

1       Insights into the direct carbonation of activated  
2       lizardite: the identification a poorly reactive  
3       amorphous Mg-rich silicate phase

4                                   *K. Rausis<sup>a,\*</sup>, A. Ćwik<sup>a</sup>, I. Casanova<sup>a,b</sup>*

5       <sup>a</sup>Institute of Energy Technologies and Barcelona Research Center in Multiscale Science and  
6       Engineering. Universitat Politècnica de Catalunya - Barcelona Tech. Campus Diagonal-Besòs,  
7       C3.11, 08019, Barcelona, Spain

8       <sup>b</sup>Department of Civil and Environmental Engineering. Universitat Politècnica de Catalunya -  
9       Barcelona Tech. Campus Nord, B1, 08034, Barcelona, Spain

10    ABSTRACT

11       This work aims to shed light on **the** yet unanswered question regarding the limited carbonation  
12       yield of activated lizardite via direct carbonation. Two amorphous Mg-rich silicate phases were  
13       identified upon activation. A rapid and complete carbonation of a highly reactive amorphous  
14       silicate phase was observed under moderately low pressure and temperature conditions (50-120°C,  
15       6 bar). Carbonation of this phase yielded to the formation of carbonates and a Si-rich passivating  
16       phase. On the other hand, the other amorphous silicate phase remained unaltered upon carbonation,

---

\* Corresponding author.

*E-mail address: kwon.rausis@upc.edu; Phone: +34 934011857*

17 fixing a significant amount of Mg within its disordered structure. The presence of poorly reactive  
18 intermediate Mg-rich silicate and Si-rich phases might be responsible for the yet unanswered  
19 relatively low carbonation efficiencies obtained via direct carbonation of activated lizardite. These  
20 limiting factors are considered to reduce the carbonation yield significantly more than the  
21 nucleation of forsterite during thermal activation. Analogous experiments carried with different  
22 meta-serpentines yielded the formation of distinct carbonate phases. The different distribution of  
23 highly and poorly-reactive amorphous phases among the different activated materials might have  
24 played an important role in the accelerated formation of magnesite (which was observed to occur  
25 once hydromagnesite formation reached a steady state) and the transformation of nesquehonite to  
26 dypingite-like phases.

## 27 KEYWORDS

28 Mineral carbonation; activated serpentine; magnesite formation; CO<sub>2</sub> sequestration, amorphous  
29 materials.

### 30 1. Introduction

31 Mineral carbonation is considered one of the safest and most suitable ways to sequester CO<sub>2</sub>  
32 (Bobicki et al., 2012; Prigiobbe et al., 2009; Sipilä et al., 2008), attempting to mimic the natural  
33 weathering of Ca/Mg-rich silicate rocks in an anthropic timescale (Gadikota et al., 2014; Kelemen  
34 and Matter, 2008). CO<sub>2</sub> is chemically reacted forming environmentally benign and stable  
35 carbonates. Natural Mg/Ca-bearing silicates are foreseen as potential raw materials for permanent  
36 CO<sub>2</sub> fixation (serpentine, olivine and pyroxenes; Dufaud et al., 2009; Gerdemann et al., 2007).  
37 Large CO<sub>2</sub> sequestration capacities, exceeding the total CO<sub>2</sub> that can be produced by burning fossil  
38 fuels (Lackner, 2003), combined with exothermically driven carbonation reactions of such

39 materials, enhances their potential for carbon capture and storage applications (Chizmeshya et al.,  
40 2002; Lackner et al., 1995; McKelvy et al., 2004).

41 Accelerating the carbonation rate relative to natural carbonation of silicate minerals is  
42 compromised by major scaling-up drawbacks (Gadikota et al., 2014; Huijgen et al., 2007; Kelemen  
43 and Matter, 2008). Pretreatment is required (heat-treatment and grinding) and aqueous slurry  
44 reactions have to be maintained at high temperatures and pressures (Benhelal et al., 2018; Farhang  
45 et al., 2016; Gerdemann et al., 2007), which stray far from post-combustion flue-gas conditions,  
46 making them currently industrially unfeasible (Linga et al., 2007).

47 Wet carbonation reactions of Mg-bearing minerals are proven to occur at kinetic rates feasible  
48 for CCUS applications, although they are not cost-effective (Huijgen et al., 2007). Dry gas-solid  
49 carbonation is the economically-desired reaction but, so far, this mechanism has been found  
50 inefficient (Fagerlund et al., 2012; Larachi et al., 2010; Zevenhoven et al., 2008), regardless of  
51 thermodynamically favorable exothermic reactions (Lackner et al., 1995). However, the addition  
52 of water vapor (Relative Humidity, RH: 100%) significantly enhances the kinetics of such  
53 reactions, when compared to dry gas-solid processes (Highfield et al., 2016; Loring et al., 2012),  
54 by allowing the formation of intermediate metastable hydrated magnesium carbonates (Fricker and  
55 Park, 2014; Zhao et al., 2010). The formation of these materials is kinetically favored although  
56 they are thermodynamically unstable when compared to magnesite ( $\text{MgCO}_3$ ) (Loring et al., 2012;  
57 Schaef et al., 2013; Swanson et al., 2014). The formation of magnesite at low temperatures is  
58 inhibited by the precipitation of hydrated carbonates, possibly because of the high hydration  
59 susceptibility of  $\text{Mg}^{2+}$  ions in solution (Deelman, 2001; Felmy et al., 2012; Zou et al., 2019). The  
60 mechanisms of formation of such hydrated and anhydrous carbonates at low pressures are not well  
61 known (Hopkinson et al., 2012; Rausis et al., 2020).

62 Ex-situ carbonation approaches make use of available above-ground Mg/Ca-rich ores, mines  
63 tailings and wastes, which have high carbonation potential (Bobicki et al., 2012; Harrison et al.,  
64 2013; Li et al., 2018; Power et al., 2013; Sanna et al., 2012; Zarandi et al., 2017a). These alkaline  
65 industrial wastes experience milling processes that lead to a dramatic increase of their surface area  
66 and reactivity (Rigopoulos et al., 2015; Werner et al., 2013). Numerous mining sites worldwide  
67 produce or have produced easy-accessible, finely ground and highly reactive ultramafic mining  
68 wastes (Pronost et al., 2012; Thom et al., 2013; Wilson et al., 2014). Large reserves of serpentinites  
69 (also abundant among ultramafic mining wastes) are of great interest for Carbon Capture,  
70 Utilization and Storage (CCUS) applications because they may contain up to 40% MgO  
71 (Zevenhoven et al., 2008). Heat treatment of serpentine (Benhelal et al., 2019b; Bhardwaj et al.,  
72 2016; Du Breuil et al., 2019; Mouedhen et al., 2017; Pasquier et al., 2014), brucite extraction from  
73 serpentine minerals (Fagerlund et al., 2012; Highfield et al., 2016; Zevenhoven et al., 2008) or  
74 atmospheric CO<sub>2</sub> fixation in mine tailings (Assima et al., 2012; Power et al., 2020, 2010; Thom et  
75 al., 2013; Turvey et al., 2018; Wilson et al., 2014; Zarandi et al., 2017a) are the major mineral  
76 carbonation areas of ultramafic waste research.

77 Calcining serpentine minerals at temperatures between 610°C to 790°C dramatically enhances  
78 their carbonation reactivity (Dlugogorski and Balucan, 2014; Du Breuil et al., 2019; Farhang et  
79 al., 2017; Li et al., 2009; Mann, 2014; McKelvy et al., 2004). This process triggers the release of  
80 OH groups from the serpentine minerals, producing a highly reactive Mg-rich silicate material.  
81 The structural disorder is the main factor that controls the high-reactivity of meta-serpentine  
82 minerals towards carbonation. It has been reported that the degree of carbonation varies with  
83 residual hydroxyl water, suggesting that there is an optimal activation temperature and residence  
84 time. This can be explained by the fact that at temperatures  $\leq 580^{\circ}\text{C}$  (equivalent to  $\geq 45\%$  of residual

85 hydroxyl water) a partial amorphization of lizardite [ $\text{Mg}_3\text{Si}_2\text{O}_5(\text{OH})_4$ ] by thermal dehydration  
86 occurs. However, at temperatures 720°C and higher (equivalent to > 5 % of residual hydroxyl  
87 content) particle sintering and crystallization of Mg-rich silicate phases, such as forsterite  
88 ( $\text{Mg}_2\text{SiO}_4$ ) and enstatite ( $\text{MgSiO}_3$ ) form from the intermediate amorphous phases, reducing  
89 significantly the reactivity of such materials and therefore, should be avoided (Du Breuil et al.,  
90 2019; Li et al., 2009). These crystalline phases are not understood to directly form from serpentine  
91 minerals but rather their formation follows a topotactic transition from intermediate phases, where  
92 the formation rate of crystalline phases decreases with increasing structural disorder (Dlugogorski  
93 and Balucan, 2014). Previous research has suggested that the dehydration of lizardite occurs by  
94 lamellar nucleation and growth. Such a process may provide binding sites to new oxyhydroxide  
95 intermediate materials (McKelvy et al., 2004), such as hydrated carbonates.

96 Previous investigations on direct carbonation (single stage) of activated serpentine have reported  
97 a relatively low carbonation yield even under extreme temperature and pressure conditions (150  
98 bar, 150°C), accounting to a yield between 40-45% (Benhelal et al., 2018; Farhang et al., 2016).  
99 The mechanisms that explain such low carbonation efficiencies remain unanswered, providing  
100 further challenges in the optimization of both activation and carbonation processes (Benhelal et  
101 al., 2019b; Du Breuil et al., 2019). It has been postulated that the formation of a Si-rich passivating  
102 layer significantly contributes to this low carbonation efficiency, by limiting the diffusive effective  
103 area for Mg extraction from the core silicate phases, reducing the carbonation efficiency (Béarat  
104 et al., 2006; Daval et al., 2011; Lafay et al., 2014). More recently it was observed that such Si-rich  
105 phases could also retain a fraction of Mg (Benhelal et al., 2019b). More importantly, it was  
106 discovered that reformation of serpentine minerals may occur upon carbonation of meta-  
107 serpentines, particularly for antigorite. However, reformation of lizardite was not observed even

108 under extreme carbonation conditions (150 bar, 150°C) while a limited carbonation yield was  
109 observed (~40%). Therefore, the low carbonation yields of activated lizardite are either explained  
110 by the formation of Mg-bearing Si-rich passivating phases or it remains unanswered.

111 Indirect carbonation routes (two stage) of activated serpentine can utilize a significantly higher  
112 Mg fraction from heat activated serpentines to form carbonate minerals than direct routes,  
113 achieving as high as 80% (Pasquier et al., 2014; Sanna et al., 2012; Werner et al., 2014). Such  
114 processes are characterized by two or more separate stages of reaction, decoupling the extraction  
115 of reactive magnesium ( $Mg^{2+}$ ) from heat activated serpentine materials, followed by the reaction  
116 of the extracted  $Mg^{2+}$  with  $CO_2$  to form carbonate minerals. This allows a better optimization of  
117 the individual steps, which not only enable a higher extraction of Mg than direct routes but also  
118 carbonate precipitation occurs typically at lower temperatures (Park and Fan, 2004; Sanna et al.,  
119 2012). Moreover, high-purity and profitable carbonates can be produced due to the removal of  
120 impurities in the steps prior to carbonation (Bobicki et al., 2012; Eloneva et al., 2012).

121 This work is aimed at investigating the role of partial dehydration of natural lizardite by heat  
122 activation in accelerated mineral carbonation reactions at moderately-low temperature and  
123 pressure conditions (50 - 120°C; 6 bar) in order to provide more insights into the processes that  
124 contribute to the relatively low carbonation efficiencies during direct carbonation of activated-  
125 lizardite. Understanding such processes is of paramount importance for the further optimization of  
126 both activation and carbonation processes in order to unlock the direct carbonation potential of  
127 such minerals. Lizardite was activated at different temperatures (610, 650 and 710°C) obtaining  
128 different relative proportions of intermediate Mg-rich silicate phases. The novelty of this work is  
129 the identification of two amorphous Mg-rich silica phases upon activation, where one of these  
130 phases was observed to be highly-reactive, obtaining a complete rapid and carbonation of this

131 phase even under moderately-low pressures and temperatures, while the other intermediate  
132 amorphous Mg-rich phase did not carbonate, retaining a significant fraction of Mg within its  
133 disordered structure. The presence of this latter phase might provide answers to the questions  
134 raised about the low carbonation yield during direct carbonation of activated lizardite. Moreover,  
135 it was found that the distinct distribution of a highly reactive Mg-rich silicate phase among the  
136 different activated serpentines played a key role into the formation and evolution of Mg-carbonate  
137 phases, particularly regarding the formation of magnesite.

