resulted in increased yield values. One way of
335 confirming this hypothesis of reducing the viscosity of the powders is to determine the
336 t_g of the powders and relate to the temperature of the dryer's outlet air.

337 As for temperature, the increase in dryer's inlet air temperature caused increase
338 in process yield, which could be attributed to the greater efficiency of heat and mass
339 transfer processes (Bazaria and Kumar, 2016). However, at temperatures above 143°C,
340 there was decrease in yield, probably due to the caramelization of encapsulating agents,
341 as well as of sugars present in blackberry pulp (Souza et al., 2015), which resulted in
342 more adhesion to wall, so the amount of powder production and yield was reduced.

343 All the produced powders showed marked reddish color and flavor
344 characteristics of blackberry fruit (**Figure 3**).

345

346 *Moisture content*

347 The results of statistical analysis applied to experimental data of the powders moisture
348 content showed that the effects of linear, quadratic and interaction factors were not
349 significant at 95% confidence interval ($p>0.05$). Due to these nonsignificant factors, it
350 was not possible to construct a predictive mathematical model for behavior of moisture
351 content of blackberry powders in function of independent variables.

352 However, **Table 1** shows that all powders produced presented moisture content
353 values lower than 6%. Ferrari et al. (2012) obtained approximately 3% moisture content
354 for blackberry juice powder produced by spray drying using inlet air temperature of
355 160°C and 5% of maltodextrin as encapsulating agent (w/w). The moisture content of
356 sumac extract powders ranged between 2.94 and 4.22% (wet basis) (Caliskan and
357 Dirim, 2016) and 0.9 to 7% for lulo powders (Igual et al., 2014).

358 For powder products, moisture content had great impact on flowability,
359 stickiness and storage stability because of its plasticizing effects and crystallization
360 behavior (Islam et al., 2016). Since water acts as plasticizer, only a small amount is
361 required to change glass transition temperature, which increases the food matrix
362 mobility during storage and causes alterations in powder (Goula and Adamopoulos,
363 2010). Thus, low water contents are desirable for powders. Any experimental run within
364 the studied range for inlet air temperature and blackberry pulp solids:arrowroot
365 starch/gum Arabic solids ratio will result in formation of powder with mean moisture
366 content below 6% that is desirable to keep it microbiologically stable.

367

368 ***Water activity***

369 Water activity values of powders ranged from 0.18 ± 0.03 to 0.36 ± 0.04 (**Table 1**).
370 Cagaita (*Eugenia dysenterica* DC.) fruit extract powders presented water activity values
371 lower than 0.3 (Daza et al., 2016). In the present study, except for run 5, that showed
372 water activity of 0.36 ± 0.04 , results of all other runs were below the limit of 0.30,
373 indicating that they are microbiologically stable, as there is no microbial growth below
374 this value, as well as that there is delay in non-enzymatic browning, one of the main
375 reactions of deterioration (Reid and Fennema, 2010).

376 The powders water activity was not significantly influenced ($p>0.05$) by the
377 blackberry pulp solids:arrowroot starch/gum Arabic solids ratio. This means that
378 powders produced with any blackberry pulp solids:arrowroot starch/gum Arabic solids
379 ratio within the range studied will present low values for water activity. On the other
380 hand, the dryer's inlet air temperature significantly influenced ($p<0.05$) the water
381 activity (**Table 2**).

382 **Figure 2B** shows that the lowest water activity values are found at inlet air
383 temperatures above 100°C , regardless of the blackberry pulp solids:arrowroot
384 starch/gum Arabic solids ratio. This may be due to higher heat transfer to the particle,
385 resulting in greater driving force for water evaporation, thus producing powders with
386 lower moisture content and water activity (Daza et al., 2016).

387

388 ***Average Size***

389 Powder particles of all the experimental runs presented varied and large sizes, with
390 diameters ranging from 50.94 ± 0.61 to 119.79 ± 3.54 μm (**Table3 and Figure 3 A and**
391 **B**). Mango powders produced with maltodextrin by spray drying ranged from 0.47 to

392 549 μm , while, without maltodextrin they ranged from 1.9 to 955 μm (Zotarelli et al.,
393 2017).

