

Phosphorous incorporation in Pd₂Sn alloys for electrocatalytic ethanol oxidation

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ABSTRACT

Direct ethanol fuel cells (DEFCs) offer multiple advantages to power electric vehicles and portable electronics, but their deployment is currently limited by the unavailability of proper electrocatalysis for the ethanol oxidation reaction (EOR). In this work, we optimize the performance of Pd-based electrocatalysts by alloying Pd with Sn and P. We first detail a synthetic method to produce Pd₂SnP_x nanorods that incorporate up to 40 % of phosphorus. These nanorods are supported on carbon black and tested for EOR. Pd₂SnP_x/C catalysts exhibit mass current densities up to 4.89 A mg_{Pd}⁻¹, well above those of Pd₂Sn/C, PdP₂/C and Pd/C reference catalysts. Furthermore, a twofold lower Tafel slope and a much longer durability are demonstrated for the Pd₂SnP_x/C catalyst. The performance improvement is rationalized with the aid of DFT calculations and is associated with a combination of an electronic and a bifunctional effect.

1. INTRODUCTION

Direct liquid fuel cells provide a means for the straight conversion of chemical energy within a liquid fuel into electricity. As liquid fuel, ethanol offers a large energy density ($8.01 \text{ KW h kg}^{-1}$), low toxicity, relatively high boiling point for safe storage, transportation and operation, and potential for bio-sourcing.^{1,2} These advantages make direct ethanol fuel cells (DEFCs) extremely appealing to power electric vehicles and portable electronics, among other. However, the deployment of DEFCs is being hampered by the high cost and moderate performances of current electrocatalysts for the ethanol oxidation reaction (EOR).³

Pt and Pt-based alloys have been the most studied and optimized EOR catalysts to date, particularly in acidic conditions, but their high cost limits their application.⁴ Compared with acid electrolytes, alkaline solutions are less corrosive and provide faster reaction kinetics for both alcohol oxidation and oxygen reduction, which enable the use of a larger variety of catalysts.⁵ These advantages together with the recent development of high-performance anion exchange membranes, have moved interest from acid- to basic-type DEFCs and from Pt to less costly catalysts. Moving away from Pt-based catalysts in alkaline solution, increasing attention is being paid to Pd, which offers lower cost, better resistance to poisoning and similar or even better catalytic activities.⁶⁻⁸ We and others have recently demonstrated that alloying Pd with Sn and optimizing the catalyst crystallographic facets significantly improve EOR performances through a combination of electronic and bifunctional effects.⁹⁻¹² We have also recently reported that the incorporation of phosphorous into Pd catalyst strongly improves its EOR performance by other mechanisms.¹³ Phosphorous inclusion provides advantages in terms of introducing additional adsorption sites,^{14,15} slightly modifying the electronic structure of Pd,¹⁶ shifting the Pd oxide formation to higher potentials that in turn results in a better stability,¹⁷ and potentially reducing the amount of Pd required to reach a certain catalytic activity, thus further reducing the overall catalyst cost.^{15,18-24}

Herein we report an approach to prepare Pd nanocrystals that incorporate both elements, Sn and P. We produced Pd_2SnP_x by reacting intermetallic Pd_2Sn with a phosphorous precursor during the nanoparticle growth stage. As-synthesized nanoparticles were supported on carbon black and tested toward ethanol oxidation in alkaline media. DFT calculations were used to identify the relationship between the measured performances and the catalyst composition.

2. EXPERIMENTAL

2.1. Chemicals

Oleylamine (OAm, 80–90%) was purchased from ACROS Organics. 1-Octadecene (ODE, 90%), palladium(II) acetylacetonate ($\text{Pd}(\text{acac})_2$, Pd 34.7wt%), tin(II) acetate ($\text{Sn}(\text{OAc})_2$, 99%), hexamethylphosphorous triamide (HMPT, 97%), trioctylphosphine (TOP, 97%), methylamine hydrochloride (MAC, 98%), potassium hydroxide (KOH, 85%), and Nafion (5 wt% in a mixture of low aliphatic alcohols and water) were obtained from Sigma-Aldrich. A reference Pd catalyst, 20% Pd on activated carbon powder, was purchased from Alfa Aesar. Carbon black Vulcan XC-72 was obtained from Fuel Cell Earth. Hexane, ethanol and acetone were of analytical grade and obtained from various sources. MilliQ water was obtained from a PURELAB flex from ELGA. All chemicals were used as received, without further purification.

