

Outstanding Methane Oxidation Performance of Pd-Embedded Ceria Catalysts Prepared by a One-step Dry Ball-Milling Method

Maila Danielis,[a] Sara Colussi,[a] Carla de Leitenburg,[a] Lluís Soler,[b] Jordi Llorca,[b] and Alessandro Trovarelli*[a]

[a] M. Danielis, dr. S. Colussi, prof. C. de Leitenburg, prof. A. Trovarelli

Polytechnic Department. University of Udine. Via del Cotonificio 108, 33100 Udine, Italy

[b] dr. L. Soler, prof. J. Llorca

Institute of Energy Technologies, Department of Chemical Engineering and Barcelona Research Centre in Multiscale Science and Engineering. Universitat Politècnica de Catalunya, EEBE. Eduard Maristany 10-14, 08019 Barcelona, Spain

Abstract: By carefully mixing Pd metal nanoparticles with CeO₂ polycrystalline powder under dry conditions a new unpredicted arrangement of the Pd-O-Ce interface is obtained, where an amorphous shell containing Palladium species dissolved in Ceria is covering a core of CeO₂ particles. The robust contact that is generated at nanoscale, along with mechanical forces generated during mixing, promotes the redox exchange between Pd and CeO₂ and creates highly reactive and stable sites constituted by PdO_x embedded into CeO₂ surface layers. This specific arrangement outperforms conventional Pd/CeO₂ reference catalysts in methane oxidation, by lowering light-off temperature by more than 50 degrees and boosting reaction rate. The origin of the outstanding activity is traced back to the structural properties of the interface, modified at nanoscale by mechano-chemical interaction, and it is unraveled by a combined set of experimental data including high resolution transmission electron microscopy and supported by recent computational studies.

The increasing concern over the abundant emissions of greenhouse gases from motor vehicles is pushing towards the development of more efficient catalysts for their abatement. This is particularly true for natural gas fueled vehicles, for which the exponential growth of the market and the concern for methane global warming potential urge for the design of catalytic systems with improved activity at low temperature and higher resistance to deactivation under operating conditions.[1] An efficient low temperature activation of the CH₄ molecule would also be a significant advancement in the field of methane utilization, an issue that is now attracting several efforts due to the increased supplies of shale gas and the consequent availability of natural gas as a feedstock.[2] Pd-based formulations are the most effective for methane oxidation, and the use of ceria as support confers additional benefits to the catalysts due to its unique redox features and to the level of Pd-Ce interfacial interactions.[3] It is reported from experimental[3b, 4] and computational[5] studies that an enhanced Pd-ceria interaction can improve significantly the catalytic activity of these materials. In particular, the presence of Pd into ceria lattice can lead to the formation of highly reactive Pd^{2+/4+} sites which show lower methane activation barriers compared to isolated PdO_x units. Interestingly, differently from what happens on PdO_x clusters, on these ionic Pd species methane activation proceeds via hydrogen abstraction, a route that is potentially very important for methane utilization.[5a]

We have already reported the increased activity of a Pd/CeO₂ catalyst prepared by solution combustion synthesis in which the substitution of Pd²⁺ ions into ceria lattice caused the formation of ordered arrays of oxygen vacancies and highly reactive undercoordinated oxygen atoms.[6] More recently we also investigated the milling of CeO₂-based materials with carbon, originating a 2D carbon layer, covering the ceria particles, and improving the interfacial redox

exchange between the two materials.[7] Here, by combining the above mentioned approaches, we use a controlled one-step dry milling procedure where Pd metal nanoparticles are put in contact with ceria particles to prepare a methane oxidation catalyst that outperforms traditional Pd/CeO₂ due to the unique structural arrangements that characterize metal/support interface at nanoscale. In addition, avoiding the use of Pd nitrate or chloride solution significantly reduces waste generation ensuring lower environmental impact. The characteristics of the preparation method, the properties and performances of the catalyst have been investigated in detail; the data suggest a correlation between the unusual morphology developed at nanoscale and the high catalytic activity observed, and this correlation is supported by most recent theoretical simulations.[5]