394 Drying temperatures and blackberry pulp solids:arrowroot starch/gum Arabic
395 solids ratio are parameters that may affect the particle size of powders obtained by spray
396 drying. When drying is performed at higher temperatures, the process is faster than
397 drying at lower temperatures, leading to immediate formation of particles and avoiding
398 particle shrinkage. Similarly, encapsulating agent concentration increases feed viscosity
399 and results in particles with larger diameters (Calomeni et al., 2017). Higher liquid
400 viscosities result in larger particles in atomizers and larger particles in spray drying
401 chamber (Jafari et al., 2017).

402 Besides the encapsulating agent, high content of sugars and acids in the fruit
403 also increases viscosity of feed mixture during spraying in drying chamber. This
404 introduces agglomeration and, consequently, produces larger particles (Shrestha et al.,
405 2007). Solutions of blackberry pulp and encapsulating agent used in feeding were
406 visually very viscous, which may have led to particles with larger diameters.

407 Araujo-Díaz et al. (2017) observed a general contraction of the volume of
408 blueberry powder without encapsulating agent, indicating collapse of microstructure of
409 the sample and suggesting crystallization of low melting sugars present in fruit juice.
410 Islam et al. (2017) observed with scanning electron microscopy that orange
411 juice/maltodextrin 60:40 powders were fused and clumped together and that orange
412 juice/maltodextrin 50:50 powders were agglomerated. Agglomerations were not found
413 in the powders produced with higher maltodextrin ratio (orange juice/maltodextrin
414 40:60 and orange juice/maltodextrin 30:70).

415 In this study, inlet air temperature and blackberry pulp solids:arrowroot
416 starch/gum Arabic solids ratio did not significantly affect particle size. The results of

417 statistical analysis applied to the experimental data of the powders average size showed
418 that the effects of linear, quadratic and interaction factors were not significant at 95%
419 confidence level ($p>0.05$). Due to these nonsignificant factors, it was not possible to
420 construct a predictive mathematical model for the behavior of average size of
421 blackberry powders in function of independent variables.

422 It is believed that, in this work, the presence of larger particles was due to a
423 possible agglomeration process (Figure 3 A and B). The particle size distributions of the
424 samples are shown in **Table 3**. Similar behavior was observed by Zotarelli et al. (2017)
425 for mango powder obtained by spray drying. This can be attributed to the formation of
426 bridges between the smallest particles, resulting in agglomeration that formed larger
427 particles (Zotarelli et al., 2017).

428

429 Insert Table 3 here

430

431 *Hygroscopicity*

432 Hygroscopicity is a material's capacity to absorb moisture from the surrounding
433 environment, and it is an important property to be considered, due to its influence on
434 food stability (Daza et al., 2016). The blackberry powders were stored for 7 days in
435 desiccators with saturated NaCl solution and 75.7% relative humidity at 25°C. As
436 shown in **Figure 3 C**, after 3 days in this condition, the powders of all tests absorbed
437 water from environment, causing caking of the particles and darkening of the powders.
438 After 7 days, powders had a very sticky appearance, indicating that blackberry powders
439 are unstable and hygroscopic, which may hinder their handling.

440

441 Insert Figure 3 here

442

443 Hygroscopicity values of powders obtained by blackberry pulp drying using an
444 arrowroot starch and gum arabic mixture as encapsulating agent ranged from
445 10.93 ± 0.17 to 15.31 ± 0.17 g of adsorbed water/100 g of solids (**Table 1**). These results
446 were lower than those found by Daza et al. (2016) for cagaita powders obtained by
447 using gum arabic (14.8–18.8 g of absorbed water per 100 g of sample) and inulin (13.8
448 and 19.4 g of absorbed water per 100 g of sample) as carrier. Dried beetroot juice
449 particles presented hygroscopicity values of 14.46–20.68 g of water/100 g of dry matter
450 (Bazaria and Kumar, 2016).