2.2. Synthesis of Pd_2SnP_x nanorods

91.4 mg (0.3 mmol) of $\text{Pd}(\text{acac})_2$, 35.5 mg (0.3 mmol) of $\text{Sn}(\text{OAc})_2$ and 68.0 mg (1 mmol) of MAC were mixed with 20 mL of OAm in a 50 mL three-neck flask connected to the Schlenk line coupled to an exhaust gas absorption solution (1 M CuSO_4). After keeping the precursor mixture under argon flow for 15 min, 1 mL of TOP was introduced. Subsequently, the solution was heated to 100 °C and maintained at this temperature for 1 h. Then temperature was slowly increased to 200 °C at a rate of 5 °C/min and maintained for 30 min. Next, temperature was increased to 300 °C in 40 min. During this temperature increase, the solution turned black indicating the occurrence of the Pd-Sn nanocrystal nucleation.²⁵ When the solution reached 300 °C, 0.2 mL (1.1 mmol) of HMPT dissolved in 0.5 mL of ODE was injected and the mixture was allowed to react for 1 h before cooling down to ambient temperature. The reaction product was precipitated by adding excess amount of acetone and centrifugation at 5000 rpm for 5 min. Then, it was re-dispersed and re-precipitated 3 times with chloroform and acetone. The final black product was dispersed in hexane.

2.3. Synthesis of reference nanocrystals: Pd_2Sn and PdP_2

Pd_2Sn nanorods were produced following the exact same protocol described above but without adding HMPT at 300 °C.²⁵ PdP_2 nanocrystals were obtained through the same procedure but without adding $\text{Sn}(\text{OAc})_2$ to the initial precursor solution.¹³ Nanoparticles were purified as detailed above and the final black precipitates were dispersed in hexane.

2.4 Catalysts preparation

$\text{Pd}_2\text{SnP}_x/\text{C}$, $\text{Pd}_2\text{Sn}/\text{C}$ and $\text{Pd}_2\text{P}/\text{C}$ electrocatalysts were prepared by supporting the corresponding nanocrystals on carbon black.²⁶ Briefly, 5 mg of Pd_2SnP_x (or $\text{Pd}_2\text{Sn}/\text{Pd}_2\text{P}$) dispersed in 5 mL of hexane were mixed with 5 mg of Vulcan XC-72 carbon dispersed in

ethanol. The mixture was sonicated for 1 h to homogeneously distribute the nanocrystals over the carbon surface. The product was collected by centrifugation and then dispersed in a mixture of 10 mL ethanol and 1 mL acetic acid to remove surface organic ligands through sonication. After washing with ethanol, the catalyst was dried naturally under ambient condition and then it was annealed at 250 °C in Ar atmosphere for 1h. The final product was dispersed in isopropanol containing 5% Nafion to obtain an ink containing a nanocrystal concentration of 1 mg/mL.

2.5 Electrochemical measurements.

Electrochemical measurements were conducted at room temperature with a BioLogic electrochemical workstation using a three-neck-type cell including a Pt gauze as counter electrode and a Hg/HgO (1 M KOH) electrode as reference. The working electrode was prepared by drop-casting 3 μ L of the catalyst ink on a 5 mm diameter glassy carbon (GC) electrode and letting it dry naturally. The same mass of particles (or Pd for the commercial sample) was used to prepare each electrode, which translated into lower amounts of Pd on the Pd₂SnP_x/C catalyst when compared with the 3 reference catalysts tested. Cyclic voltammetry (CV) curves were recorded at a scan rate of 50 mV s⁻¹ in Ar-saturated aqueous solutions that contained 0.5 M KOH or 0.5 M KOH + 0.5 M ethanol. Chronoamperometry (CA) measurements were conducted at -0.1 V vs. Hg/HgO for 7000 s in a 0.5 M KOH + 0.5 M ethanol electrolyte.