## 138 2. Materials and methods

### 139 2.1. Analytical

140 Crystalline phases were identified by X-Ray Powder Diffraction (XRD), using a Bruker D8™  
141 diffractometer with Cu K $\alpha$  radiation. Analyses were conducted in a 2 $\theta$  deg range of 5 to 80°, with  
142 a step-size of 0.01° and measuring time of 1 second per step. Fourier Transformed Infrared  
143 Spectrograms (FTIR) were acquired by a FTIR Nicolet 6700™. An attenuated total reflection  
144 (ATR) module was used to record ATR spectra utilizing a germanium crystal (mid-IR, from 750  
145 – 4000 cm<sup>-1</sup>) of the carbonated samples. Transmission spectra of the starting materials (225-4000  
146 cm<sup>-1</sup>) were acquired for analysis of the OH vibration modes. The samples (~3% total mass) were  
147 mixed with KBr (~97%) and pressed into pellets. Data were acquired using 64 scans and 2 data  
148 point spacing. Raman spectra were obtained with an inVia Qontor™ confocal Raman microscope,  
149 equipped with a green laser with an excitation wavelength of 532 nm. Given the substantial  
150 heterogeneity of phase distribution at the microscale after reaction, Raman spectra presented below  
151 correspond to the average of 40 measurements on each sample in order to obtain representative  
152 results. Bulk chemical compositions were determined by X-ray Fluorescence Spectroscopy (XRF)  
153 by the fusion bead method on a UniQuant® apparatus from Thermo Fisher Scientific™.

154 Temperature Programmed Desorption of CO<sub>2</sub> and H<sub>2</sub>O (CO<sub>2</sub>, H<sub>2</sub>O-TPD) analysis was acquired by  
155 BELCAT-M™ instrument equipped with Thermal Conductivity Detector (TCD) in order to  
156 measure the amount of CO<sub>2</sub> stored in the reacted samples. Data were acquired at a heating rate of  
157 10°C/min from room temperature to 850°C, under a He flow of 50mL/min. Calibration of the CO<sub>2</sub>  
158 signal of the TCD was carried out on the basis on measuring the moles of CO<sub>2</sub> from different  
159 known gas mixture compositions varying the CO<sub>2</sub>/He proportions (0.34; 0.18; 0.10). Calibration  
160 of the water vapor signal was carried out by measuring the moles of water vapor originated from  
161 calcining (using a heating rate of 10°C/min) brucite (>99% BioUltra CAS number: 1309-42-8),  
162 Mg(OH)<sub>2</sub>. Secondary-electron Scanning Electron Microscopy (SEM) imaging of powder samples  
163 was carried out with a cross-beam work station Zeiss Neon 40™ workstation, operated at 5keV.  
164 The particle size distribution of samples was measured by a Malvern Panalytical MasterSizer 3000.  
165 Analysis were performed in an aqueous dispersion of the solid samples in deionized water. In this  
166 study, an uncertainty of ±5 % in the particle size analysis was considered.

167

## 168 2.2. Samples

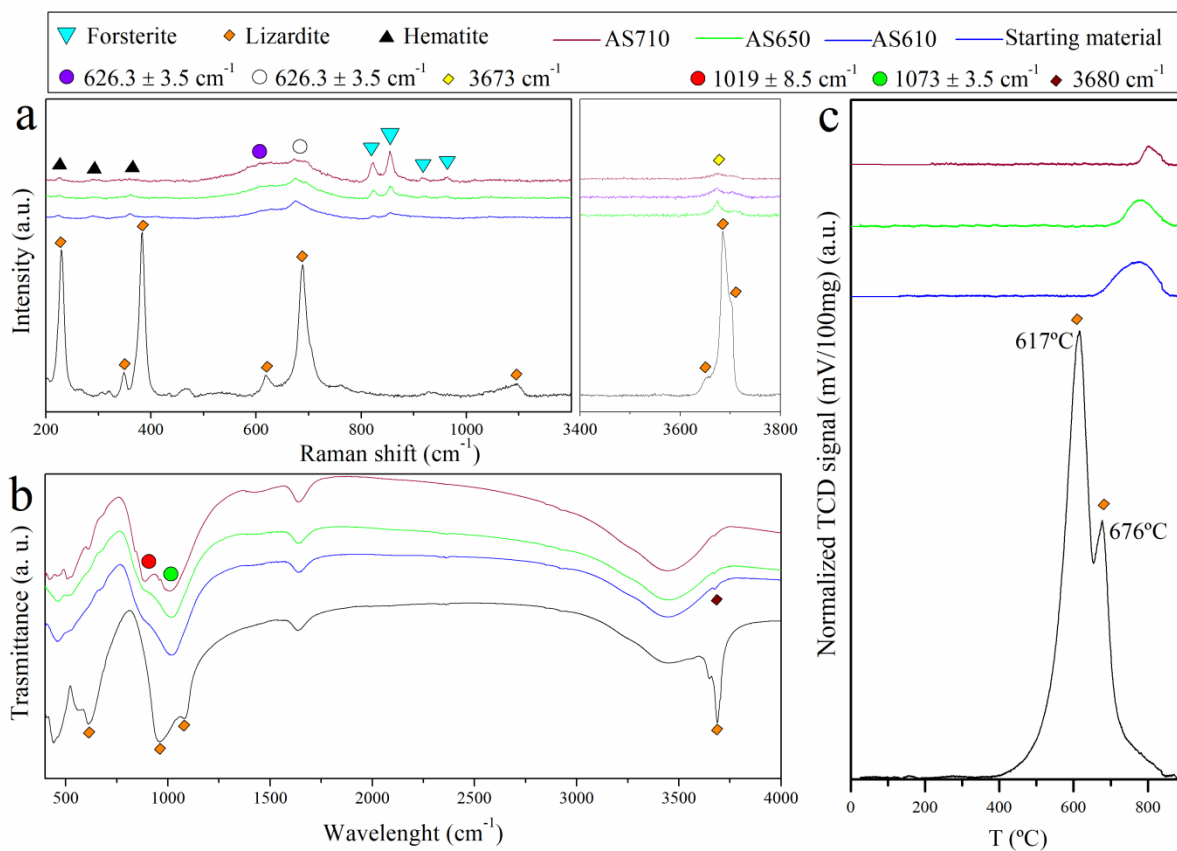
169 Serpentine were obtained from the Hispaniola Island, located in an orogenic complex at the  
170 northern edge of the Caribbean plate. Powder XRD analysis confirmed that the starting material  
171 was composed of lizardite (Figure S1a). Other serpentine phases (e.g. antigorite, chrysotile) were  
172 not observed. Minor magnetite (Fe<sup>3+</sup><sub>2</sub> Fe<sup>2+</sup> O<sub>4</sub>) was also identified (serpentinites generally contains  
173 from 5 to 15 magnetite wt%). The oxide composition of the material was determined by XRF:  
174 SiO<sub>2</sub>, 41.45; TiO<sub>2</sub>, 0.01; Al<sub>2</sub>O<sub>3</sub>, 0.59; Fe<sub>2</sub>O<sub>3</sub>, 8.71; MnO, 0.11; MgO, 35.98; CaO, 0.10. Loss of  
175 ignition accounted for 12.24 wt.% of the original material which is slightly lower than the water  
176 content from stoichiometric lizardite (13.04 wt%). The atomic Mg/(Mg+Fe) ratio was 0.805.



177 Detailed information of the sample's geochemistry can be found in Marchesi, et al., 2016  
178 (Marchesi et al., 2016).

### 179 2.3. Experimental procedure

180 The material was subjected to a prograde heating rate of 1°C/min up to 610 (AS610), 650  
181 (AS650) and 710°C (AS710) respectively, and maintained for 16h at the desired temperature,  
182 generating an activated Mg-rich silicate material (product of the amorphization of lizardite; Figure  
183 1, S1). Prior to heat treatment, the material was ground to a powder and sieved to obtain grains of  
184 size smaller than 45  $\mu\text{m}$  (Figure S1b). A detailed analysis of the starting material and the evolution  
185 of Mg-rich silicate phases upon activation can be found in section S1 and S2, respectively.



186

187 **Figure 1.** (a) Raman, emphasizing the OH vibration region, (b) FTIR, (c) TPD analysis of the  
 188 starting materials and the products after heat activation

189 The **direct moist** carbonation experimental setup consists of a stainless steel pressurized continuous  
 190 flow reactor placed within a furnace with an integrated thermocouple (Scheme S1; Rausis et al.,  
 191 2020). Heat activated lizardite was loaded into the reactor and heated to the desired temperature  
 192 (50, 90 and 120°C), using N<sub>2</sub> as a carrier gas (in order to avoid reaction of the activated materials  
 193 with CO<sub>2</sub> during heating or cooling). Then, CO<sub>2</sub> was introduced into the system and the pressure  
 194 was adjusted by pressure regulators and a back-pressure regulator, achieving a constant value of 6  
 195 bar for a given gas flowrate. Prior to introduction in the reactor, CO<sub>2</sub> flowed through a ~50 mL  
 196 vessel containing water; temperature and pressure were chosen to produce an estimated gas  
 197 mixture with > 90% RH. Conditions were kept isothermal during different reaction times, from 30  
 198 minutes to 4 hours. After the experiments, pressure was released and N<sub>2</sub> was used to purge the  
 199 residual CO<sub>2</sub> while cooling. CO<sub>2</sub> and water vapor partial pressures were estimated by the saturated  
 200 water vapor pressure Antoine equation and Raoult's law. CO<sub>2</sub> partial pressure accounts for 5.9,  
 201 5.4 and 4.2 bar for 50, 90 and 120°C experiments, respectively. Water vapor partial pressure  
 202 accounts for 0.1, 0.6 and 1.8 bar for 50, 90 and 120°C experiments, respectively. Table 1  
 203 summarizes the experiments carried out as well as the specific partial pressures for both CO<sub>2</sub> and  
 204 H<sub>2</sub>O<sub>(g)</sub> of each experiment.

Activated material	Time (h)	50°C	90°C	120°C
		P <sub>CO2</sub> : 5.9; P <sub>H2O(g)</sub> : 0.1	P <sub>CO2</sub> : 5.4; P <sub>H2O(g)</sub> : 0.6	P <sub>CO2</sub> : 4.2; P <sub>H2O(g)</sub> : 1.8
AS610	0.5	Nsq	Dyp, AMC	Hmg
	1	Nsq	Dyp	Hmg
	2	Nsq	Dyp	Hmg, Mag

	4	Nsq	Dyp	Hmg, Mag
<b>AS650</b>	0.5	Nsq	Dyp, AMC	Hmg
	1	Nsq	Dyp	Hmg
	2	Nsq	Dyp	Hmg
	4	Dyp, AMC	Dyp	Hmg, Mag
<b>AS710</b>	0.5	Nsq	Dyp, AMC	Hmg
	1	Nsq	Dyp, AMC	Hmg
	2	Nsq	Dyp	Hmg
	4	Dyp, AMC	Dyp	Hmg, Mag

205

206 **Table 1.** Summary of the carried experiments, specific experimental conditions and the identified  
207 carbonate phases.  $P_{CO_2}$  and  $P_{H_2O(g)}$  stands for  $CO_2$  and  $H_2O$  vapor partial pressure, respectively.  
208  $CO_2$  dilution with water vapor (relative humidity  $\geq 90\%$ ) was estimated following the saturated  
209 water vapor pressure Antoine equation and Raoult's law. Nsq: Nesquehonite, Dyp: Dypingite,  
210 Hmg: Hydromagnesite, Mag: Magnesite, AMC: possibly an amorphous Mg carbonate.

211

### 212 3. Results and discussion

#### 213 3.1. Formation of Mg-carbonate phases

214 Newly formed carbonates were identified upon reaction of the three different activated lizardites.  
215 Figure 2 shows the Raman spectra of the reaction products from experiments carried at 50, 90 and  
216 120°C during 30 minutes to 4 hours at 6 bar. At 120°C two newly formed peaks were identified  
217 ( $1094.2 \pm 0.4$ ,  $1116.6 \pm 0.3 \text{ cm}^{-1}$ ) within the region of the characteristic of the  $\nu_1$  symmetric  
218 stretching mode ( $\nu_{1sym}$ ) of the carbonate ion ( $CO_3^{2-}$ ) (Edwards et al., 2005; Frost, 2011) for all three