451 Inlet air temperature and blackberry pulp solids:arrowroot starch/gum Arabic
452 solids ratio significantly influenced ($p<0.05$) the hygroscopicity of blackberry powders,
453 which presented positive and negative linear effect, respectively (**Table 2**). Inlet air
454 temperature was the variable that most influenced the final product's hygroscopicity.

455 According to **Figure 2C**, the lowest values of hygroscopicity were obtained
456 when lower inlet air temperature and higher blackberry pulp solids:arrowroot
457 starch/gum arabic solids ratio were used. This same behavior was observed by Bazaria
458 and Kumar (2016) for dried beetroot juice particles. According to the authors, this could
459 be well explained by the increasing moisture content with lower inlet air temperature.
460 Powders with very low moisture content tend to be more hygroscopic. The capacity to
461 adsorb ambient moisture is related to the water concentration gradient between the
462 product and the surrounding air (Tonon et al., 2008).

463 As for the blackberry pulp solids:arrowroot starch/gum Arabic solids ratio, both
464 arrowroot starch and gum arabic are materials with low hygroscopicity; consequently,
465 blackberry pulp microencapsulation tends to reduce the resulting powder's
466 hygroscopicity. This fact demonstrated the capacity of arrowroot starch and gum arabic

467 mixture as encapsulating agent to improve the hygroscopicity values of the blackberry
468 powders obtained and make them more stable. These results are in agreement with those
469 observed for orange juice, cactus pear juice, cagaita fruit extracts and beetroot juice
470 powders obtained by spray drying, which showed decreased hygroscopicity due to
471 increased carrier agent concentration (Rodriguez-Hernandez et al., 2005; Bazaria and
472 Kumar, 2016; Daza et al., 2016; Islam et al., 2016).

473 Hygroscopicity of orange juice powder decreased from 0.195 ± 0.02 to
474 0.143 ± 0.01 g H₂O/g with increasing maltodextrin concentration (Islam et al., 2016). In
475 this study, the blackberry powder of run 3 produced with inlet air temperature of 143 °C
476 and ratio of blackberry pulp solids:arrowroot starch/gum Arabic solids of 1:0.72 was the
477 most hygroscopic (15.31 g of adsorbed water/100 g of solids), whereas the powder of
478 run 2, produced with inlet air temperature of 107 °C and ratio of blackberry pulp
479 solids:arrowroot starch/gum Arabic solids of 1:1.78, was the least hygroscopic (10.93 g
480 of adsorbed water/100 g of solids).

481

482 ***Solubility***

483 Solubility is another important parameter that may be evaluated after powder
484 production, because it can potentially affect some of their properties, such as the
485 reconstitution of dry extract or the availability of encapsulated compounds in a food
486 system (Daza et al., 2016). Solubility of blackberry powder particles ranged from
487 58.39 ± 0.99 to $79.37\pm 5.25\%$ (**Table 1**), lower than those reported by Daza et al. (2016)
488 and Santana et al. (2016) in their studies on spray dried cagaita (*Eugenia dysenterica*
489 DC.) fruit extracts obtained by using gum arabic (94.4–97.8%) and inulin (87.7–95.9%)
490 and spray dried jussara pulp produced by using ternary mixture of gum

491 arabic/maltodextrin/whey protein concentrate (78.81–93.46%) and gum arabic/modified
492 starch/soy protein isolate (81.23–92.75%), respectively.

493 The differences in solubility can be explained by chemical structure of each
494 carrier agent. The occurrence of water adsorption by a carbohydrate is attributed to the
495 links between hydrogen present in water molecules and hydroxyl groups available in
496 amorphous regions of substrate as well as in regions that have a crystalline surface
497 (Negrão-Murakami et al., 2017).

498 The solubility of blackberry powders was significantly ($p < 0.05$) influenced by
499 variable inlet air temperature, presenting a positive linear and quadratic effect. The
500 interaction between inlet air temperature and blackberry pulp solids:arrowroot
501 starch/gum Arabic solids ratio also showed a significant positive effect on the solubility
502 of blackberry powders (**Table 2**).