2.6 Structural and chemical characterization

Powder X-ray diffraction (XRD) patterns were collected from the samples supported on a Si substrate on a Bruker-AXS D8 Advanced X-ray diffractometer with Ni-filtered (2 μ m thickness) Cu K radiation ($\lambda=1.5406$ Å) operating at 40 kV and 40 mA. Scanning electron microscopy (SEM) analysis was conducted with a ZEISS Auriga microscope equipped with an energy dispersive X-ray spectroscopy (EDS) detector operating at 20 kV. Transmission electron microscopy (TEM) images were carried out with a ZEISS LIBRA 120 operating at 120 kV and a JEOL 1011 at 100 kV. High-resolution TEM (HRTEM) analysis was carried out using a field emission gun FEI™ Tecnai F20 microscope at 200 kV with a point-to-point resolution of 0.19 nm. Annular dark-field scanning transmission electron microscope (HAADF-STEM) was combined with electron energy loss spectroscopy (EELS) in the Tecnai F20 with a GATAN QUANTUM filter. X-ray photoelectron spectroscopy (XPS) was analyzed on a SPECS system equipped with an Al anode XR50 source operating at 150 mW and a Phoibos 150 MCD-9 detector. The pressure of the analysis chamber was below 10⁻⁷ Pa. The CasaXPS program (Casa Software Ltd., UK) was employed for

the data process. Fourier transform infrared spectroscopy (FTIR) was performed on an Alpha Bruker FTIR spectrometer with a platinum attenuated total reflectance (ATR) single reflection module. Thermogravimetric analyses (TGA) were carried out using a PerkinElmer Diamond TG/DTA instrument. Samples were measured in N₂ from ambient temperature to 700°C at a heating rate of 5 °C/min.

2.7 Computational details

All calculations were performed using the Vienna Ab initio Simulation Package (VASP)²⁷⁻³⁰ within the density functional theory (DFT) framework. Perdew-Burke-Ernzerhof (PBE) functional³¹ was used to treat the exchange-correlation energy. The projector augmented-wave (PAW)³² was applied and the energy cutoff was 400 eV. The sampling over Brillouin zone was treated by the Monkhorst-Pack technique,³³ and a (2×2×1) grid was introduced. Geometry optimization process was repeated until the energy change of two adjacent ionic steps is less than 10⁻⁵ eV and the force on the atoms less than -0.03 eV/Å. Furthermore, dispersion interactions were treated on the DFT-D3 level.^{34,35} During the calculation, the (2×2×1) supercells for Pd₂Sn (001) and P-modified surfaces were used and displayed in Figure S1. A vacuum slab of 15 Å was applied to avoid the pseudo interactions between the periodic images along z axis. The adsorption energies for OH⁻ on different sites of the surfaces were calculated based on the following equation,

$$E_{ad.} = E_{OH/slabb} - E_{OH^-} - E_{slabb} \quad (1)$$

where $E_{OH/slabb}$, E_{OH^-} , and E_{slabb} are the total energies for OH/slabb, OH⁻, and the pure surface, respectively. Furthermore, the energy of OH⁻ was calculated by,³⁶

$$E(OH^-) = E(H_2O) - [\frac{1}{2}E(H_2) - PH \times k_B T \ln 10] \quad (2)$$

3. RESULTS AND DISCUSSION

3.1 Pd₂SnP_x nanorods

Figure 1a displays a representative TEM micrograph of the particles obtained from the reaction of Pd(acac)₂ and Sn(OAc)₂ within OAm, MAC and TOP and the posterior phosphorization step at 300 °C using HMPT (see details in the experimental section). The produced nanoparticles displayed elongated morphologies with an average length and width of (24 ± 3) × (9 ± 1) nm (Figure 1a inset). This morphology resembled that of Pd₂Sn nanorods produced following the same strategy but without the incorporation of HMPT.²⁵ The XRD pattern of the particles displayed an orthorhombic phase with space group Pnma, matching the reference pattern

from Pd₂Sn (JCPDS 01-089-2057). No evidence of additional diffraction peak corresponding to secondary phases, such as tetragonal Pd₅PSn, PdP₂ or SnP, could be observed. HRTEM analysis (Figure 1c) results confirmed the orthorhombic (S.G.: Pnma) Pd₂Sn phase with lattice parameters: a = 5.6500 Å, b = 4.3100 Å, c = 8.1200 Å. STEM-EELS elemental compositional maps unequivocally displayed the presence of Pd, Sn and P evenly distributed throughout the purified nanorods. EDS analysis confirmed the presence of P and allowed to quantify the overall elemental ratios as Pd/Sn/P = 2.1/1.0/2.2. To test the volatility of the measured phosphorous, samples were annealed under argon at 400 °C. After this process, EDS analysis showed a minor decrease of the phosphorus concentration: Pd/Sn/P = 2.1/1.0/1.7.