The mechanically mixed samples (denoted with M) were prepared by mixing together metallic Pd nanoparticles with CeO₂ powder aged at 1173 K in a mini ball mill, to obtain a nominal Pd loading of 1% wt. (PdCeM). Reference catalysts with the same nominal Pd loading were also synthesized by incipient wetness impregnation on the same CeO₂ support (PdCeIW) and by solution combustion synthesis (PdCeSCS). An additional catalyst, where PdO nanoparticles were used in substitution of Pd metal in the milling procedure, was also prepared for comparison (PdOCeM). To check the effect of the support, comparison of PdCeM with Pd supported on ZrO₂ (PdZrM) prepared by the same procedure was also carried out. The details on samples preparation and the milling parameters are reported in the Supporting Information, along with the detailed description of testing conditions and characterization methods. Stability under reaction conditions and durability were tested in comparison to PdCeIW following six reaction cycles up to 1173 K and monitoring time on stream behavior also under hydrothermal conditions. Comparison of X-ray diffraction and temperature programmed reduction profiles of PdCeM, PdCeIW and PdOCeM are reported in Figure S1 and S2. The light-off curves of methane combustion under lean atmosphere for the different Pd-ceria formulations are shown in Figure 1, along with the corresponding cooling part of the cycle.

In these experiments the catalysts were cycled under reaction conditions between room temperature and 1173 K for 2 heating/cooling cycles and the second cycle was selected as representative of the catalytic behavior, unless otherwise stated. Interestingly, the overall performance of the M samples strongly depends on the nature of the palladium precursor. PdCeM has a much higher activity than PdOCeM in the whole temperature range, and its behavior outperforms significantly that of the impregnated sample and of the catalyst made by solution combustion synthesis, which was reported as one of the best literature examples.[3b, 6] This can be seen either by the lower light-off temperature or by the higher reaction rate measured for the PdCeM sample in a recycle reactor, as reported in Table 1.

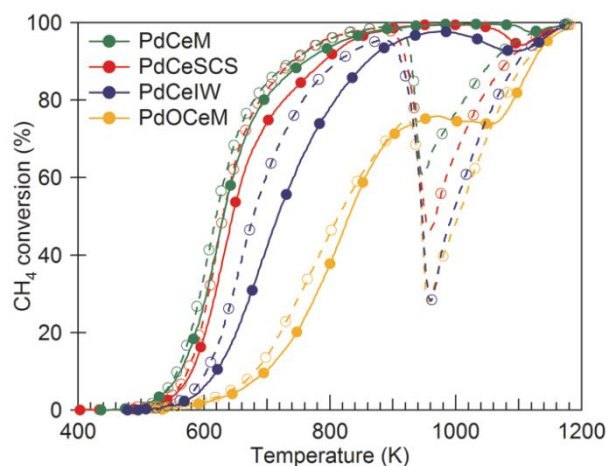


Figure 1. Light-off curves for Pd-CeO₂ catalysts (2nd cycle). Solid line, closed symbols: heating part of the cycle; dashed line, open symbols: cooling part of the cycle. Conditions: GHSV ca. 200000 h⁻¹, 0.5% CH₄, 2% O₂, He to balance.

Table 1. Physico-chemical properties and activity parameters for methane combustion.

Table 1. Physico-chemical properties and activity parameters for methane combustion.

Sample	Pd loading (wt%) ^[a]	Surface area (m ² /g)	T10 ^[b] (K)	Reaction rate ^[c] (μmol/g _{Pd} *s)
PdCeM	0.81	3.2	564	208
PdOCeM	0.80	4.1	700	16
PdCeIW	0.97	2.3	619	32
PdCeSCS	0.93	5.9	581	112

[a] measured by ICP elemental analysis; [b] temperature for 10% conversion; [c] measured at 623 K in a recycle reactor.

The better performance of PdCeM is maintained also in the cooling portion of the cycle, where the drop of activity due to the dynamics of Pd-PdO transformation follows the order PdCeM<PdCeSCS<PdOCeM<PdCeIW. The catalyst stability has been successfully checked over six light-off cycles (Figure S3) where it can be seen that PdCeM shows a stable CH₄ conversion behavior from the third cycle onward. Time on stream behavior has also been investigated both under reaction conditions and in the presence of large excess of water (Figure S4), which is known to accelerate deactivation in Pd-based catalysts.[8] Catalysts prepared by milling are more stable with an overall activity loss of ca. 25% after 24 h on stream, compared with a loss of 70% observed in reference PdCeIW.