503 Less soluble powders were obtained at lower inlet air temperatures and higher
504 blackberry pulp solids:arrowroot starch/gum Arabic solids ratio (**Figure 2D**), similar to
505 the behavior observed for hygroscopicity. Although gum arabic is highly soluble (Daza
506 et al., 2016), arrowroot starch in its natural form is highly insoluble in water at room
507 temperature, which probably contributed to the decrease of blackberry powders
508 solubility.

509 On the other hand, more soluble powders were produced when extreme inlet air
510 temperatures were used, as shown in **Figure 2D**. Higher temperatures result in faster
511 drying rates, avoiding the particle encountering during drying, maintaining the initial
512 structure formed. Consequently, more porous or fragmented particles are produced at
513 higher temperatures, increasing the surface of particles exposed to water, facilitating the
514 access of water into its structure, hence favoring solubilization (Souza et al., 2015).

515

516 *Optimization of process parameters and analysis of the model*

517 The optimum spray drying conditions for blackberry pulp were determined by surface
518 response methodology, in order to obtain higher process yield and soluble powders in
519 water with low hygroscopic. Due to variation in particle size causing agglomeration it
520 was not possible to generate a predictive mathematical model for the behavior of
521 average size of blackberry powders as a function of independent variables, this response
522 variable was not considered for choosing optimal drying conditions.

523 Moisture content and water activity were low for all runs (moisture content <
524 6% and water activity < 0.36). Therefore, powders produced with any inlet air
525 temperature and blackberry pulp solids:arrowroot starch/gum Arabic solids ratio within
526 the studied range would present good microbiological stability, hence these response
527 variables were not considered to choose optimal drying conditions.

528 Analyzing the model for process yield (**Figure 2A**), the highest values were
529 observed using intermediate inlet air temperature and high blackberry pulp
530 solids:arrowroot starch/gum Arabic solids ratio. According to **Figure 2C**, the lowest
531 values for hygroscopicity were obtained when lower inlet air temperature and higher
532 blackberry pulp solids:arrowroot starch/gum Arabic solids ratio were used. On the other
533 hand, more soluble powders were produced at extreme inlet air temperatures and high
534 blackberry pulp solids:arrowroot starch/gum Arabic solids ratio, as shown in **Figure**
535 **2D**.

536 Thus, the temperature of 143 °C was recommended as optimized condition,
537 since at higher temperatures, powder solubility increased and process yield were
538 reduced at temperatures above 143 °C. As process yield and powder solubility increased
539 with increasing blackberry pulp solids:arrowroot starch/gum Arabic solids ratio and
540 hygroscopicity decreased, the ratio of blackberry pulp solids to arrowroot starch/gum

541 Arabic solids of 1:1.78 was used as optimum condition. Run 4, with inlet air
542 temperature of 143 °C and blackberry pulp solids:arrowroot starch/gum Arabic solids
543 ratio of 1:1.78 was capable of producing powders with low hygroscopicity (12.99 g of
544 adsorbed water/100 g of solids), good solubility in water (74.47%), and satisfactory
545 process yield (50.06%), as shown in **Table 1**.

546 The optimized conditions for blackberry pulp spray drying were experimentally
547 reproduced and process yield, hygroscopicity and solubility were determined in
548 triplicate, as shown in **Table 4**, with predicted mean and experimental values according
549 to the quadratic model.

550

551 Insert Table 4 here

552

553 As expected, the powder produced in optimized condition had low moisture
554 content and water activity, $1.45\pm 0.51\%$ and 0.13 ± 0.04 , respectively, indicating
555 microbiological stability. The values observed for process yield, hygroscopicity, and
556 solubility were relatively close to those observed previously for run 4, as shown in
557 **Table 1**. Based on the values for relative deviation (% DR) obtained for each response
558 variable, the optimization methodology used was considered satisfactory.