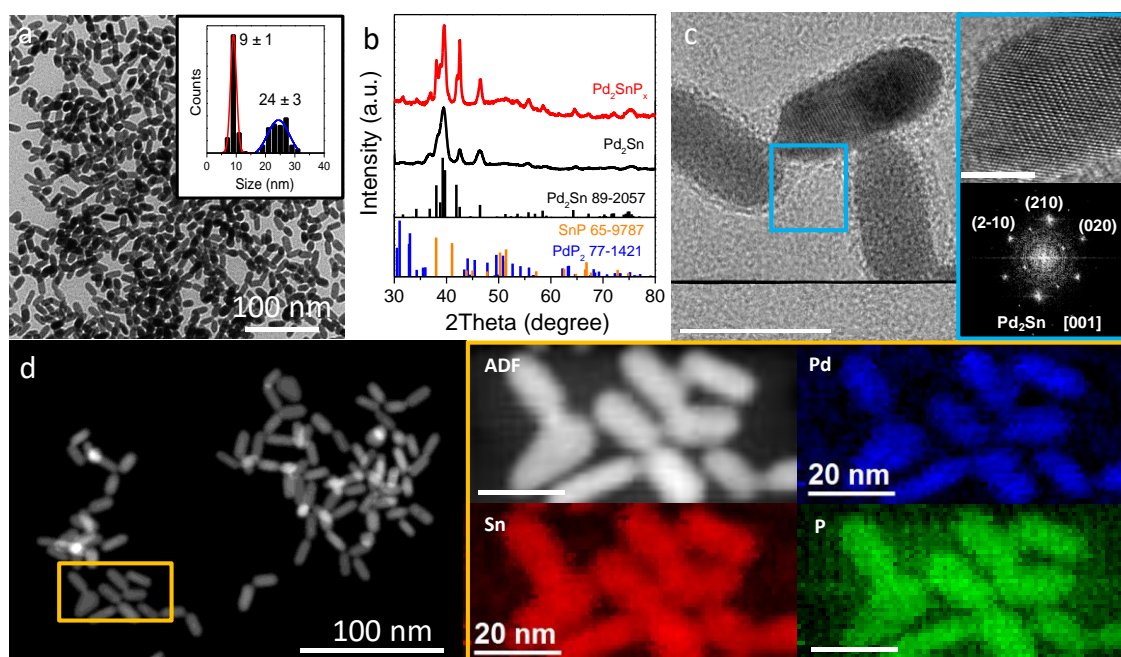


Figure 1. (a) TEM micrograph and histograms of the length (blue) and width (red) distribution of Pd₂SnP_x nanorods. (b) XRD patterns of Pd₂SnP_x and Pd₂Sn nanorods. (c) HRTEM micrograph of Pd₂SnP_x nanoparticles and power spectrum (FFT) of a particle visualized along its [001] zone axis. (d) HAADF-STEM micrograph of Pd₂SnP_x particles and STEM – EELS elemental composition maps from the orange square area: Pd (blue), Sn (red) and P (green).

Figure 2 displays the XPS spectra of purified Pd₂SnP_x nanorods and the Pd₂SnP_x/C catalyst. To prepare the catalysts, Pd₂SnP_x particles were supported on carbon black and treated with acetic acid to displace organic ligands (see experimental section for details). The Pd 3d spectrum of the purified Pd₂SnP_x nanorods exhibited one doublet at 335.4 (3d_{5/2}) and 340.6 eV (3d_{3/2}) that was assigned to a Pd⁰ chemical environment (Figure 2a).^{37,38} After preparing the catalyst, a second doublet appeared at 337.4 eV (3d_{5/2}) and 342.6 eV (3d_{3/2}) as shown in figure

2b. This doublet was ascribed to a Pd²⁺ chemical state and accounted for ca. 14 % of the probed surface Pd.³⁷ The appearance of this oxidized component was associated with the exposure of the unprotected nanoparticles surface to ambient atmosphere during manipulation and transportation.