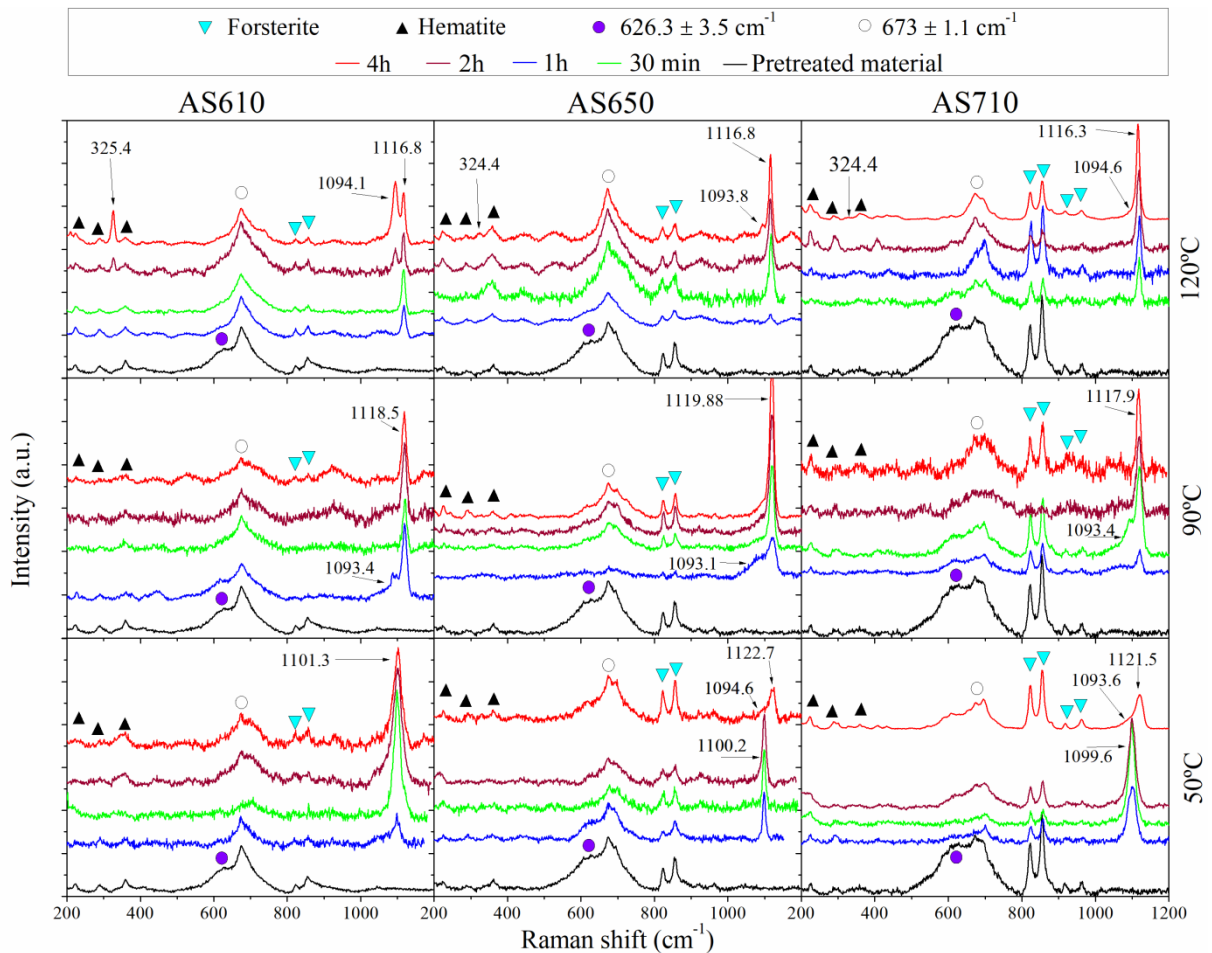
219 activated materials. The  $1094.2 \pm 0.4$  peak is correlated to the emergence of the  $324.9 \pm 0.5$  peak  
220 in the lattice vibration region ( $100\text{-}500\text{ cm}^{-1}$ ). Such peaks are especially evident in AS610, and  
221 they are only observed at 2 and 4 hours. Those peaks might suggest the presence of magnesite  
222 ( $\text{MgCO}_3$ ).

223 Comparison between the Full Width Half Maximum (FWHM) and peak position of the  $\nu_{1\text{sym}}$   
224 carbonate peak of the reaction products is shown on Figure S3. Calculated data from experiments  
225 carried out at  $120^\circ\text{C}$  show that the  $1094.2 \pm 0.4\text{ cm}^{-1}$  peak fit well with reference magnesite for all  
226 the pretreated materials. For AS610 materials, the second peak ( $1116.6 \pm 0.3\text{ cm}^{-1}$ ) fits very well  
227 with hydromagnesite,  $\text{Mg}_5(\text{CO}_3)_4(\text{OH})_2 \cdot 4(\text{H}_2\text{O})$ . However, for AS650 and AS710, this peak is  
228 approaching the reference data for dypingite,  $\text{Mg}_5(\text{CO}_3)_4(\text{OH})_2 \cdot 5\text{H}_2\text{O}$ . This latter mineral has a  
229 similar composition to hydromagnesite but it is structurally more disordered with a variable  
230 amount of water molecules per unit (Canterford et al., 1984; Davies and Bubela, 1973; Rausis et  
231 al., 2020).

232 Two different peaks  $\nu_{1\text{sym}}$  were identified after reactions performed at  $90^\circ\text{C}$  ( $1093.4$ ,  $1118.9 \pm 1$   
233  $\text{cm}^{-1}$ ). The position of both peaks remains constant for all the activated materials, irrespective of  
234 their reaction times. The first peak ( $1093.4\text{ cm}^{-1}$ ) despite having similar position to that of  
235 magnesite, does not emerge together with the lattice vibration peak of magnesite ( $324.9 \pm 0.5$ ),  
236 suggesting the presence of a different carbonate phase. Calculated FWHM vs peak position shows  
237 that the  $1093.4\text{ cm}^{-1}$  peak does not correlate with any other represented Mg-carbonate phase  
238 (Figure S3). Such peak is similar to the one observed by previous studies (Rausis et al., 2020),  
239 which suggest that this peak might be associated with a hydrous amorphous Mg-carbonate (AMC)  
240 phase that has similar composition and dehydration temperature ranges to nesquehonite. This peak  
241 is only observed at 30 minutes of reaction for AS610 and AS650. However, this peak is not

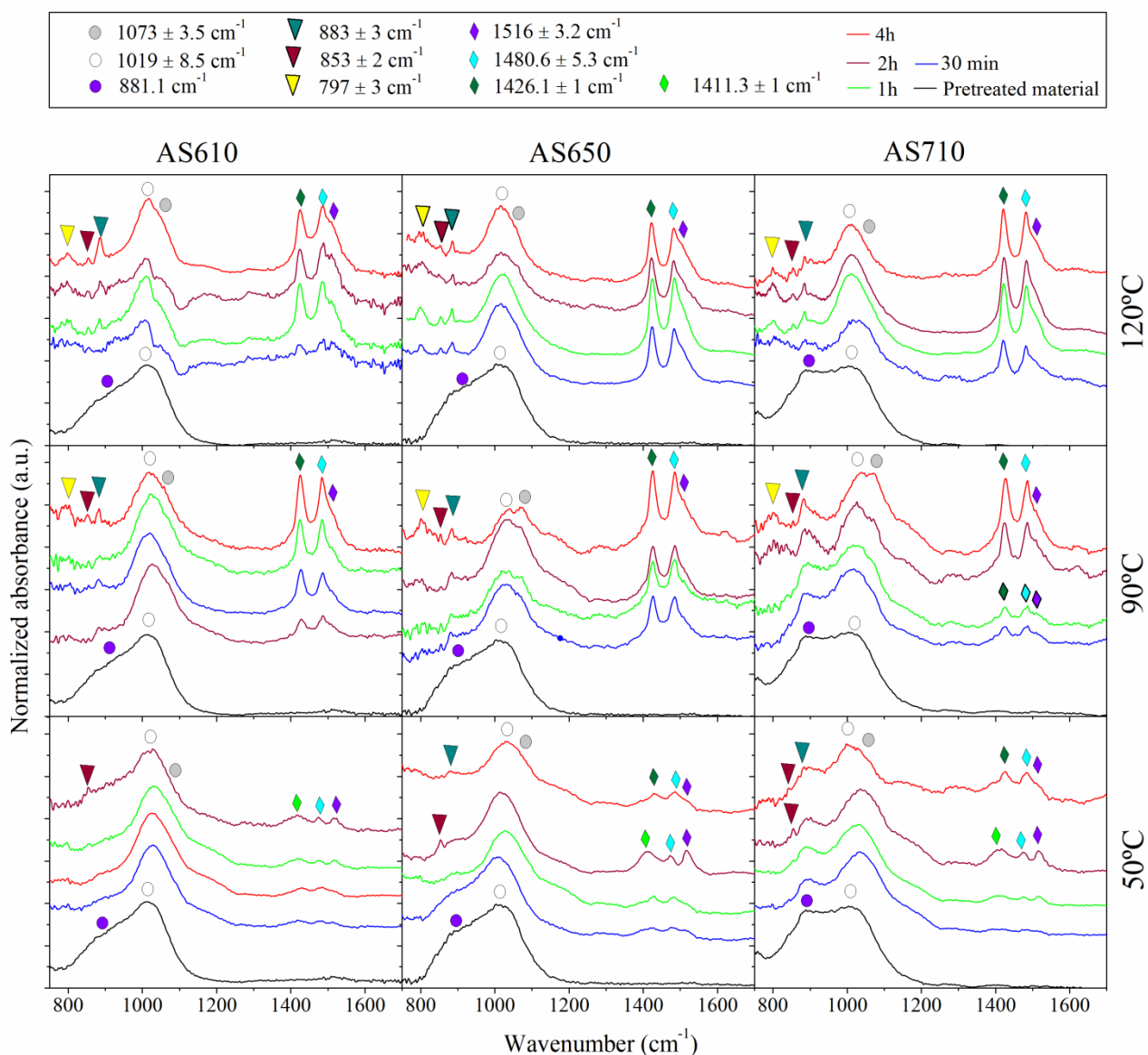
242 observed until 1 hour of reaction for the AS710 experiments. The inexistence of this peak at longer  
 243 reaction times (2 and 4 hours) suggest that the phase responsible for this peak acts as precursor to  
 244 the phase associated with the  $1118.9 \pm 1 \text{ cm}^{-1}$  peak.

245 The second peak ( $1118.9 \pm 1 \text{ cm}^{-1}$ ) appears to be slightly shifted when compared to the one  
 246 observed from 120°C experiments ( $1116.6 \pm 0.3 \text{ cm}^{-1}$ ). The calculated FWHM vs peak position  
 247 data shows a good fit with reference dypingite.



248  
 249 **Figure. 2.** Raman spectra of three different meta-serpentine (activated at 610, 650 and 710°C) and  
 250 the reaction solid products from experiments carried at 50, 90 and 120°C from 30 minutes to 4  
 251 hours.

252 Analyses of the solid products from experiments performed at 50°C show the presence of three  
253 different peaks ( $1094.1 \pm 0.5$ ,  $1100.5 \pm 0.9$ ,  $1122.1 \pm 0.6 \text{ cm}^{-1}$ ) within the  $\nu_{1\text{sym}}$  region. At this  
254 temperature, clear differences are observed for different activated materials. The  $1094.1 \pm 0.5 \text{ cm}^{-1}$   
255 peak is similar to the one observed at 90°C (associated with a possible AMC). The second peak  
256 ( $1100.5 \pm 0.9$ ) fits well with reference nesquehonite,  $\text{Mg}(\text{HCO}_3)(\text{OH}) \cdot 2(\text{H}_2\text{O})$ , only for the AS650  
257 materials. For AS610 and AS710, such peak is observed to be in similar position as nesquehonite  
258 but wider. Moreover, AS610 materials shows the presence of only the  $1100.5 \pm 0.9$  peak at any  
259 reaction time. This peak is only identified from 30 minutes to 2 hours of reaction for the AS650  
260 and AS710 materials. However, at 4 hours, it is no longer identified and two distinct peaks have  
261 emerged ( $1094.1 \pm 0.5$  and  $1122.1 \pm 0.6 \text{ cm}^{-1}$ ). This suggests that the  $1100.5 \pm 0.9$  peak nourishes  
262 the growth of these two latter peaks, in agreement with recent studies (Rausis et al., 2020). The  
263  $1122.1 \pm 0.6 \text{ cm}^{-1}$  peak is only observed for AS650 and AS710 and has the similar position with  
264 reference dypingite but with higher FWHM, probably suggesting a highly disordered structure  
265 (Rausis et al., 2020). The emerged  $1094.1 \pm 0.5 \text{ cm}^{-1}$  peak is associated with a possibly amorphous  
266 phase, as previously discussed. FTIR analysis also evidences the formation of carbonates, and the  
267 observed phases are consistent with Raman observations (Figure 3; see section S3)