559

560 **Conclusions**

561 This study indicated that the arrowroot starch and gum arabic mixture used as
562 encapsulating agent and the increase in the higher drying inlet air temperatures were
563 capable of making blackberry pulp more stable by encapsulation, increasing the
564 efficiency of the drying process and producing powders microbiologically stable, with
565 lower values for hygroscopicity and higher solubility in water. Temperature of 143 °C

566 and blackberry pulp solids:arrowroot starch/gum arabic solids ratio of 1:1.78 were the
567 ideal conditions to obtain high yield and blackberry powders that are soluble in water
568 and less hygroscopic. In future work, the stability of the powders during long periods of
569 storage should be evaluated.

570

571 **Disclosure statement**

572 The authors report no conflicts of interest. The authors alone are responsible for the
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574

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581

582 **References**

583

584 Araujo-Díaz S.B., Leyva-Porras C., Aguirre-Bañuelos P., Álvarez-Salas C.,
585 Saavedra-Leos Z. Evaluation of the physical properties and conservation of the
586 antioxidants content, employing inulin and maltodextrin in the spray drying of
587 blueberry juice. *Carbohydrate Polymers*, 2017;167:317–325.

588

589 Association of Official Analytical Chemists (AOAC). 2006. Official Methods of
590 Analysis, (18th ed.). Association of Official Analytical Chemists, Gaithersburg,
591 Maryland.

592

593 Bazaria B., Kumar P. Optimization of spray drying parameters for beetroot juice
594 powder using response surface methodology (RSM). Journal of the Saudi Society of
595 Agricultural Sciences, 2016; xxx:xxx–xxx.

596

597 Bechgaard T.K., Gulbitten O., Mauro J.C., Smedskjaer M.M. Parametric study of
598 temperature-modulated differential scanning calorimetry for high-temperature oxide
599 glasses with varying fragility. Journal of Non-Crystalline Solids, 2018; 484:84-94.

600

601 Bhandari B.R., Datta N., Howes T. Problems associated with spray drying of sugar-
602 rich foods. Drying Technology, 1997; 15(2): 671–684.

603

604 Cai Y.Z., Corke H. Production and properties of spray-dried *Amaranthus* betacyanin
605 pigments. Journal of Food Science, 2000; 65(7): 1248-1252.

606

607 Caliskan G., Dirim S.N. The effect of different drying processes and the amounts of
608 maltodextrin addition on the powder properties of sumac extract powders. Powder
609 Technology, 2016; 287: 308–314.

610

611 Calomeni A.V., de Souza V.B., Tulini F.L., Thomazini M., Ostroschi L.C., de
612 Alencar S.M., Massarioli A.P., Balieiro J.C.C., de Carvalho R.A., Favaro-Trindade

613 C.S. Characterization of antioxidant and antimicrobial properties of spray-dried
614 extracts from peanut skins. *Food and Bioproducts Processing*, 2017; 105: 215-223.
615

616 Cano-Chauca M., Stringheta P.C., Ramos A.M., Cal-Vidal J. Effect of the carriers
617 on the microstructure of mango powder obtained by spray drying and its functional
618 characterization. *Innovative Food Science and Emerging Technologies*, 2005; 6(4):
619 420–428.
620

621 Chegini G.R., Ghobadian B. Effect of spray-drying conditions on physical
622 properties of orange juice powder. *Drying Technology*, 2005; 23(3): 657–668.
623

624 Chuang L., Panyoyai N., Katopo L., Shanks R., Kasapis S. Calcium chloride effects
625 on the glass transition of condensed systems of potato starch. *Food Chemistry*,
626 2016; 199: 791–798.
627

628 Cruz R., El Dash A.A.M. Amido de chuchu (*Seichium edule*, Swartz). Efeito de
629 fosfatação em sua viscosidade. *Boletim SBCTA*, 1984; 18(4): 371-378.
630

631 D’Agostino M.F., Sanz J., Sanz M.L., Giuffrè A.M., Sicari V., Soria A.C.
632 Optimization of a Solid-Phase Microextraction method for the Gas
633 Chromatography–Mass Spectrometry analysis of blackberry (*Rubus ulmifolius*
634 Schott) fruit volatiles. *Food Chemistry*, 2015; 178: 10–17.
635

636 Dai J., Patel J.D., Mumper R.J. Characterization of blackberry extract and its
637 antiproliferative and anti-inflammatory properties. *Journal of Medicinal Food*,
638 2007; 10(2): 258–265.