The Sn 3d spectra indicated the presence of two chemical states already in the purified Pd₂SnP_x nanoparticles, before ligand displacement (Figure 2a). A first doublet at 484.6 eV (Sn 3d_{5/2}) and 493.0 eV (Sn 3d_{3/2}) was assigned to Sn⁰ and accounted for 32 % of the probed Sn.^{37,38} The second doublet, located at 486.6 eV (Sn 3d_{5/2}) and 495.0 eV (Sn 3d_{3/2}), was assigned to an oxidized Sn component, Sn^{x+}, and accounted for the other 68 % of the probed Sn.³⁷ After supporting the nanoparticles on carbon black and displacing the ligands, the oxidized Sn component increased up to the 77 % of the total Sn probed (Figure 2b).

Two phosphorous chemical states were also identified from the XPS analysis of the purified Pd₂SnP_x nanoparticles, before ligand displacement (Figure 2a). These chemical states were assigned to P within a metal phosphide lattice, at 130.0 eV (P 2p_{3/2}) and 130.9 (P 2p_{1/2}), and an oxidized phosphorous form tentatively identified as a phosphate (PO₄)³⁻, at 133.1 eV (P 2p_{3/2}) and 134.0 (P 2p_{1/2}).^{16,37,39} The oxidized component accounted for ca. 65 % of the total P observed. When supported on carbon black and after ligand displacement, only the oxidized component was identified (Figure 2b).

The Pd₂SnP_x surface atomic ratio, as determined by XPS, was Pd/Sn/P = 1/0.97/1.37. Therefore, taking into account EDS data, the surface of the Pd₂SnP_x nanorods was Sn- and P-rich. This result correlated well with the higher percentages of oxidized tin and phosphorous obtained, and might be related to the higher tendency for these two elements to oxidize under ambient atmosphere compared with Pd. Similar results were obtained for Pd₂Sn, with an XPS elemental ratio of Pd/Sn = 1.2.²⁵