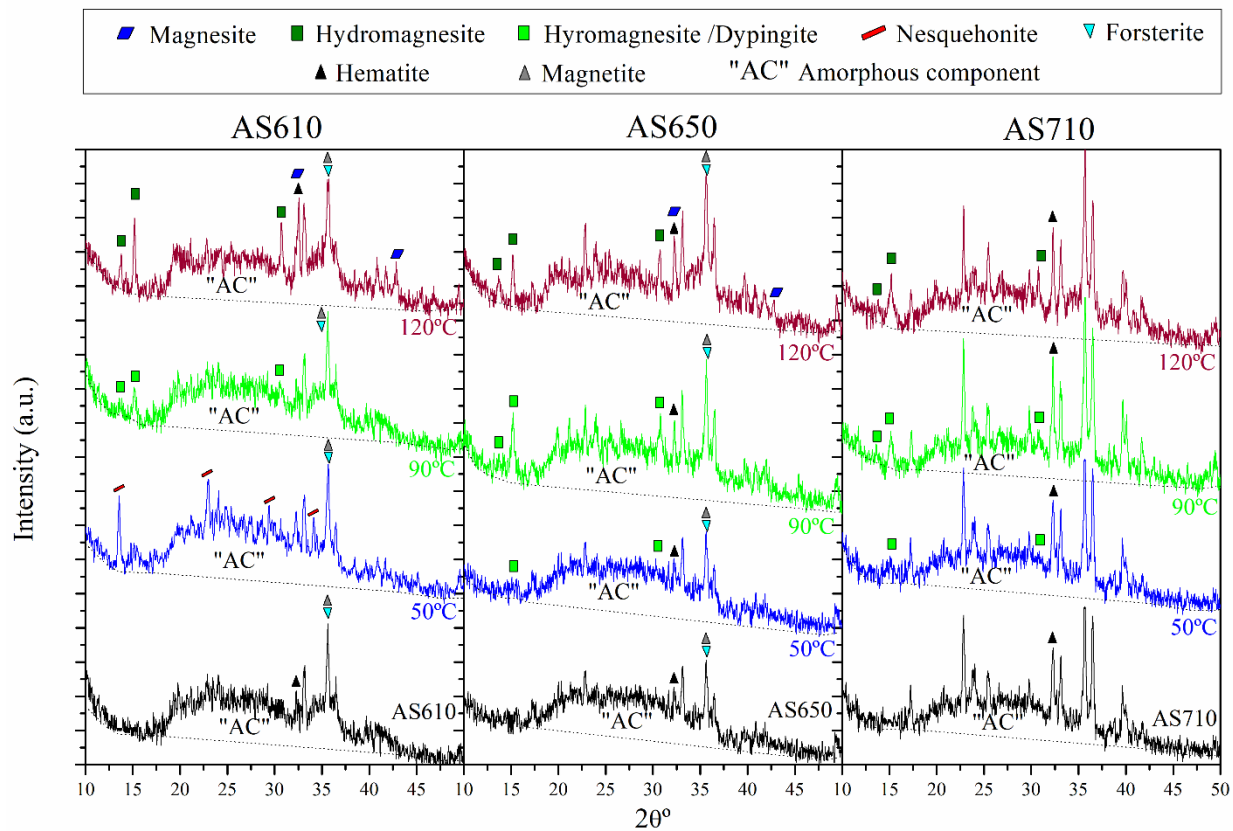


268

269 **Figure 3. FTIR-ATR analysis of the pretreated and carbonated materials at 50, 90 and 120°C and**  
 270 **6 bar, from 30 minutes to 4 hours.**

271 XRD analysis of the activated and carbonated materials (Figure 4) corroborates Raman and FTIR  
 272 observations. At 120°C, characteristic XRD patterns for hydromagnesite (Fricker and Park, 2013;  
 273 Schaefer et al., 2013) were identified for all the activated materials, and magnesite (Giammar et al.,  
 274 2005; Schaefer et al., 2013) only for the AS610 and AS650 materials. A hydromagnesite-dypingite

275 phase was observed at 90°C, resembling XRD features observed by Hövelmann et al., 2012.  
 276 Nesquehonite was observed only at 50°C for AS610. On the other hand, AS650 and AS710 shows  
 277 the presence of a highly disordered dypingite-like phase. The identification of different carbonate  
 278 phases for different activated material under identical carbonation conditions suggest that the  
 279 activated materials play a key role not only in the formation of carbonate phases but also in their  
 280 evolution during carbonation reactions.



281  
 282 **Figure 4.** XRD analysis of the activated and carbonated materials at 50, 90 and 120°C during 4  
 283 hours. Unmarked peaks also correspond to forsterite.

284 Evolution of the carbonation reaction was also monitored by SEM (Figure 5). Hydromagnesite  
 285 plates, arranged in rosettes of crystals  $\geq 1\mu\text{m}$  in size (as in Maroto-Valer et al., 2005 and Power et  
 286 al., 2019) are observed in the AS610 materials carbonated during 1h at 120°C (Figure 5a) as well

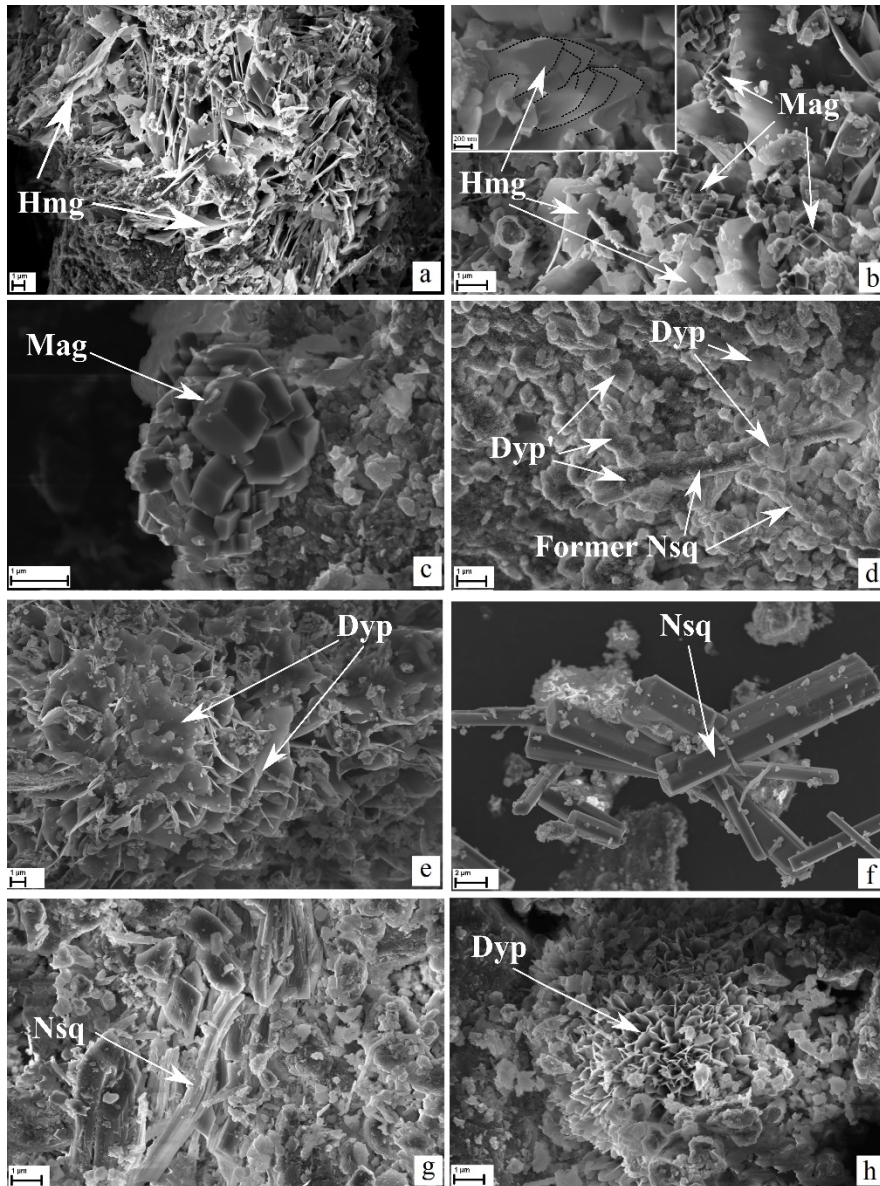


287 as a progressive formation to euhedral magnesite ( $\sim 1\mu\text{m}$ ) (Prigiobbe and Mazzotti, 2013) over  
288 time (2h, Figure. 5b; 4h, Figure 5c). Figure 5b inset and c shows that an aggregation of  
289 hydromagnesite and magnesite crystals respectively, which were possibly formed by nucleation  
290 and crystal growth (Giammar et al., 2005).

291 Elongated and prismatic rod-like structures ( $\sim 5\mu\text{m}$ ), with morphological features resembling  
292 those of nesquehonite (Hänchen et al., 2008; Zarandi et al., 2017b), were identified in the 30  
293 minutes experiments at  $90^\circ\text{C}$  for AS610 materials (Figure 5d). On this prismatic structure is  
294 observed overgrowths of flaky nanocrystals ( $<100\text{nm}$ ) and more developed flaky microcrystals  
295 ( $<1\mu\text{m}$ ), exhibiting features of the “house of cards” texture, which is characteristic of the  
296 transformation of nesquehonite to hydromagnesite or dypingite (Hao and Du, 2009; Hopkinson et  
297 al., 2012; Power et al., 2016; Rausis et al., 2020). The smaller, nanometer-sized crystals also form  
298 sub-spherical aggregates, similar to those reported by Zarandi et al., 2017. Only a dypingite-like  
299 phase, possibly coexisting with an amorphous phase (Rausis et al., 2020), were identified with  
300 Raman and XRD. Therefore, the rod-like structure might be evidence that the identified dypingite  
301 might have formed from the transformation of an early-nesquehonite, exhibiting a well-developed  
302 “house of cards texture”. Such transformation mechanism is a good example of the Ostwald step  
303 rule (Morse and Casey, 1988). This texture is commonly observed on dissolution-recrystallization  
304 self-assembly growth mechanisms. Therefore, this may imply a possible surface water layer  
305 mediating the dissolving-recrystallization mechanism (Taifan et al., 2016). This layer may stem  
306 from either molecular water of the dissolving mineral or from the condensation of water vapor.

307 After 1 hour of reaction, experiments performed at  $90^\circ\text{C}$  for AS610 showed only rosette crystal  
308 arrangements made of dypingite flakes were observed (Figure 5d), resembling features observed  
309 by Hopkinson et al., 2008.

310 Experiments performed at 50°C and 2h for AS650 produced massive rod crystals characteristic  
311 of nesquehonite (Figure 5f). However, analogous experiments on AS710 showed acicular  
312 aggregates that are texturally comparable to nesquehonite (Hopkinson et al., 2008) (Figure 5g).  
313 Raman and XRD analysis showed that the massive nesquehonite has similar FWHM peak to the  
314 reference mineral. However, broader peaks with the same peak position as reference nesquehonite  
315 are associated to the acicular aggregation of oriented prismatic crystals. Carbonation of the AS710  
316 material during 4h results in the formation of rosette crystal arrangements conforming to dypingite  
317 morphology (Figure 5h), indicating the transformation of nesquehonite to dypingite, as also  
318 suggested by the Raman and XRD results.



319

320 **Figure 5.** Representative SEM images of carbonated samples. AS610 carbonated at 120°C for 1h

321 (a), 2h (b) and 4h (c); at 90°C for 30min (d) and 1h (e). Reaction products of AS650 obtained at

322 50°C after 4h (f). Carbonated products of the AS710 materials carbonated at 50°C for 2h (g) and

323 4h (h). Hmg: hydromagnesite, Mag: magnesite, Dyp': nano-dypingite (<100nm), Dyp: dypingite,

324 Nsq: nesquehonite.

325 The estimated CO<sub>2</sub>:H<sub>2</sub>O ratios of the carbonate products (calculated from TPD data; see section  
326 S4, S5) are consistent with the stoichiometric composition of the identified carbonates as  
327 summarized in table 1.

328

### 329 3.2. Evolution of Mg-rich silicate phases upon carbonation

330

331 The intensity of the wide Raman peak located at  $626.3 \pm 3.5 \text{ cm}^{-1}$  (which emerged from thermal  
332 activation, Figure 1a) is diminishing as the carbonation reaction proceeds, probably suggesting  
333 that the phase (responsible for this Raman broad peak) partially or fully nourishes the formation  
334 of carbonates (Figure 2). Since forsterite and minor hematite/magnetite were the only identified  
335 crystalline phases upon activation (as Q<sub>3</sub> dehydroxylate II was not identified), the presence of the  
336 Raman broad peak located at  $626.3 \pm 3.5 \text{ cm}^{-1}$  might be associated with an amorphous Mg-rich  
337 silicate phase, product of the amorphization of lizardite. However, the  $673 \pm 1.1 \text{ cm}^{-1}$  peak (which  
338 also might be associated with an amorphous Mg-rich silicate phase) remained relatively unchanged  
339 upon carbonation. Therefore, this might suggest that these two Raman peaks are associated with  
340 two different amorphous Mg-rich silicate phases (possibly to Q<sub>1</sub> dehydroxylate I and “Q<sub>2</sub>  
341 amorphous enstatite”, since such phases are the only known amorphous intermediate phases of  
342 activated lizardite, see section S2), with the phase responsible for the  $626.3 \pm 3.5 \text{ cm}^{-1}$  Raman  
343 peak, being the most reactive. To our knowledge, this is the first evidence of the significantly  
344 different reactivity of two coexisting intermediate amorphous Mg-rich silicate phases that form  
345 upon activation.

346 FTIR analyses show changes to the Si-O-Si stretching modes region are observed after  
347 carbonation (Figure 3). Upon carbonation, two peaks are observed ( $1019 \pm 8.5$  and  $1073.55 \pm 3.95$

348  $\text{cm}^{-1}$ ). The  $1019 \pm 8.5 \text{ cm}^{-1}$  peak (as also observed in the activated materials) **remains** relatively  
349 unchanged, possibly indicating that the intermediate phase responsible for this peak as well as  
350 overlapping forsterite remained seemingly unreacted upon carbonation. On the other hand, the  
351  $888.1 \text{ cm}^{-1}$  broad peak (observed in the activated materials) is no longer identified upon  
352 carbonation and an emerging well-defined peak at similar position is observed ( $883 \pm 3 \text{ cm}^{-1}$ ),  
353 characteristic of hydromagnesite-like phases and magnesite. The intermediate phase responsible  
354 for the  $888.1 \text{ cm}^{-1}$  broad peak was the only identified reactant upon carbonation, indicating that  
355 this phase is partially or fully nourishing the formation of carbonates. Comparison with Raman  
356 results (Figure 2) and the analysis of the starting materials (Figure 1, S1) suggest that the phase  
357 responsible for the  $888.1 \text{ cm}^{-1}$  FTIR broad peak might be associated **with** a highly reactive  
358 amorphous Mg-rich silicate phase (HRAS), which is strongly associated with the phase responsible  
359 for the  $626.3 \pm 3.5 \text{ cm}^{-1}$  Raman peak. Analogously, the unreacted  $1019 \pm 8.5 \text{ cm}^{-1}$  FTIR peak might  
360 also be associated **with** the poorly-reactive amorphous phase (PRAS) responsible for the  $673 \pm 1.1$   
361  $\text{cm}^{-1}$  Raman peak.