Light-off activity behavior of PdCeM is also affected by the modification of milling parameters. It is observed that, increasing milling intensity, the overall light-off profiles of the catalyst shift to higher temperatures, indicating a drop of reaction rates compared to our standard PdCeM sample (see Figure S5).

Also, milling under loose conditions without using balls does provide catalysts active in a first cycle at low temperature but suffering of dramatic deactivation, due to the lack of nanoscale interactions between Pd and ceria and extensive sintering at higher temperatures (Figure S6). This shows that the choice of our milling parameters for PdCeM sample (10 minutes milling at an oscillation frequency of 15 Hz with a ball to powder ratio of 10) optimizes activity performances.

Methane oxidation light-off profiles were also collected on the corresponding ZrO₂ supported catalysts, and they did not evidence any significant difference among samples prepared by impregnation and by mechanical milling (Figure S7). This strongly supports the fact that the origin of the unique activity of PdCeM must be found in a specific characteristic of the Pd-CeO₂ interface that is promoted during milling, and not in a more general behavior of samples prepared by a mechanochemical procedure.

In parallel to light-off cycles, temperature programmed oxidation experiments (TPO, Figure 2) showed for fresh PdCeM the oxidation of Pd at low temperature (cycle 1), and the presence of at least three PdO decomposition peaks (cycles 2 and 3), indicating the coexistence of different palladium species. Quantitative re-oxidation of Pd during cooling occurs in one single peak at ca. 910 K. A comparison with PdCeIW, which presents only two oxygen release peaks, is shown in Figure S8.

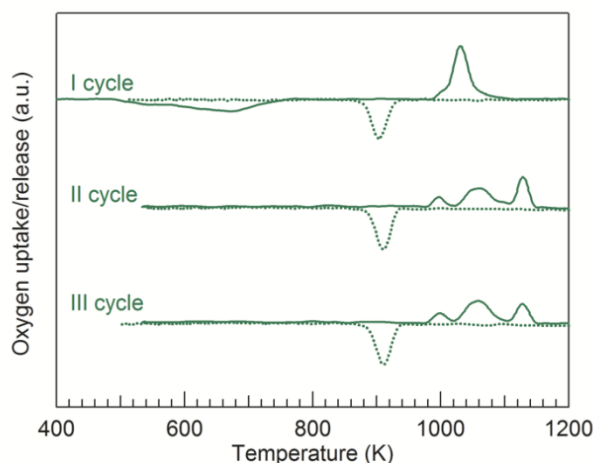


Figure 2. TPO profiles for PdCeM over three consecutive heating/cooling cycles. Solid line: heating ramp; dotted line: cooling ramp.

Details on the Pd-CeO₂ morphology were obtained by HRTEM analysis on the fresh samples. Figure 3 (A,B) shows the surface of PdCeIW where, as expected, small Pd nanoparticles (ca. 2 nm) are well dispersed over a clean ceria surface. In contrast, PdCeM is characterized by ceria crystallites that are covered by an amorphous layer measuring between 2 and 5 nm in thickness (Figure 3 C-F). This amorphous shell is compact and perfectly defined, following the perimeter of the ceria particles (Figure 3C-D). Interestingly, the ceria crystallites covered by this layer present a more rounded morphology, suggesting that the spreading of Pd by mechanical mixing affects their surface. Ceria nanoparticles show well-defined lattice fringes at 3.12 and 2.71 Å in both samples, which correspond to the (111) and (200) crystallographic

planes of CeO₂, respectively. In Figure 3D the EDX analysis of the shell is reported, which contains both ceria and Pd (the Cu signal originates from the TEM grid), indicating that the shell is comprised of a mixed Pd-Ce phase.

In addition to this amorphous layer, some smaller particles measuring less than 5 nm are also detected, mostly decorating the ceria crystallites (Figure 3E,F). Lattice fringe analysis of these nanoparticles (see insets “c” and “d” corresponding to FT images of “a” and “b”, respectively, in Figure 3F) shows fringes at 2.25 and 1.95 Å. They correspond to the (111) and (200) crystallographic planes of Pd metal. Noticeably, these Pd nanoparticles are embedded in the amorphous shell, which suggests that the shell is produced by the distribution of Pd metal nanoparticles over the ceria support upon mechanical mixing. Figure 3E represents nicely this situation: a very small nanoparticle (less than 2 nm) diffuses into the shell at the edges, still preserving some crystallographic order (see the FT image in inset “a” showing fringes of Pd metal).