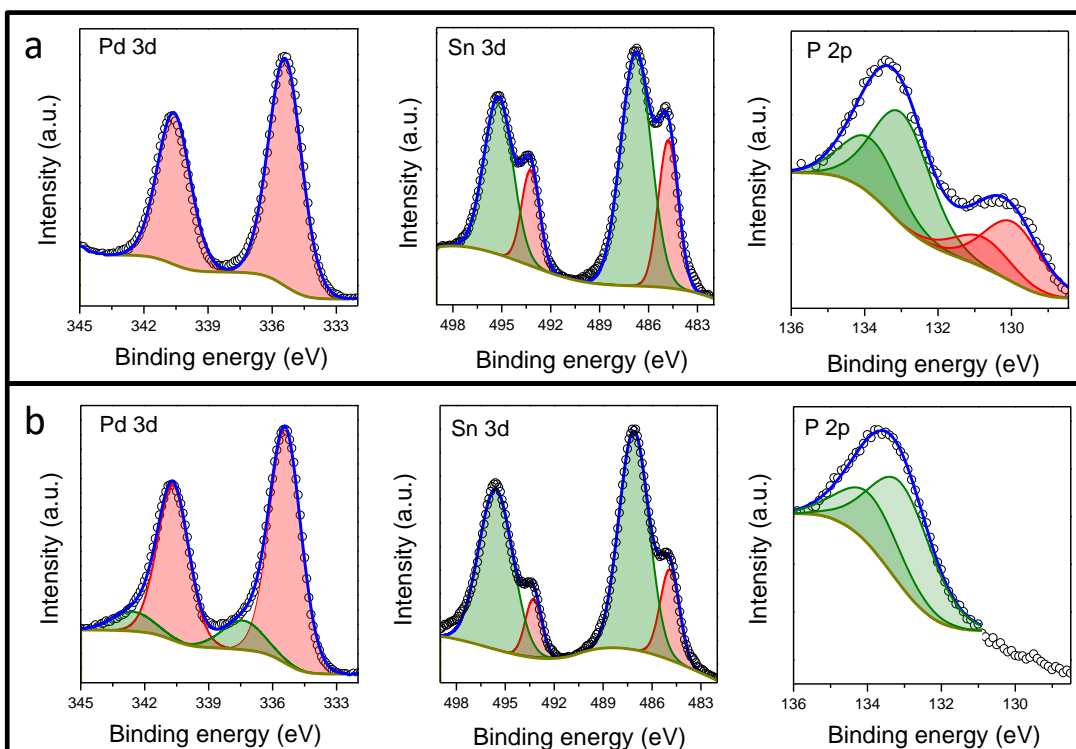


Figure 2. XPS spectra of Pd, Sn and P from Pd₂SnP_x particles (a) and the Pd₂SnP_x/C catalyst (b).

3.2 Electrocatalytic ethanol oxidation

Figure 3a displays the CV curves recorded after 30 activation cycles. The current density peaks in the region between -0.5 V and -0.9 V vs. Hg/HgO were attributed to hydrogen adsorption in the cathodic scan and desorption in the anodic scan.^{40,41} The current density peaks at ca. -0.2 V vs. Hg/HgO in the forward scan were associated with the oxidation of surface Pd. During the reverse scan, clear PdO reduction peaks were identified at around -0.2 V vs. Hg/HgO.

The electrochemical active surface area (ECSA) of the catalysts was estimated from the coulombic charge associated with the PdO reduction peak:

$$ECSA = \frac{Q (\mu C \cdot cm^{-2})}{Q_{PdO} (\mu C \cdot cm_{Pd}^{-2}) \times Pd_{loading} (mg \cdot cm^{-2}) \times 10}$$

where $Q_{PdO} = 405 \mu C cm^{-2}$ was the charge associated to the reduction of a PdO monolayer, the coulombic charge Q was calculated by integrating the area of the PdO reduction peak, and the Pd loading was the amount of Pd on the working electrode.¹² Using this equation, ECSA values for Pd/C, PdP₂/C, Pd₂Sn/C and Pd₂SnP_x/C catalysts were $50.7 m^2 g^{-1}$, $61.1 m^2 g^{-1}$, $76.8 m^2 g^{-1}$, and $116.8 m^2 g^{-1}$, respectively. Notice that significantly larger ECSAs were obtained with the addition of Sn and P to Pd, and the highest ECSA was obtained when incorporating both elements simultaneously to obtain the Pd₂SnP_x/C catalyst.