362 Moreover, the  $888.1 \text{ cm}^{-1}$  FTIR band associated **with** the reactive amorphous phase observed  
363 during this study might also not **contain a silanol group** (Benhelal et al., 2019b), **as this functional**  
364 **group** (as well as siloxane and  $\text{Si-O-Al}^{2+}/\text{Na}^{2+}/\text{Mg}^{2+}$  groups) is associated **with** the formation of a  
365 Si-rich passivating layer (Casey et al., 1988; Chizmeshya et al., 2006; Hellmann et al., 1990; Lafay  
366 et al., 2014), since it is inconsistent with the highly-reactive nature of this intermediate and  
367 probably amorphous Mg-rich silicate phase.

368 The identified peak at  $1073.55 \pm 3.95 \text{ cm}^{-1}$  (formed upon carbonation and different from the un-  
369 activated lizardite, Figure 1b) might suggest the formation of phases containing siloxane groups  
370 (Benhelal et al., 2019b) or amorphous silica (Tran et al., 2013). This is consistent with the

371 formation of a passivating Si-rich phase (Chizmeshya et al., 2006; Hellmann et al., 1990; Lafay et  
372 al., 2014), Numerous studies have reported that such phases play an important role in the  
373 passivation of the carbonation reaction (Béarat et al., 2006; Julcour et al., 2015). A fraction of Mg  
374 can also be stored in this Si-rich phase reducing the available Mg fraction to form carbonates  
375 (Benhelal et al., 2019b).

376 XRD studies also show the presence of a broad hump from 17 to 43  $2\theta^\circ$  in all the analyzed  
377 samples, suggesting the presence of an amorphous component (Blue et al., 2017; Fukushi et al.,  
378 2017; McKelvy et al., 2004) even after carbonation (Figure 4), maybe accounting for the unreacted  
379 PRAS, Si-rich passivating phases and, in some experiments, amorphous carbonates mentioned  
380 above.

381 In a recent study it was observed that the recrystallization of serpentine minerals from the  
382 intermediate phases may occur upon direct aqueous carbonation at elevated pressures (120-150  
383 bar) of activated serpentine, particularly for antigorite (Benhelal et al., 2019b). As discussed by  
384 the authors, the re-crystallization of serpentine is considered to be an un-desired reaction, as such  
385 reaction increases the energy penalty of the overall reaction and competes with carbonation  
386 (consuming a fraction of the available reactive Mg from amorphous intermediate phases) reducing  
387 the reaction efficiency. In this study, the re-formation of lizardite upon carbonation of the activated  
388 materials was not observed as evidenced by the lack of its characteristic Raman, XRD, FTIR and  
389 TPD features upon carbonation.

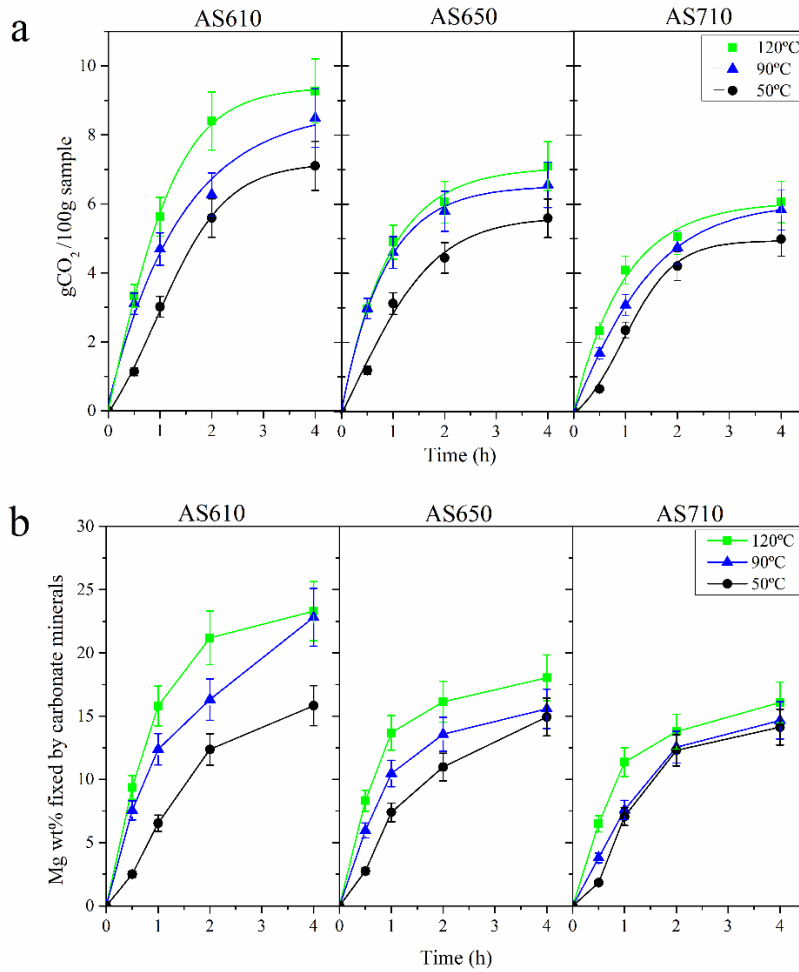
390 The reactivity towards mineral carbonation of activated serpentine is primarily due to its  
391 amorphous nature (Dlugogorski and Balucan, 2014; Mann, 2014; McKelvy et al., 2004). Du Breuil  
392 et al., 2019a quantified the intermediate phases that formed during activation of lizardite at  
393 different temperatures and reported that such values have a linear correlation with the obtained

394 carbonation efficiency upon reaction with CO<sub>2</sub>. In this study, the coexistence of HRAS and PRAS  
395 played a crucial role in the moist carbonation reactions, since it was consistently observed that the  
396 HRAS was the main or only phase that contributed to the formation of carbonates. On the other  
397 hand, PRAS remained unreacted upon carbonation. This observation provides important and novel  
398 insights for direct carbonation processes of activated serpentine. The formation of HRAS upon  
399 activation is desired since it is highly reactive even under moderately low pressures (6 bar; 120°C).  
400 Such pressure and temperature conditions are close to industrial flue gas emissions (Highfield et  
401 al., 2016; Rausis et al., 2020; Swanson et al., 2014). This strongly suggests that high pressures and  
402 temperatures are not required for the carbonation of this phase. On the other hand, PRAS can be  
403 considered as an undesired product of activation, since it is significantly less reactive than HRAS  
404 and also fixes a significant amount of Mg within its disordered silicate structure.

405 In this study, no evidence of forsterite carbonation was observed. This is consistent with previous  
406 observations where intermediate amorphous silicate phases (formed upon serpentine heat  
407 activation) are more reactive than forsterite. However, it has been reported that the carbonation of  
408 forsterite is partially unlocked at high pressures and temperatures (185°C and 150 bar) achieving  
409 even higher reactivity than for activated lizardite (Gerdemann et al., 2007).

### 410 3.3. Time resolved carbonation efficiency

411 The extent of carbonation (expressed as g CO<sub>2</sub> /100 g of sample), as well as the estimated Mg  
412 fraction fixed by carbonates based on TPD data (Figure S4, S5; see section S6) are shown in Figure  
413 6. Higher temperature pretreatments induced a lower carbonation yield. A maximum of 9.3g of  
414 CO<sub>2</sub> sequestered per 100 grams of sample was achieved at 120°C and 4h for AS610, which  
415 accounts to 23.3% of the available Mg fraction fixed by carbonates.



416

417 **Figure 6. (a)** Grams of CO<sub>2</sub> sequestered per 100 grams of sample, as estimated from TPD analysis.

418 **(b)** Amount of Mg fixed by carbonate minerals after carbonation of AS610, AS650 and AS710.

419 Error bars take into account the phase variability and the calculated data from three analogous

420 experiments.

421 The limited extraction of Mg from intermediate silicate phases upon carbonation implies that

422 the reaction has been partially inhibited during the studied timeframe. The coupled formation of

423 carbonates and amorphous silica plays an important role in the passivation of the reaction, as

424 previous studies have reported (Béarat et al., 2006; Benhelal et al., 2019a; Julcour et al., 2015).



425 The presence of magnetite and hematite may play a role in the passivation of the carbonation  
426 reactions, as previous work has discussed (Fauth et al., 2002; Mouedhen et al., 2017).

427 The lower carbonation yield observed for AS650 and AS710 relative to AS610 is probably due  
428 to undesired nucleation of forsterite from intermediate phases upon thermal activation, as has been  
429 extensively reported in previous studies (Dlugogorski and Balucan, 2014; Du Breuil et al., 2019;  
430 McKelvy et al., 2004). Moreover, the larger particle sizes of materials activated at 650 and 710°C  
431 and hence, lower overall surface area, probably contribute to their lower carbonation yield (Figure  
432 S1b). However, it has been reported that the reactivity of activated lizardite is likely to be more  
433 influenced by the mineralogy than by surface area (Du Breuil et al., 2019). In the context of this  
434 paper, the Mg fraction from AS710 that forms carbonates is only up to 7% lower than in the case  
435 of AS610, despite the significant higher yield of forsterite in the materials activated at 710°C. This  
436 might indicate that the nucleation of forsterite, despite reducing the carbonation yield, is not the  
437 main reason for the reduced carbonation yield of activated lizardite. On the other hand, undesired  
438 re-crystallization of lizardite was not observed upon carbonation. Therefore, the main limiting  
439 factor of the direct carbonation of activated lizardite is either attributed to the formation of  
440 passivating phases or there are limiting factors that are yet undefined.

441 Only one highly-reactive phase (HRAS) is formed upon thermal activation of lizardite (see  
442 section 3.2). The formation of both intermediate PRAS (this study) and Q<sup>3</sup> dehydroxylate II  
443 (Farhang et al., 2016) are undesired due to their low reactivity and they fix a significant fraction  
444 of available Mg. Moreover, the carbonation of HRAS results in the formation of carbonates as well  
445 as a Si-rich phase formed that might retained a fraction of Mg, which further limits the extent of  
446 reaction, aside from its characteristic passivating nature. These limiting factors, particularly the  
447 formation of PRAS, might be responsible for the yet unanswered limited carbonation efficiencies

448 obtained via direct aqueous and moist carbonation of lizardite. It may also provide important  
449 insights in the optimization of both activation and carbonation processes of activated lizardite.  
450 These limiting factors are considered to reduce the carbonation yield significantly more than the  
451 nucleation of forsterite in AS710 relative to AS610.

452 Bhardwaj et al., 2016 reported a rapid and limited direct moist carbonation of activated lizardite  
453 at low pressures and temperatures (1 bar, 65-95°C), sequestering a maximum of 7.5g of CO<sub>2</sub> per  
454 100g of sample. Similar results were also reported by Veetil et al., 2015 (7gCO<sub>2</sub>/100g sample)  
455 upon direct moist carbonation of activated lizardite, although at significantly higher temperature  
456 and pressure (200°C, 25bar). Such limited carbonation efficiencies are slightly lower than those  
457 obtained in this work. The reduced carbonation yields obtained in this study and those reported by  
458 Bhardwaj et al., 2016 and Veetil et al., 2015 are likely attributed to the limited abundance of HRAS  
459 in these activated serpentines.