639

640 Daza L.D., Fujita A., Fávoro-Trindade C.S., Rodrigues-Ract J.N., Granato D.,
641 Genovese M.I. Effect of spray drying conditions on the physical properties of
642 Cagaita (*Eugenia dysenterica* DC.) fruit extracts. *Food and Bioproducts Processing*,
643 2016; 97: 20-29.

644

645 Eldridge J.A., Repko D., Mumper R.J. Retention of Polyphenolic Species in Spray-
646 Dried Blackberry Extract Using Mannitol as a Thermoprotectant. *Journal of*
647 *Medicinal Food*, 2014; 17(10): 1064–1069.

648

649 Elisia I., Hu C., Popovich D.G., Kitts D.D.. Antioxidant assessment of an
650 anthocyanin-enriched blackberry extract. *Food Chemistry*, 2007; 101(3): 1052–
651 1058.

652

653 Ferrari C.C., Ribeiro C.P., Aguirre J.M. Spray drying of blackberry pulp using
654 maltodextrin as carrier agent. *Brazilian Journal of Food Technology*, 2012; 15(2):
655 157-165.

656

657 Gharsallaoui A., Roudaut G., Chambin O., Voilley A., Saurel R. Applications of
658 spray-drying in microencapsulation of food ingredients: An overview. *Food*
659 *Research International*, 2007; 40(9): 1107–1121.

660

661 Gomar A., Hosseini A., Mirazi N. Preventive effect of *Rubus fruticosus* on learning
662 and memory impairment in an experimental model of diabetic neuropathy in male
663 rats. *PharmaNutrition*, 2014; 2(4): 155–160.
664

665 Goula A.M., Adamopoulos K.G. A new technique for spray drying orange juice
666 concentrate. *Innovative Food Science and Emerging Technologies*, 2010; 11(2):
667 342-351.
668

669 Hager T.J., Howard L.R., Liyanage R., Lay J.O., Prior R.L. Ellagitannin
670 composition of blackberry as determined by HPLC-ESI-MS and MALDI-TOF-MS.
671 *Journal of Agricultural and Food Chemistry*, 2008; 56(3): 661–669.
672

673 Hardenburg R.E., Watada A.E., Wang C.Y. 1986. The commercial storage of fruits,
674 vegetables and commercial nursery stocks. US Department of agriculture,
675 *Agriculture Handbook*, p. 66.
676

677 Hoover R. Composition, molecular structure, and physicochemical properties of
678 tuber and root starches: a review. *Carbohydrate Polymers*, 2001; 45(3): 253-267.
679

680 Igual M., Ramires S., Mosquera L.H., Martínez-Navarrete N. Optimization of spray
681 drying conditions for lulo (*Solanum quitoense* L.) pulp. *Powder Technology*, 2014;
682 256: 233–238.
683

684 Islam M.Z., Kitamura Y., Kokawa, Monalisa K., Tsai F.H., Miyamura S. Effects of
685 micro wet milling and vacuum spray drying on the physicochemical and antioxidant

686 properties of orange (*Citrus unshiu*) juice with pulp powder. Food and Bioproducts
687 Processing, 2017; 101: 132–144.

688

689 Islam M.Z., Kitamura Y., Yamano Y., Kitamura M. Effect of vacuum spray drying
690 on the physicochemical properties, water sorption and glass transition phenomenon
691 of orange juice powder. Journal of Food Engineering, 2016; 169:131–140.