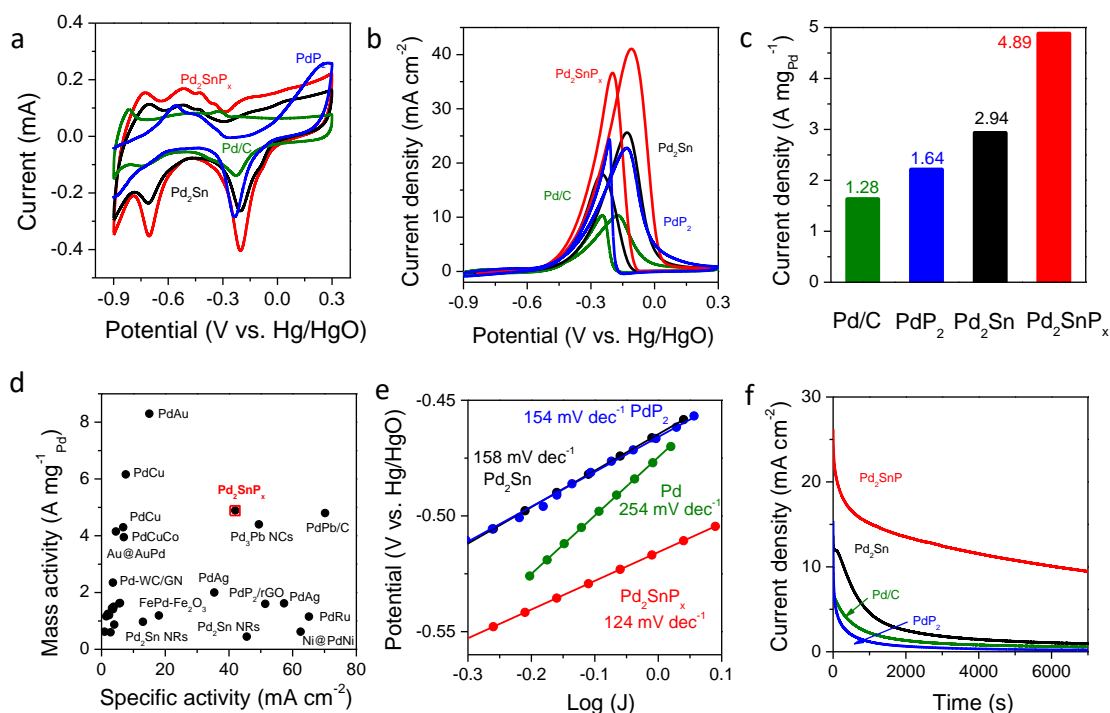


Figure 3. (a) CV curves (after 30 stabilization cycles) of Pd₂SnP_x/C, Pd₂Sn/C, PdP₂/C and commercial Pd/C catalysts in 0.5 M KOH aqueous solution. (b) CV curves, (c) mass peak current density and (d) Mass current density and specific current density of Pd₂SnP_x/C compared with Pd-based catalysts reported in the literature. (e) Tafel plots in 0.5 M KOH + 0.5 M EtOH aqueous solution. (f) CA data in 0.5 M KOH + 0.5 M EtOH aqueous solution at -0.1 V vs. Hg/HgO.

Figure 3b displays the CV curves of the electrocatalysts in 0.5 M KOH + 0.5 M EtOH solution. The two characteristic ethanol oxidation peaks were identified in the anodic and reverse scans for all the electrocatalysts tested. In the forward scan, the current density associated with the EOR started rising at ca. -0.55 V vs. Hg/HgO for all samples, and reached a maximum at a potential in the range from -0.10 V to -0.17 V vs. Hg/HgO, depending on the catalyst composition. Above these potentials, the current density decreased due to the surface oxidation of palladium. The catalyst containing phosphorous and/or tin displayed peaks at slightly higher potentials than the Pd/C catalyst. In the reverse scan, a sharp rise in the current density was triggered by the reduction of PdO at a voltage range between -0.08 V vs. Hg/HgO for Pd₂SnP_x/C and -0.18 for Pd/C. The presence of Sn and P promoted the EOR activity and best performance was obtained when both elements were alloyed together with Pd. Pd₂SnP_x/C catalyst was characterized by the highest peak current density up to 41.2 mA cm⁻², compared with the 25.5 mA cm⁻² for Pd₂Sn/C, 22.5 mA cm⁻² for PdP₂/C and 10.3 mA cm⁻² for Pd/C. These values resulted in dramatically high mass current densities, up to 4.89 A mg_{Pd}⁻¹ (Figure 3c), for

Pd₂SnP_x/C when compared with the reference catalysts tested here and those found in the literature. Figure 3d compares the specific and mass activities of Pd₂SnP_x/C with reported Pd-based catalysts further demonstrating that the simultaneous incorporation of Sn and P effectively improved the Pd activity toward EOR.^{9,12,16,42-58} Additionally, the potential increase required to rise the current density was also significantly low for Pd₂SnP_x/C, especially when compared with commercial Pd/C, as noted in the Tafel plots displayed in figure 3e.

The electrocatalyst long-term stability was evaluated by chronoamperometry measurements (Figure 3f). All the catalysts showed a sharp current density decay during the first 1000 s, which was ascribed to the surface accumulation of strongly adsorbed intermediates that partially blocked the active sites. The Pd₂SnP_x/C catalyst showed a lower decay and was able to maintain much higher current densities during the whole chronoamperometric test, displaying very high current densities of 9.52 mA cm⁻² even after 7000 s operation.