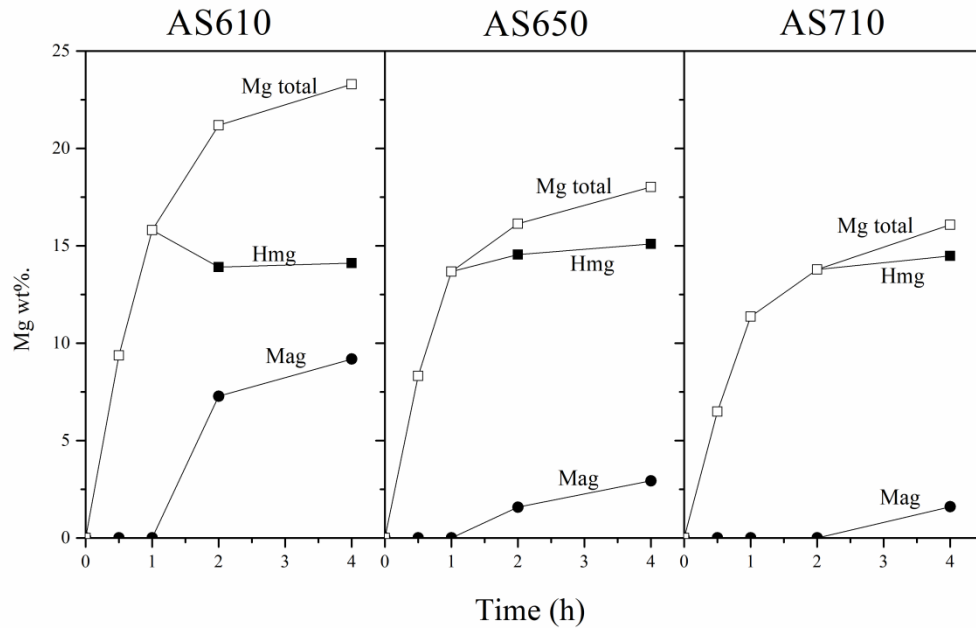
460 On the basis of these observations, activation processes for lizardite can be further optimized by  
461 adjusting activation temperature and residence time in order to (i) obtain a complete or almost  
462 complete transformation of lizardite as well as a complete transformation of Q<sup>3</sup> dehydroxylate II  
463 to amorphous intermediate Mg-rich silicate phases, (ii) increase the proportion of HRAS relative  
464 to PRAS (this study) and (iii) avoid the nucleation of forsterite and enstatite as well as particle  
465 sintering. This might be achieved by heat activating lizardite at 750°C for 15 min (Du Breuil et al.,  
466 2019) or at lower temperatures over prolonged residence times (610°C for ≤16h; this study).  
467 Carbonation and activation processes should be focused on minimizing the passivation effect due  
468 to undesired reactions and the formation of passivating layers (if possible). Moreover, the direct  
469 carbonation conditions at which these materials are tested could be significantly optimized by  
470 working at moderately low pressures (≤10 bar; see section S7).

471

### 472 3.3.1. Magnesite formation

473 The Mg wt% stored by hydromagnesite and magnesite was possible to estimate since the  
474 associated thermal decarbonation associated with those minerals (observed with TPD, Figure S4)  
475 were differentiated (Figure 7). Hydromagnesite formation reached a steady state at 1h for AS610  
476 and at 2h for AS650 and AS710, accounting to ~15% of the total available Mg in activated materials.  
477 This possibly indicates that some process is hindering the formation hydromagnesite, even if  
478 sufficient  $Mg^{2+}$ ,  $CO_2$  and  $H_2O$  are available. One possibility is that the reaction environment is  
479 saturated with respect to hydromagnesite. Magnesite only started forming once hydromagnesite  
480 formation had reached the steady state.

481 The formation of magnesite from direct aqueous carbonation requires relatively high temperatures  
482 ( $>100^\circ C$ ), elevated  $CO_2$  partial pressures ( $\sim 100$  bar) and/or extended reaction times (Hänchen et  
483 al., 2008; Hopkinson et al., 2012; Montes-Hernandez et al., 2012; Swanson et al., 2014). In this  
484 study, magnesite was observed to form at 2h of reaction at moderately low pressures and  
485 temperatures ( $120^\circ C$ , 6bar) upon AS610 direct moist carbonation. Our results suggest that the  
486 formation of magnesite is greatly accelerated once the formation of hydromagnesite reached a  
487 steady state and sufficient  $Mg^{2+}$  is available. Magnesite content was estimated to be lower for the  
488 higher temperature activated materials. This might be explained by the slower formation of  
489 hydromagnesite on such materials, delaying the time needed for hydromagnesite formation to  
490 reach the steady state.



491

492 **Figure 7.** Mg wt% stored in carbonate minerals after carbonation of AS610, AS650 and AS710  
 493 at 120°C, from 30 minutes to 4 hours. (Mg total) Mg wt%. that has been stored by both (Hmg)  
 494 hydromagnesite and (Mag) magnesite.

495 The formation of different carbonate phases under analogous experimental conditions among the  
 496 different activated-serpentines, suggest that the different relative proportion of HRAS relative to  
 497 PRAS among such materials plays a key role on the formation and evolution of Mg-carbonate  
 498 phases, as observed for the accelerated formation of magnesite as well as transition of nesquehonite  
 499 to dypingite-like phases and possibly to a hydrous AMC.

500

#### 501 4. Conclusions

502 This experimental study provides new insights on both the role that the intermediate phases of  
 503 three different meta-lizardites (pretreated at 610, 650 and 710°C) play during carbonation and the  
 504 formation of hydrated and anhydrous Mg-carbonates. The reaction temperature is the dominant  
 505 factor that controls the formation of the different carbonate phases and their hydration level. At

506 120°C, hydromagnesite and magnesite were identified. Magnesite only appeared when  
507 hydromagnesite formation reach a steady state, especially for the 610°C activated materials. This  
508 may suggest that magnesite formation might be accelerated once hydromagnesite formation  
509 reached an steady state and sufficient  $Mg^{2+}$  is available. At 90°C, probably nesquehonite (formed  
510 in less than 30 minutes) transformed into the identified dypingite-like phases and probably an  
511 amorphous carbonate phase. Nesquehonite remained untransformed from experiments performed  
512 at 50°C only for the 610°C activated materials. However, for the higher temperature activated  
513 materials (650 and 710°C), it was completely transformed (from 2 to 4 hours of reaction) into a  
514 highly-disordered dypingite and probably an amorphous carbonate phase.

515 Different carbonate phases were identified during analogous carbonation experiments between the  
516 three different activated materials, suggesting that the reacting materials play a key role in  
517 carbonate phase formation and evolution. This might be attributable to the possible coexistence of  
518 different amorphous Mg-rich silicate phases that were formed upon lizardite activation and the  
519 distribution of such phases depending on the activation temperature. It was found that two different  
520 amorphous Mg-rich silicate phases were formed upon activation. The amorphous phase associated  
521 with the  $888.1$  and  $626.3 \pm 3.5$   $cm^{-1}$  FTIR and Raman peak, respectively, is found to be highly-  
522 reactive, as this phase exclusively or mainly nourished the formation of carbonates. A complete  
523 carbonation of this phase could be obtained at moderately-low pressure and temperature conditions  
524 with reasonable conversion rates. The other amorphous phase, associated with the  $673 \pm 1.1$  and  
525  $1019 \pm 8.5$   $cm^{-1}$  FTIR and Raman peak, respectively, remains seemingly unreacted upon  
526 carbonation. The presence of this poorly-reactive phase might provide important insights to the  
527 yet unanswered question regarding the limited carbonation yield during direct carbonation of  
528 activated serpentine routes, since, upon activation and carbonation, it retains a significant fraction

529 of Mg within its disordered structure. Moreover, forsterite nucleation in the materials activated at  
530 710°C yielded **only up to** 7% decrease on the extracted Mg fraction to form carbonates when  
531 compared to the materials activated at 610°C. This strongly **suggests** that the nucleation of  
532 forsterite, despite reducing the carbonation yield, is not the main reason for the low carbonation  
533 yield via direct **moist** carbonation of activated lizardite.

534 Both activation and carbonation conditions should be optimized to increase the proportion of  
535 highly relative to poorly-reactive amorphous Mg-rich silicate phases, as well as to avoid undesired  
536 side reactions in order to unlock (if possible) the direct carbonation potential of activated lizardite.  
537 If such a process cannot be significantly further optimized, such as increasing the proportion of  
538 HRAS relative to PRAS during activation of lizardite, other routes for the carbonation of lizardite  
539 should be considered such as indirect carbonation processes of both activated and non-activated  
540 lizardite.

541

## 542 ACKNOWLEDGEMENTS

543 This work has been partially funded by the Government of Catalonia through the FI-2017  
544 program for the recruitment of early-stage researchers (K.R.). Contract number: 2017 FI\_B00129  
545 (K.R.). Authors are grateful to Prof. Joaquín Proenza (Universitat de Barcelona) who kindly  
546 provided the samples studied in this research. The authors gratefully acknowledge Prof. Alissa  
547 Park and Mr. Guanhi Rim for insightful discussions. Technical assistance in sample  
548 characterization of the reaction products by Drs. Trifon Trifonov and Montserrat Domínguez-  
549 Escalante, from the Barcelona Research Center in Multiscale Science and Engineering. Drs Jorge  
550 Molinero and Andrés Idiart from Amphos<sup>21</sup> Consulting S.L. España are gratefully acknowledged  
551 for their collaboration in the framework of the InnoEnergy PhD mobility program funding to A.C.

552 REFERENCES

- 553 Assima, G.P., Larachi, F., Beaudoin, G., Molson, J.W., 2012. CO<sub>2</sub> sequestration in chrysotile  
554 mining residues - Implication of watering and passivation under environmental conditions  
555 CO<sub>2</sub> sequestration in chrysotile mining residues - Implication of watering and passivation  
556 under environmental co. *Ind. Eng. Chem. Res.* 51, 8726–8734.  
557 <https://doi.org/10.1021/ie202693q>
- 558 Béarat, H., Mckelvy, M.J., Chizmeshya, A.V.G., Gormley, D., Nunez, R., Carpenter, R.W.,  
559 Squires, K., Wolf, G.H., 2006. Carbon sequestration via aqueous olivine mineral carbonation:  
560 Role of passivating layer formation. *Environ. Sci. Technol.* 40, 4802–4808.
- 561 Benhelal, E., Oliver, T.K., Farhang, F., Hook, J.M., Rayson, M.S., Brent, G.F., Stockenhuber, M.,  
562 Kennedy, E.M., 2019a. Structure of Silica Polymers and Reaction Mechanism for Formation  
563 of Silica-Rich Precipitated Phases in Direct Aqueous Carbon Mineralization. *Ind. Eng. Chem.*  
564 *Res.* <https://doi.org/10.1021/acs.iecr.9b04379>
- 565 Benhelal, E., Rashid, M.I., Rayson, M.S., Brent, G.F., Oliver, T., Stockenhuber, M., Kennedy,  
566 E.M., 2019b. Direct aqueous carbonation of heat activated serpentine: Discovery of  
567 undesirable side reactions reducing process efficiency. *Appl. Energy* 242, 1369–1382.  
568 <https://doi.org/10.1016/j.apenergy.2019.03.170>
- 569 Benhelal, E., Rashid, M.I., Rayson, M.S., Prigge, J.D., Molloy, S., Brent, G.F., Cote, A.,  
570 Stockenhuber, M., Kennedy, E.M., 2018. Study on mineral carbonation of heat activated  
571 lizardite at pilot and laboratory scale. *J. CO<sub>2</sub> Util.* 26, 230–238.  
572 <https://doi.org/10.1016/j.jcou.2018.05.015>
- 573 Bhardwaj, R., Van Ommen, J.R., Nugteren, H.W., Geerlings, H., 2016. Accelerating Natural CO<sub>2</sub>  
574 Mineralization in a Fluidized Bed. *Ind. Eng. Chem. Res.* 55, 2946–2951.  
575 <https://doi.org/10.1021/acs.iecr.5b04925>
- 576 Blue, C.R., Giuffre, A., Mergelsberg, S., Han, N., De Yoreo, J.J., Dove, P.M., 2017. Chemical and  
577 physical controls on the transformation of amorphous calcium carbonate into crystalline  
578 CaCO<sub>3</sub> polymorphs. *Geochim. Cosmochim. Acta* 196, 179–196.

579 <https://doi.org/10.1016/j.gca.2016.09.004>

580 Bobicki, E.R., Liu, Q., Xu, Z., Zeng, H., 2012. Carbon capture and storage using alkaline industrial  
581 wastes. *Prog. Energy Combust. Sci.* 38, 302–320. <https://doi.org/10.1016/j.pecs.2011.11.002>

582 Canterford, J., Tsambourakis, G., Lambert, B., 1984. Some observations on the properties of  
583 dypingite,  $Mg_5(CO_3)_4(OH)_2 \cdot 5H_2O$ , and related minerals. *Mineral. Mag.* 48, 437–442.

584 Casey, W.H., Westrich, H.R., Arnold, G.W., 1988. Surface chemistry of labradorite feldspar  
585 reacted with aqueous solutions at pH = 2, 3, and 12. *Geochim. Cosmochim. Acta* 52, 2795–  
586 2807. [https://doi.org/https://doi.org/10.1016/0016-7037\(88\)90147-0](https://doi.org/https://doi.org/10.1016/0016-7037(88)90147-0)

587 Chizmeshya, A.V.G., Mckelvy, M.J., Sharma, R., Carpenter, R.W., Bearat, H., 2002. Density  
588 functional theory study of the decomposition of  $Mg(OH)_2$ : a lamellar dehydroxylation model.  
589 *Mater. Chem. Phys.* 77, 416–425.

590 Chizmeshya, A.V.G., McKelvy, M.J., Wolf, G.H., Carpenter, R.W., Gormley, D., Diefenbacher,  
591 J., Marzke, R., 2006. Enhancing the atomic-level understanding of CO<sub>2</sub> mineral sequestration  
592 mechanisms via advanced computational modeling.