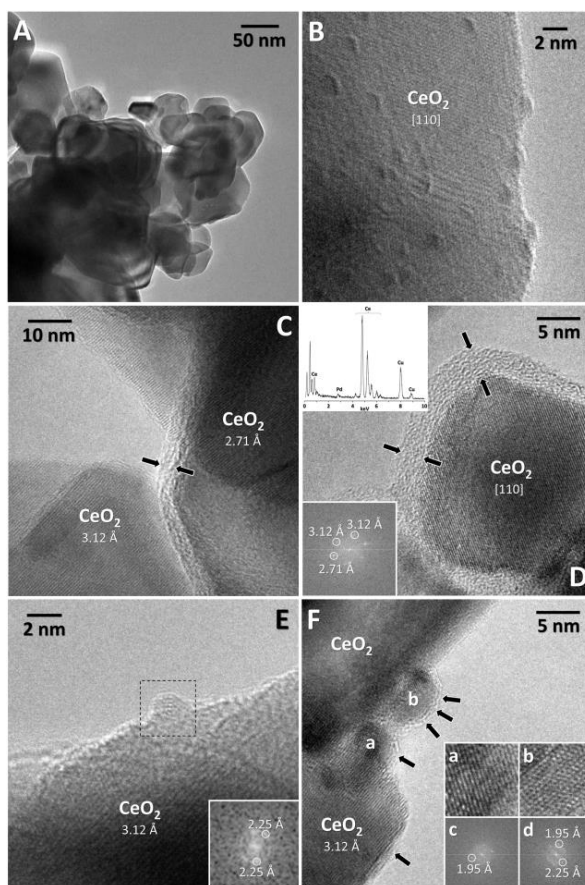


Figure 3. HRTEM images of PdCeIW (A,B) and PdCeM (C-F).

Remarkably, this morphology is not observed on PdOCeM and PdZrM where well defined PdO and Pd nanoparticles are respectively found over the support (see Figure S9 and S10 for representative samples). Moreover, the mechanical milling of pure CeO₂ under the same conditions does not induce any change of the surface (Figure S11) indicating that surface amorphisation takes place only upon mixing of Pd and ceria.

A similar core-shell structure where Pd covers SnO₂ particles was observed on a Pd/SnO₂ catalyst prepared by wet impregnation;[9] however, the Pd-Sn alloy based shell disappeared under oxidizing atmosphere. Conversely, the amorphous shell observed on PdCeM is also stable under reaction conditions, as demonstrated by the HRTEM image of the used sample after two cycles (Figure 4 A and B) in which it is possible to recognize the presence of two fringes, one at 3.1 Å corresponding to the (111) crystallographic planes of the ceria substrate, and another one at a greater spacing likely due to inclusion of PdO within ceria lattice, where Pd is strongly interacting with the support. This is in accordance with the existence of small domains of Pd completely embedded in the amorphous shell, as discussed above for the fresh PdCeM sample. Figure 4 (C and D) shows representative images of the shell around ceria after 6 reaction cycles, which is marked between arrows along with the crystallographic planes exposed by the ceria crystallites. From these images it is clear that the shell is preserved after the sixth cycle. Interestingly, no remaining Pd containing particles have been identified indicating that all Pd is still spread within the layer surrounding the ceria particles. Similarly, time on stream behavior under hydrothermal conditions does not alter the structure of the layer, indicating stability also in the presence of excess of water (Figure S12).

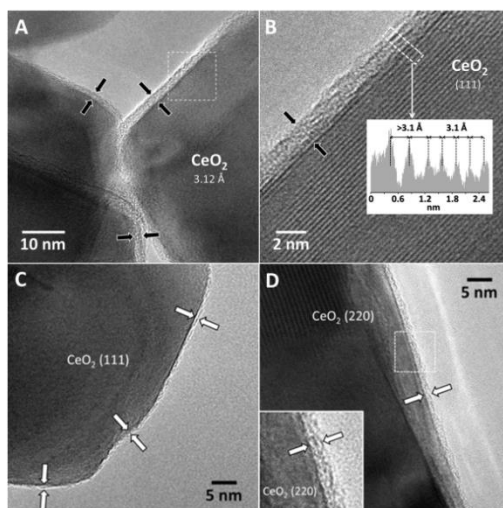


Figure 4. HRTEM images of PdCeM after two (A, B) and six (C, D) methane oxidation tests.