3.3 DFT Calculations

To evaluate the effect of phosphorus, DFT calculations were carried out (computational details and models can be found on the experimental section and the supporting information). According to previous literature, in alkaline media, EtOH is dehydrogenated into adsorbed acetyl, which is further oxidized to acetate by hydroxide species. The oxidation of the acetyl to acetic acid by adsorbed hydroxyl is regarded as the rate-limiting step, while the stripping of the acetic acid in the form of acetate ions in alkaline solution is very rapid.^{59,60} We calculated the OH⁻ adsorption energies at different sites of the catalysts surface (Table 1) and related these values to the catalyst activity considering that a higher chemical adsorption of OH⁻ increases activity by facilitating the formation of CH₃COOH.⁶¹ For a pure Pd₂Sn surface used as a reference, the average Bader charges for Pd and Sn species at the topmost layer are -0.282 and +0.596, respectively. As a result, the adsorption of OH⁻ at Sn sites should be more energetically favorable than at Pd sites. Additionally, according to the optimized geometries, OH⁻ tends to be located at the bridge or center but not at the top sites, i.e. Sn-Pd bridge, Pd-Pd bridge, and Pd₃ center. Due to the slightly different Bader charges, the adsorption energies for the bridge site of Sn-Pd dimers varies slightly with an average value of -0.821 eV. Furthermore, in consideration of the large difference in adsorption energies between Pd- and Sn-relevant sites and the opposite charges, the selective adsorption of CH₃CO radicals near Pd site and that of OH⁻ near Sn ones is to be expected, which benefits the catalytic reaction. These results are consistent with the improved catalytic performances of Pd₂Sn with respect to Pd toward EOR.³⁸

When phosphorus was introduced into the system, two representative models were considered (Figure S1b and 1c). A first model corresponded to the incorporation of P within the Pd₂Sn lattice electronically influencing Pd and Sn surface reaction sites and incorporating new adsorption sites. A second model considered the presence of oxidized P on the catalyst surface according to XPS results. In the first model, the Bader charges of Pd near P increased slightly, while those of Sn remained nearly unchanged, which can be confirmed by the EDD diagram in Figure S2 of the SI. The adsorption energies of OH⁻ at different sites all decreased to a certain extent, which facilitated overcoming the EOR rate-limiting step. The lowest adsorption energies corresponded to the adsorption of OH⁻ on top of P. In a second model, we took into account XPS results that experimentally evidenced the presence of oxidized P species, PO_x, on the catalyst surface. As shown in Figure S1c and Figure S3, due to the surface oxidation, Sn ions close to P are oxidized to a much higher valence state, and an electron transfer is clearly observed (Figure S3c). These significant changes in electronic structures lead to a larger decrease of the adsorption energies for OH⁻ (Table S1), which we believe favored boosting the catalytic activity of the material. We believe that the promotion of the OH⁻ adsorption not only contributed to increase the EOR activity, but was also helpful to oxidize poisoning species, thus increasing the catalyst stability.

Table 1 Adsorption energies for OH⁻ on different sites of Pd₂Sn and Pd₂SnP_x surfaces, considering two sites and chemical states of P, within the lattice as P and at the surface as PO_x.

	Sn-Pd bridge	Pd-Pd bridge	Pd ₃ center	P top
Pd ₂ Sn	-0.821	-0.501	-0.499	–
Pd ₂ Sn incorporating P	-0.851	-0.552	-0.580	-0.925
Pd ₂ Sn incorporating surface PO _x	-1.041	-0.560	-0.658	–

CONCLUSIONS

In summary, Pd₂SnP_x nanorods were synthesized through phosphorization of Pd₂Sn nanocrystals with a highly active reagent-HMPT in a one-pot two-steps colloidal reaction. Pd₂SnP_x/C catalysts exhibited significantly enhanced activity and durability toward EOR in alkaline media, when compared with Pd₂Sn/C, PdP₂/C and commercial Pd/C catalysts. The introduction of P additionally improved the durability of Pd₂SnP catalyst and resulted in lower Tafel slopes that denoted a faster charge transfer kinetics or a larger density of active sites. DFT calculations showed that the incorporation of phosphorous either as lattice P or as a surface phosphate, allowed reducing the OH⁻ adsorption energy both through an electronic effect and a direct bifunctional role, thus contributing to overcome the rate limiting step in EOR and reducing the rate of adsorption of poisoning species.

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