593 Daval, D., Sissmann, O., Menguy, N., Saldi, G.D., Guyot, F., Martinez, I., Corvisier, J., Garcia,  
594 B., Machouk, I., Knauss, K.G., Hellmann, R., 2011. Influence of amorphous silica layer  
595 formation on the dissolution rate of olivine at 90°C and elevated pCO<sub>2</sub>. *Chem. Geol.* 284,  
596 193–209. <https://doi.org/https://doi.org/10.1016/j.chemgeo.2011.02.021>

597 Davies, P.J., Bubela, B., 1973. The transformation of nesquehonite into hydromagnesite. *Chem.*  
598 *Geol.* 12, 289–300. [https://doi.org/10.1016/0009-2541\(73\)90006-5](https://doi.org/10.1016/0009-2541(73)90006-5)

599 Deelman, J.C., 2001. Breaking Ostwald’s Rule. *Chemie der Erde* 61, 224–235.

600 Dlugogorski, B.Z., Balucan, R.D., 2014. Dehydroxylation of serpentine minerals: Implications for  
601 mineral carbonation. *Renew. Sustain. Energy Rev.* 31, 353–367.  
602 <https://doi.org/10.1016/j.rser.2013.11.002>

603 Du Breuil, C., Pasquier, L.C., Dipple, G., Blais, J.F., Iliuta, M.C., Mercier, G., 2019. Mineralogical



604 transformations of heated serpentine and their impact on dissolution during aqueous-phase  
605 mineral carbonation reaction in flue gas conditions. *Minerals* 9, 1–14.  
606 <https://doi.org/10.3390/min9110680>

607 Dufaud, F., Martinez, I., Shilobreeva, S., 2009. Experimental study of Mg-rich silicates  
608 carbonation at 400 and 500 °C and 1 kbar. *Chem. Geol.* 265, 79–87.  
609 <https://doi.org/10.1016/j.chemgeo.2009.01.026>

610 Edwards, H.G.M., Villar, S.E.J., Jehlicka, J., Munshi, T., 2005. FT-Raman spectroscopic study of  
611 calcium-rich and magnesium-rich carbonate minerals. *Spectrochim. Acta - Part A Mol.*  
612 *Biomol. Spectrosc.* 61, 2273–2280. <https://doi.org/10.1016/j.saa.2005.02.026>

613 Eloneva, S., Said, A., Fogelholm, C., Zevenhoven, R., 2012. Preliminary assessment of a method  
614 utilizing carbon dioxide and steelmaking slags to produce precipitated calcium carbonate.  
615 *Appl. Energy* 90, 329–334. <https://doi.org/10.1016/j.apenergy.2011.05.045>

616 Fagerlund, J., Highfield, J., Zevenhoven, R., 2012. Kinetics studies on wet and dry gas – solid  
617 carbonation of MgO and Mg(OH)<sub>2</sub> for CO<sub>2</sub> sequestration. *RSC Adv.* 10380–10393.  
618 <https://doi.org/10.1039/c2ra21428h>

619 Farhang, F., Oliver, T.K., Rayson, M., Brent, G., Stockenhuber, M., Kennedy, E., 2016.  
620 Experimental study on the precipitation of magnesite from thermally activated serpentine for  
621 CO<sub>2</sub> sequestration. *Chem. Eng. J.* 303, 439–449. <https://doi.org/10.1016/j.cej.2016.06.008>

622 Farhang, F., Rayson, M., Brent, G., Hodgins, T., Stockenhuber, M., Kennedy, E., 2017. Insights  
623 into the dissolution kinetics of thermally activated serpentine for CO<sub>2</sub> sequestration. *Chem.*  
624 *Eng. J.* 330, 1174–1186. <https://doi.org/10.1016/j.cej.2017.08.073>

625 Fauth, D.J., Baltrus, J.P., Soong, Y., Knoer, J.P., Howard, B.H., Graham, W.J., Maroto-Valer,  
626 M.M., Andrésen, J.M., 2002. Carbon Storage and Sequestration as Mineral Carbonates, in:  
627 Maroto-Valer, M.M., Song, C., Soong, Y. (Eds.), *Environmental Challenges and Greenhouse*  
628 *Gas Control for Fossil Fuel Utilization in the 21st Century*. Springer US, Boston, MA, pp.  
629 101–117. [https://doi.org/10.1007/978-1-4615-0773-4\\_8](https://doi.org/10.1007/978-1-4615-0773-4_8)

630 Felmy, A.R., Qafoku, O., Arey, B.W., Hu, J.Z., Hu, M., Schaefer, H.T., Ilton, E.S., Hess, N.J.,

631 Pearce, C.I., Feng, J., Rosso, K.M., 2012. Reaction of water-saturated supercritical CO<sub>2</sub> with  
632 forsterite : Evidence for magnesite formation at low temperatures. *Geochim. Cosmochim.*  
633 *Acta* 91, 271–282. <https://doi.org/10.1016/j.gca.2012.05.026>

634 Fricker, K.J., Park, A.A., 2013. Effect of H<sub>2</sub>O on Mg(OH)<sub>2</sub> carbonation pathways for combined  
635 CO<sub>2</sub> capture and storage. *Chem. Eng. Sci.* 100, 332–341.  
636 <https://doi.org/10.1016/j.ces.2012.12.027>

637 Fricker, K.J., Park, A.H.A., 2014. Investigation of the different carbonate phases and their  
638 formation kinetics during Mg(OH)<sub>2</sub> slurry carbonation. *Ind. Eng. Chem. Res.* 53, 18170–  
639 18179. <https://doi.org/10.1021/ie503131s>

640 Frost, R.L., 2011. Raman spectroscopic study of the magnesium carbonate mineral  
641 hydromagnesite (Mg 5[(CO 3) 4(OH) 2]·4H 2O). *J. Raman Spectrosc.* 42, 1690–1694.  
642 <https://doi.org/10.1002/jrs.2917>

643 Fukushi, K., Suzuki, Y., Kawano, J., Ohno, T., Ogawa, M., Yaji, T., Takahashi, Y., 2017.  
644 Speciation of magnesium in monohydrocalcite: XANES, ab initio and geochemical modeling.  
645 *Geochim. Cosmochim. Acta* 213, 457–474. <https://doi.org/10.1016/j.gca.2017.06.040>

646 Gadikota, G., Matter, J., Kelemen, P., Park, A.A., 2014. Chemical and morphological changes  
647 during olivine carbonation for CO<sub>2</sub> storage in the presence of NaCl and NaHCO<sub>3</sub>. *Phys.*  
648 *Chem. Chem. Phys.* 16, 4679. <https://doi.org/10.1039/c3cp54903h>

649 Gerdemann, S.J., O’Connor, W.K., Dahlin, D.C.D.C., Penner, L.R., Rush, H., O’Conor, W.K.,  
650 Dahlin, D.C.D.C., Penner, L.R., Rush, H., 2007. Ex situ aqueous mineral carbonation.  
651 *Environ. Sci. Technol.* 41, 2589–2593. <https://doi.org/10.1021/es0619253>

652 Giammar, D.E., Bruant, R.G., Peters, C.A., 2005. Forsterite dissolution and magnesite  
653 precipitation at conditions relevant for deep saline aquifer storage and sequestration of carbon  
654 dioxide. *Chem. Geol.* 217, 257–276. <https://doi.org/10.1016/j.chemgeo.2004.12.013>

655 Hänchen, M., Prigiobbe, V., Baciocchi, R., Mazzotti, M., 2008. Precipitation in the Mg-carbonate  
656 system—effects of temperature and CO<sub>2</sub> pressure. *Chem. Eng. Sci.* 63, 1012–1028.  
657 <https://doi.org/10.1016/J.CES.2007.09.052>

658 Hao, Z., Du, F., 2009. Synthesis of basic magnesium carbonate microrods with a “house of cards”  
659 surface structure using rod-like particle template. *J. Phys. Chem. Solids* 70, 401–404.  
660 <https://doi.org/10.1016/j.jpcs.2008.11.005>

661 Harrison, A.L., Power, I.M., Dipple, G.M., 2013. Accelerated carbonation of brucite in mine  
662 tailings for carbon sequestration. *Environ. Sci. Technol.* 47, 126–134.  
663 <https://doi.org/10.1021/es3012854>

664 Hellmann, R., Eggleston, C.M., Hochella, M.F., Crerar, D.A., 1990. The formation of leached  
665 layers on albite surfaces during dissolution under hydrothermal conditions. *Geochim.*  
666 *Cosmochim. Acta* 54, 1267–1281. [https://doi.org/https://doi.org/10.1016/0016-](https://doi.org/https://doi.org/10.1016/0016-7037(90)90152-B)  
667 [7037\(90\)90152-B](https://doi.org/https://doi.org/10.1016/0016-7037(90)90152-B)

668 Highfield, J., Chen, J., Haghightlari, M., Abacka, J., Zevenhoven, R., 2016. Low-temperature  
669 gas-solid carbonation of magnesia and magnesium hydroxide promoted by non-immersive  
670 contact with water. *RSC Adv.* 6, 89655–89664. <https://doi.org/10.1039/C6RA16328A>

671 Hopkinson, L., Kristova, P., Rutt, K., Cressey, G., 2012. Phase transitions in the system MgO-  
672 CO<sub>2</sub>-H<sub>2</sub>O during CO<sub>2</sub> degassing of Mg-bearing solutions. *Geochim. Cosmochim. Acta* 76, 1–  
673 13. <https://doi.org/10.1016/j.gca.2011.10.023>

674 Hopkinson, L., Rutt, K., Cressey, G., 2008. The Transformation of Nesquehonite to  
675 Hydromagnesite in the System CaO-MgO-H<sub>2</sub>O-CO<sub>2</sub>: An Experimental Spectroscopic  
676 Study. *J. Geol.* 116, 387–400. <https://doi.org/10.1086/588834>

677 Hövelmann, J., Putnis, C. V., Ruiz-Agudo, E., Austrheim, H., 2012. Direct nanoscale observations  
678 of CO<sub>2</sub> sequestration during brucite [Mg(OH)<sub>2</sub>] dissolution. *Environ. Sci. Technol.* 46, 5253–  
679 5260. <https://doi.org/10.1021/es300403n>

680 Huijgen, W.J.J., Comans, R.N.J., Witkamp, G.J., 2007. Cost evaluation of CO<sub>2</sub> sequestration by  
681 aqueous mineral carbonation. *Energy Convers. Manag.* 48, 1923–1935.  
682 <https://doi.org/10.1016/j.enconman.2007.01.035>

683 Julcour, C., Bourgeois, F., Bonfils, B., Benhamed, I., Guyot, F., Bodéan, F., Petiot, C., Gaucher,  
684 É.C., 2015. Development of an attrition-leaching hybrid process for direct aqueous mineral

685 carbonation. *Chem. Eng. J.* 262, 716–726. <https://doi.org/10.1016/j.cej.2014.10.031>

686 Kelemen, P.B., Matter, J., 2008. In situ carbonation of peridotite for CO<sub>2</sub> storage. *Proc. Natl. Acad.*  
687 *Sci. U. S. A.* 105, 17295–17300. <https://doi.org/10.1073/pnas.0805794105>

688 Lackner, K.S., 2003. A Guide to CO<sub>2</sub> Sequestration. *Science* (80-. ). 300, 1677–1678.

689 Lackner, K.S., Wendt, C.H., Butt, D.P., Joyce, E.L., Sharp, D.H., 1995. Carbon dioxide disposal  
690 in carbonate minerals. *Energy* 20, 1153–1170. [https://doi.org/10.1016/0360-5442\(95\)00071-](https://doi.org/10.1016/0360-5442(95)00071-N)  
691 N

692 Lafay, R., Montes-Hernandez, G., Janots, E., Chiriac, R., Findling, N., Toche, F., 2014.  
693 Simultaneous precipitation of magnesite and lizardite from hydrothermal alteration of olivine  
694 under high-carbonate alkalinity. *Chem. Geol.* 368, 63–75.  
695 <https://doi.org/10.1016/j.chemgeo.2014.01.008>

696 Larachi, F., Daldoul, I., Beaudoin, G., 2010. Fixation of CO<sub>2</sub> by chrysotile in low-pressure dry and  
697 moist carbonation: Ex-situ and in-situ characterizations. *Geochim. Cosmochim. Acta* 74,  
698 3051–3075. <https://doi.org/10.1016/J.GCA.2010.03.007>

699 Li, J., Hitch, M., Power, I.M., Pan, Y., 2018. Integrated mineral carbonation of ultramafic mine  
700 deposits—A review. *Minerals* 8, 1–18. <https://doi.org/10.3390/min8040147>

701 Li, Wenzhi, Li, Wen, Li, B., Bai, Z., 2009. Electrolysis and heat pretreatment methods to promote  
702 CO<sub>2</sub> sequestration by mineral carbonation. *Chem. Eng. Res. Des.* 87, 210–215.  
703 <https://doi.org/10.1016/j.cherd.2008.08.001>

704 Linga, P., Kumar, R., Englezos, P., 2007. The Clathrate Hydrate Process for Post and Pre-  
705 combustion Capture of Carbon Dioxide. *J. Hazard. Mater.* 149, 625–629.  
706 <https://doi.org/10.1016/j.jhazmat.2007.06.086>

707 Loring, J.S., Thompson, C.J., Zhang, C., Wang, Z., Schaef, H.T., Rosso, K.M., 2012. In situ  
708 infrared spectroscopic study of brucite carbonation in dry to water-saturated supercritical  
709 carbon dioxide. *J. Phys. Chem. A* 116, 4768–77. <https://doi.org/10.1021/jp210020t>

710 Mann, J., 2014. Serpentine Activation for CO<sub>2</sub> Sequestration. Thesis Disertation. The University  
711 of Sideny.