692

693 Jafari S.M., Ghalenoei M.G., Dehnad D. Influence of spray drying on water
694 solubility index, apparent density, and anthocyanin content of pomegranate juice
695 powder. Powder Technology, 2017; 311: 59-65.

696

697 Joo M., Lewandowski N., Auras R., Harte J., Almenar E. Comparative shelf life
698 study of blackberry fruit in bio-based and petroleum-based containers under retail
699 storage conditions. Food Chemistry, 2011; 126(4): 1734–1740.

700

701 Kafkas E., Kosar M., Türemis N., Baser K.H.C. Analysis of sugars, organic acids
702 and vitamin C contents of blackberry genotypes from Turkey. Food Chemistry,
703 2006; 97(4): 732-736.

704

705 Leonel M., Cereda M.P., Sarmiento S.B.S. Arrowroot (*Maranta arundinacea*) as a
706 Possible Raw Material for Starch Industries. Brazilian Journal Food Technology,
707 2002; 5: 151-155.

708

709 Machado A.P.F., Pasquel-Reátegui J.L., Barbero G.F., Martínez J. Pressurized
710 liquid extraction of bioactive compounds from blackberry (*Rubus fruticosus* L.)

711 residues: a comparison with conventional methods. Food Research International,
712 2015; 77(3): 675–683.

713

714 Mothé C.G., Rao M.A. Thermal behavior of gum Arabic in comparison with cashew
715 gum. Thermochemica Acta, 2000; 357-358: 9-13.

716

717 Negrão-Murakami A.N., Nunes G.L., Pinto S.S., Murakami F.S., Amante E.R.,
718 Petrus J.C.C., Prudêncio E.S., Amboni R.D.M.C. Influence of DE-value of
719 maltodextrin on the physicochemical properties, antioxidant activity, and storage
720 stability of spray dried concentrated mate (*Ilex paraguariensis* A. St. Hil.). LWT -
721 Food Science and Technology, 2017; 79: 561-567.

722

723 Perdomo J., Cova A., Sandoval A.J., Garía L., Laredo E., Müller A.J. Glass
724 transition temperatures and water sorption isotherms of cassava starch.
725 Carbohydrate Polymers, 2009; 76(2): 305–3013.

726

727 Ramírez, M.J., Giraldo, G.I., Orrego, C.E. Modeling and stability of polyphenol in
728 spray-dried and freeze-dried fruit encapsulates. Powder Technology, 2015; 277: 89–
729 96.

730

731 Ré M.I. Microencapsulation by spray drying. Drying Technology, 1998; 16(6):
732 1195-1236.

733

734 Reid D.S., Fennema O.R. 2010. Água e gelo. In: Damodaran S., Parkin K.L.,
735 Fennema O.R., (Eds.), Química de Alimentos de FENNEMA. Artmed, Porto
736 Alegre, 25–74.

737

738 Rodriguez-Hernandez G.R., Gonzalez-Garcia R., Grajales-Lagunes A., Ruiz-
739 Cabrera M.A., Abud-Archila M., Spray-drying of cactus pear juice (*Opuntia*
740 *streptacantha*): effect on the physicochemical properties of powder and
741 reconstituted product, *Drying Technology*, 2005; 23(4): 955–973.

742

743 Romero C.A.J., Yépez B.D.V. Ultrasound as pretreatment to convective drying of
744 Andean blackberry (*Rubus glaucus* Benth). *Ultrasonics Sonochemistry*, 2015; 22:
745 205–210.

746

747 Saavedra -Leos Z., Leyva-Porras C., Araujo-Díaz S.B., Toxqui-Terán A., Borrás-
748 Enríquez A.J. Technological application of maltodextrins according to the degree of
749 polymerization. *Molecules*, 2015; 20(12): 21067–21081.

750

751 Saavedra-Leos M.Z., Alvarez-Salas C., Esneider-Alcalá M., Toxqui-Terán A.,
752 Pérez-García S.A., Ruiz-Cabrera M. Towards an improved calorimetric
753 methodology for glass transition temperature determination in amorphous sugars.
754 *CyTA – Journal of Food*, 2012; 10(4): 258–267.