The reasons behind the structural rearrangement of the surface in PdCeM during milling are not straightforward and should be the result of a combination of different elements. Some interesting indications on the phenomena that might take place during the mechanical mixing of Pd and ceria powders come from the studies on solid state amorphisation.[10] In these studies it is evidenced that mechanical alloying increases vacancies, chemical disordering at atomic level and nanocrystalline grain boundaries, which in turn raise the free energy of the crystalline phase favoring the stabilization of the amorphous state, particularly at nanometer scale. This process usually starts with the amorphisation of the edges, and in some cases proceeds through the formation of a crystalline solid solution which is then transformed into the amorphous phase. Interestingly, the formation of point and lattice defects by milling has been proposed as the rate limiting step for amorphisation.[11]

It should be observed though that, in general, in the studies dealing with solid state amorphisation the energies employed are much higher than those of our dry mixing method, nevertheless in the case of palladium and ceria the process might be speeded up by other factors, like the specific interaction between Pd and CeO₂.^[12] This interaction, which could account for an easier solid state reaction between the two components, involves the formation of vacancies and/or more active oxygen states at the metal-oxide interface as observed for other systems after milling.^[13] In addition, it has been reported that the oxidation state of cerium ions in solid solutions can be altered at room temperature by changing mechanically the local stress state, and that the distribution of Ce³⁺/Ce⁴⁺ can be influenced by stress gradients.^[14]

Indeed, XPS studies carried out on PdCeM and PdCeIW after one reaction cycle (Table 2) show that the ratio between Ce(III) and Ce(IV) is higher on the sample prepared by mechanical grinding compared to the impregnated one, and also to pure milled CeO₂ (sample CeM). This indicates that the interplay between Pd and ceria on PdCeM is stronger and induces a higher degree of ceria reduction. In addition, a better and more homogeneous Pd distribution is also observed in milled samples which is maintained after the first reaction cycles.

Table 2. Data from XPS analysis.

Sample	Pd/Ce	Ce(III)/Ce	Pd(0)	Pd(II) (%)	Pd(IV) (%)
CeM	-	0.16	-	-	-
PdCeM ^a	0.19(0.18) ^b	0.24(0.12)	0(0)	82(78)	18(22)
PdCeIW ^a	0.15(0.15)	0.15(0.12)	0(0)	76(87)	24(13)

[a] collected after one reaction cycle; [b] in parentheses data collected after six reaction cycles.

Characterization after six reaction cycles shows an increase of Pd(IV) in milled sample compared to PdCeIW while the amount of Ce(III) become similar, likely due to prolonged oxidation cycles at high temperature. In addition, the better Pd distribution of PdCeM is maintained after stability tests. This is also confirmed by comparing the Raman spectra obtained by mapping 144 μm² of the surface of PdCeM and PdCeIW (Figure S13). In both samples the more intense signal is due to the F2g vibrational mode of CeO₂ (461 cm⁻¹), but a signal originating from the B1g vibrational mode of PdO is also observed (646 cm⁻¹). Collecting several spectra, it is clearly seen that the intensity ratio between the two signals is rather constant for PdCeM (Figure S13), indicating a more homogeneous spreading of Pd over CeO₂, as it can be expected from its distribution within the surface layer. A broad Raman signal covering the region between 550-600 cm⁻¹ is also detected in PdCeM; peaks in this region are attributed to surface defects in ceria^[15] that might include those generated by close interaction and inclusion of Pd into CeO₂ lattice.

The information gathered from HRTEM and XPS studies show that on PdCeM there is a unique arrangement of Pd and ceria that is not observed on samples prepared by conventional routes. This arrangement is the result of an interaction between Pd and ceria promoted by mechanical milling and by the redox characteristics of the two components. We recently reported that the milling of ceria with carbon soot results in the formation of a CeO₂ core wrapped in a soft

carbon shell[7]; the nanoscale arrangement created by mixing was promoted by the different hardness of the two materials that helps the spreading of the softer carbon particles on the surface of ceria. This might explain why the core-shell structure observed here is obtained only when mixing Pd metal nanoparticles and ceria and not when harder materials like PdO and/or ZrO₂ are used (0.6 vs 4 GPa for Pd metal and ceria, respectively, against 8 for zirconia[16]). It is true in fact that the adhesive force between two compressed particles varies inversely with their hardness.[17]