712 Marchesi, C., Garrido, C.J., Proenza, J.A., Hidas, K., Varas-Reus, M.I., Butjosa, L., Lewis, J.F.,  
713 2016. Geochemical record of subduction initiation in the sub-arc mantle: Insights from the  
714 Loma Caribe peridotite (Dominican Republic). *Lithos* 252–253, 1–15.  
715 <https://doi.org/10.1016/j.lithos.2016.02.009>

716 Maroto-Valer, M.M., Fauth, D.J., Kuchta, M.E., Zhang, Y., Andrésen, J.M., 2005. Activation of  
717 magnesium rich minerals as carbonation feedstock materials for CO<sub>2</sub> sequestration. *Fuel*  
718 *Process. Technol.* 86, 1627–1645. <https://doi.org/10.1016/j.fuproc.2005.01.017>

719 McKelvy, M.J., Chizmeshya, A.V.G., Diefenbacher, J., Béarat, H., Wolf, G., 2004. Exploration of  
720 the role of heat activation in enhancing serpentine carbon sequestration reactions. *Environ.*  
721 *Sci. Technol.* 38, 6897–6903. <https://doi.org/10.1021/es049473m>

722 Montes-Hernandez, G., Renard, F., Chiriac, R., Findling, N., Toche, F., 2012. Rapid precipitation  
723 of magnesite from Mg(OH)<sub>2</sub>-H<sub>2</sub>O-CO<sub>2</sub> slurry enhanced by NaOH and heat-ageing step (from  
724 20 to 90°C). *Cryst. Growth Des.* 12, 5233–5240.

725 Morse, J., Casey, W., 1988. Ostwald processes and mineral paragenesis in sediments. *Am. J. Sci.*  
726 288, 537–560.

727 Mouedhen, I., Kemache, N., Pasquier, L.C., Cecchi, E., Blais, J.F., Mercier, G., 2017. Effect of  
728 pCO<sub>2</sub> on direct flue gas mineral carbonation at pilot scale. *J. Environ. Manage.* 198, 1–8.  
729 <https://doi.org/10.1016/j.jenvman.2017.04.048>

730 Park, A.-H.A., Fan, L.-S., 2004. CO<sub>2</sub> mineral sequestration: physically activated dissolution of  
731 serpentine and pH swing process. *Chem. Eng. Sci.* 59, 5241–5247.  
732 <https://doi.org/10.1016/J.CES.2004.09.008>

733 Pasquier, L.C., Mercier, G., Blais, J.F., Cecchi, E., Kentish, S., 2014. Reaction mechanism for the  
734 aqueous-phase mineral carbonation of heat-activated serpentine at low temperatures and  
735 pressures in flue gas conditions. *Environ. Sci. Technol.* 48, 5163–5170.  
736 <https://doi.org/10.1021/es405449v>

737 Power, I.M., Dipple, G.M., Bradshaw, P.M.D., Harrison, A.L., 2020. Prospects for CO<sub>2</sub>  
738 mineralization and enhanced weathering of ultramafic mine tailings from the Baptiste nickel  
739 deposit in British Columbia, Canada. *Int. J. Greenh. Gas Control* 94, 102895.  
740 <https://doi.org/10.1016/j.ijggc.2019.102895>

741 Power, I.M., Dipple, G.M., Southam, G., 2010. Bioleaching of ultramafic tailings by  
742 *Acidithiobacillus* spp. for CO<sub>2</sub> sequestration. *Environ. Sci. Technol.* 44, 456–462.  
743 <https://doi.org/10.1021/es900986n>

744 Power, I.M., Harrison, A.L., Dipple, G.M., 2016. Accelerating Mineral Carbonation Using  
745 Carbonic Anhydrase. *Environ. Sci. Technol.* 50, 2610–2618.  
746 <https://doi.org/10.1021/acs.est.5b04779>

747 Power, I.M., Harrison, A.L., Dipple, G.M., Wilson, S., Kelemen, P.B., Hitch, M., Southam, G.,  
748 2013. Carbon Mineralization : From Natural Analogues to Engineered Systems From Natural  
749 Analogues to Engineered Systems. *Rev. Mineral. Geochemistry*.  
750 <https://doi.org/10.2138/rmg.2013.77.9>

751 Power, I.M., Harrison, A.L., Dipple, G.M., Wilson, S.A., Barker, S.L.L., Fallon, S.J., 2019.  
752 Magnesite formation in playa environments near Atlin, British Columbia, Canada. *Geochim.*  
753 *Cosmochim. Acta* 255, 1–24. <https://doi.org/10.1016/j.gca.2019.04.008>

754 Prigiobbe, V., Hänchen, M., Werner, M., Baciocchi, R., Mazzotti, M., 2009. Mineral carbonation  
755 process for CO<sub>2</sub> sequestration. *Energy Procedia* 1, 4885–4890.  
756 <https://doi.org/10.1016/j.egypro.2009.02.318>

757 Prigiobbe, V., Mazzotti, M., 2013. Precipitation of Mg-carbonates at elevated temperature and  
758 partial pressure of CO<sub>2</sub>. *Chem. Eng. J.* 223, 755–763.  
759 <https://doi.org/10.1016/j.cej.2013.03.033>

760 Pronost, J., Beaudoin, G., Lemieux, J.M., Hébert, R., Constantin, M., Marcouiller, S., Klein, M.,  
761 Duchesne, J., Molson, J.W., Larachi, F., Maldague, X., 2012. CO<sub>2</sub>-depleted warm air venting  
762 from chrysotile milling waste (Thetford Mines, Canada): Evidence for in-situ carbon capture  
763 from the atmosphere. *Geology* 40, 275–278. <https://doi.org/10.1130/G32583.1>

- 764 Rausis, K., Ćwik, A., Casanova, I., 2020. Phase evolution during accelerated CO<sub>2</sub> mineralization  
765 of brucite under concentrated CO<sub>2</sub> and simulated flue gas conditions. *J. CO<sub>2</sub> Util.* 37, 122–  
766 133. <https://doi.org/10.1016/j.jcou.2019.12.007>
- 767 Rigopoulos, I., Petallidou, K.C., Vasiliades, M.A., Delimitis, A., Ioannou, I., Efstathiou, A.M.,  
768 Kyratsi, T., 2015. Carbon Dioxide storage in Olivine Basalts : Effect of Ball Milling Process.  
769 *Powder Technol.* 273, 220–229. <https://doi.org/10.1016/j.powtec.2014.12.046>
- 770 Sanna, A., Hall, M.R., Maroto-Valer, M., 2012. Post-processing pathways in carbon capture and  
771 storage by mineral carbonation (CCSM) towards the introduction of carbon neutral materials.  
772 *Energy Environ. Sci.* 5, 7781. <https://doi.org/10.1039/c2ee03455g>
- 773 Schaef, H., McGrail, B., Loring, J., Bowden, M., Arey, B., Rosso, K.M., 2013. Forsterite  
774 [Mg<sub>2</sub>SiO<sub>4</sub>] Carbonation in wet supercritical CO<sub>2</sub>: An in Situ High-Pressure X-ray Diffraction  
775 Study. *Environ. Sci. Technol.* 47, 174–181.
- 776 Sipilä, J., Teir, S., Zevenhoven, R., 2008. Carbon Dioxide Sequestration by Mineral Carbonation :  
777 Literature Review Update 2005-2007, Report for Faculty of Technology Heat Engineering  
778 Laboratory. Turku, Finland.
- 779 Swanson, E.J., Fricker, K.J., Sun, M., Park, A.H.A., 2014. Directed precipitation of hydrated and  
780 anhydrous magnesium carbonates for carbon storage. *Phys. Chem. Chem. Phys.* 16, 23440–  
781 23450. <https://doi.org/10.1039/c4cp03491k>
- 782 Taifan, W., Boily, J., Baltrusaitis, J., 2016. Surface chemistry of carbon dioxide revisited. *Surf.*  
783 *Sci. Rep.* 71, 595–671. <https://doi.org/10.1016/j.surfrep.2016.09.001>
- 784 Thom, J.G.M., Dipple, G.M., Power, I.M., Harrison, A.L., 2013. Chrysotile dissolution rates:  
785 Implications for carbon sequestration. *Appl. Geochemistry* 35, 244–254.  
786 <https://doi.org/10.1016/j.apgeochem.2013.04.016>
- 787 Tran, T.N., Pham, T.V.A., Le, M.L.P., Nguyen, T.P.T., Tran, V.M., 2013. Synthesis of amorphous  
788 silica and sulfonic acid functionalized silica used as reinforced phase for polymer electrolyte  
789 membrane. *Adv. Nat. Sci. Nanosci. Nanotechnol.* 4. [https://doi.org/10.1088/2043-  
790 6262/4/4/045007](https://doi.org/10.1088/2043-6262/4/4/045007)

791 Turvey, C.C., Wilson, S.A., Hamilton, J.L., Tait, A.W., McCutcheon, J., Beinlich, A., Fallon, S.J.,  
792 Dipple, G.M., Southam, G., 2018. Hydrotalcites and hydrated Mg-carbonates as carbon sinks  
793 in serpentinite mineral wastes from the Woodsreef chrysotile mine, New South Wales,  
794 Australia: Controls on carbonate mineralogy and efficiency of CO<sub>2</sub> air capture in mine  
795 tailings. *Int. J. Greenh. Gas Control* 79, 38–60. <https://doi.org/10.1016/j.ijggc.2018.09.015>

796 Veetil, S.P., Pasquier, L., Blais, J., 2015. Direct gas – solid carbonation of serpentinite residues in  
797 the absence and presence of water vapor : a feasibility study for carbon dioxide sequestration.  
798 *Environ. Sci. Pollut. Res.* 22, 13486–13495. <https://doi.org/10.1007/s11356-015-4580-x>

799 Werner, M., Hariharan, S., Mazzotti, M., 2014. Flue gas CO<sub>2</sub> mineralization using thermally  
800 activated serpentine: From single- to double-step carbonation. *Phys. Chem. Chem. Phys.* 16,  
801 24978–24993. <https://doi.org/10.1039/c4cp02786h>

802 Werner, M., Hariharan, S.B., Bortolan, A. V., Zingaretti, D., Baciocchi, R., Mazzotti, M., 2013.  
803 Carbonation of activated serpentine for direct flue gas mineralization. *Energy Procedia* 37,  
804 5929–5937. <https://doi.org/10.1016/j.egypro.2013.06.519>

805 Wilson, S.A., Harrison, A.L., Dipple, G.M., Power, I.M., Barker, S.L.L., Ulrich Mayer, K., Fallon,  
806 S.J., Raudsepp, M., Southam, G., 2014. Offsetting of CO<sub>2</sub> emissions by air capture in mine  
807 tailings at the Mount Keith Nickel Mine, Western Australia: Rates, controls and prospects for  
808 carbon neutral mining. *Int. J. Greenh. Gas Control* 25, 121–140.  
809 <https://doi.org/10.1016/j.ijggc.2014.04.002>

810 Zarandi, A., Larachi, F., Beaudoin, G., Plante, B., Sciortino, M., 2017a. Ambient mineral  
811 carbonation of different lithologies of mafic to ultramafic mining wastes/tailings – A  
812 comparative study. *Int. J. Greenh. Gas Control* 63, 392–400.  
813 <https://doi.org/10.1016/j.ijggc.2017.06.016>

814 Zarandi, A., Larachi, F., Beaudoin, G., Plante, B., Sciortino, M., 2017b. Nesquehonite as a carbon  
815 sink in ambient mineral carbonation of ultramafic mining wastes. *Chem. Eng. J.* 314, 160–  
816 168. <https://doi.org/10.1016/j.cej.2017.01.003>

817 Zevenhoven, R., Teir, S., Eloneva, S., 2008. Heat optimisation of a staged gas – solid mineral



818 carbonation process for long-term CO<sub>2</sub> storage. *Energy* 33, 362–370.  
819 <https://doi.org/10.1016/j.energy.2007.11.005>

820 Zhao, L., Sang, L., Jun, C., Ji, J., Teng, H.H., 2010. Aqueous carbonation of natural brucite:  
821 Relevance to CO<sub>2</sub> sequestration. *Environ. Sci. Technol.* 44, 406–411.  
822 <https://doi.org/10.1021/es9017656>

823 Zou, Z., Habraken, W.J.E.M., Matveeva, G., Jensen, A.C.S., Bertinetti, L., Hood, M.A., Sun, C.,  
824 Gilbert, P.U.P.A., Polishchuk, I., Pokroy, B., Mahamid, J., Politi, Y., Weiner, S., Werner, P.,  
825 Bette, S., Dinnebier, R., Kolb, U., Zolotoyabko, E., Fratzl, P., 2019. A hydrated crystalline  
826 calcium carbonate phase: Calcium carbonate hemihydrate. *Science* (80-. ). 363, 396–400.  
827 <https://doi.org/10.1126/science.aav0210>

828

829