755

756 Santana A., Cano-Higueta D.M., de Oliveira R.A., Telis V.R.N. Influence of
757 different combinations of wall materials on the microencapsulation of jussara pulp
758 (*Euterpe edulis*) by spray drying. *Food Chemistry*, 2016; 212:1–9.

759

760 Sartori T., Menegalli, F.C. Development and characterization of unripe banana
761 starch films incorporated with solid lipid microparticles containing ascorbic acid.
762 Food Hydrocolloids, 2016; 55, 210-219.

763

764 Schlemmer D., Sales M.J.A., Resck I.S. Preparação, Caracterização e Degradação
765 de Blendas PS/TPS Usando Glicerol e Óleo de Buriti como Plastificantes.
766 Polímeros: Ciência e Tecnologia, 2010; 20(1): 6-13.

767

768 Shrestha A.K., Ua-arak T., Adhikari B.P., Howes T., Bhandari B.R. Glass transition
769 behavior of spray dried orange juice powder measured by differential scanning
770 calorimetry (DSC) and thermal mechanical compression test (TMCT). International
771 Journal of Food Properties, 2007; 10(3): 661–673.

772

773 Souza V.B., Thomazini M., Balieiro J.C.C., Fávoro-Trindade C.S. Effect of spray
774 drying on the physicochemical properties and color stability of the powdered
775 pigment obtained from vinification by products of the Bordo grape (*Vitis labrusca*).
776 Food and Bioproducts Processing, 2015; 93: 39–50.

777

778 Tavares L., Figueira I., Macedo D., McDougall G.J., Leitão M.C., Vieira H.L.A.,
779 Stewart D., Alves P.M., Ferreira R.B., Santos C.N. Neuroprotective effect of
780 blackberry (*Rubus* sp.) polyphenols is potentiated after simulated gastrointestinal
781 digestion. Food Chemistry, 2012; 131(4):1443–1452.

782

783 Tonon R.V., Brabet C., Hubinger M.D. Influence of process conditions on the
784 physicochemical properties of açai (*Euterpe oleraceae* Mart.) powder produced by
785 spray drying. *Journal of Food Engineering*, 2008; 88(3):411–418.
786

787 Villas-Boas F., Franco C.M.L. Effect of bacterial β -amylase and fungal α -amylase
788 on the digestibility and structural characteristics of potato and arrowroot starches.
789 *Food Hydrocolloids*, 2016; 52: 795-803.
790

791 Wang S., Langrish T. A review of process simulations and the use of additives in
792 spray drying. *Food Research International*, 2009; 42(1): 13–25.
793

794 Winarti C., Richana N., Sunarti T.C. Effect of acid hydrolysis on the characteristics
795 of and rographolide-loaded arrowroot starch nanoparticles. *International Journal of*
796 *Food Engineering*, 2015; 1(1): 29–33.
797

798 Wu C.S., Liao H.T. Interface design and reinforced features of arrowroot (*Maranta*
799 *arundinacea*) starch/polyester-based membranes: Preparation, antioxidant activity,
800 and cytocompatibility. *Materials Science and Engineering C*, 2017; 70(1): 54–61.
801

802 Yousefi S., Emam-Djomeh Z., Mousavi S.M. Effect of carrier type and spray drying
803 on the physicochemical properties of powdered and reconstituted pomegranate juice
804 (*Punica granatum* L.). *Journal of Food Science and Technology*, 2011; 48(6): 677–
805 684.
806

807 Zia-Ul-Haq M., Riaz M., De Feo V., Jaafar H.Z., Moga M. *Rubus fruticosus* L.:
808 constituents, biological activities and health related uses. *Molecules*, 2014; 19(8)
809 10998–11029.

810

811 Zotarelli M.F., da Silva V.M., Durigon A., Hubinger M.D., Laurindo J.B.
812 Production of mango powder by spray drying and cast-tape drying. *Powder*
813 *Technology*, 2017; 305: 447–454.

814

815