The high reactivity for methane oxidation over Pd/CeO₂ interfacial sites was recently described by the group of Janik, using integrated DFT and empirical reactive force field methods[5b]. In their study partially embedded Pd clusters are shown to favor the formation of metastable transient Pd⁴⁺ ions inserted into ceria lattice which are indicated as the most reactive for methane activation. The authors predict that, starting from supported Pd clusters, Pd atoms can migrate across the ceria surface and assume a higher oxygen coordination being incorporated into the lattice when encountering steps, vacancies and/or grain boundaries, forming active oxidized Pd species. It is remarkable to observe that this description well agrees with our HRTEM observation of nanometer scale Pd clusters embedded in an amorphous Pd-CeO₂ shell (Figure 2 E,F), as if this layer would be originated by the dissolution of Pd nanoclusters into the ceria lattice. A similar situation, with copper clusters dispersed into the ceria lattice at atomic scale, has been recently reported following the mechanical mixing of cerium and copper complexes.[18] This unique embedded configuration might explain the reasons why active Pd⁴⁺ centers in PdCeM are more efficient than in PdCeIW, where the presence of Pd⁴⁺ (also detected by XPS) is not characterized by the same nanoscale environment. This picture might also explain why promotion of activity is not observed for PdZrM and PdOCeM. Thanks to the oxygen exchange properties of ceria, Pd⁴⁺ ions are formed on CeO₂ under conditions much different from other supports.[5b] Moreover, the appearance of these species is prompted by the migration of Pd atoms in the lattice from metallic Pd clusters on the surface[5b], a situation that likely could not be feasible in presence of stable PdO clusters.

In summary, it is shown that the formation of a specific nanoscale arrangement, with Pd moieties embedded in the outer surface layers of ceria, promotes methane activation at much lower temperature compared to conventional Pd/CeO₂ catalysts. These experimental results, supported by a strong theoretical background developed independently[5], open the way to the design of highly active Pd-ceria catalytic systems via sustainable mechanical synthesis routes. In addition, and perhaps more importantly, they put the accent on the role of mechanical stress in modifying at nanoscale the properties of ceria, which can offer a powerful tool in the design of materials with undisclosed properties.

Acknowledgements

Financial support from Ford Motor Company under 2014-2195R URP Award “Three-way catalyst materials for compressed natural gas vehicles” is kindly acknowledged. MD acknowledges Regione Friuli Venezia Giulia for funding PhD under Operating Program of the European Social Fund 2014/2020. JL is a Serra Hunter Fellow and is grateful to ICREA Academia program and grants MINECO/FEDER ENE2015-63969 and GC 2017 SGR 128.

- [1] R. J. Farrauto, *Science* 2012, 337, 659-660.
- [2] P. Tang, Q. J. Zhu, Z. X. Wu, D. Ma, *Energ Environ Sci* 2014, 7, 2580-2591.
- [3] a) S. Colussi, A. Trovarelli, C. Cristiani, L. Lietti, G. Groppi, *Catalysis Today* 2012, 180, 124-130; b) M. Cargnello, J. J. Delgado Jaen, J. C. Hernandez Garrido, K. Bakhmutsky, T. Montini, J. J. Calvino Gamez, R. J. Gorte, P. Fornasiero, *Science* 2012, 337, 713-717; c) S. Fouladvand, S. Schernich, J. Libuda, H. Gronbeck, T. Pingel, E. Olsson, M. Skoglundh, P. A. Carlsson, *Top Catal* 2013, 56, 410-415; d) J. Nilsson, P. A. Carlsson, S. Fouladvand, N. M. Martin, J. Gustafson, M. A. Newton, E. Lundgren, H. Gronbeck, M. Skoglundh, *ACS Catalysis* 2015, 5, 2481-2489.
- [4] a) L. Meng, J.-J. Lin, Z.-Y. Pu, L.-F. Luo, A.-P. Jia, W.-X. Huang, M.-F. Luo, J.-Q. Lu, *Appl. Catal. B-Environ.* 2012, 119, 117-122; b) Y. Zhu, S. R. Zhang, J. J. Shan, L. Nguyen, S. H. Zhan, X. L. Gu, F. Tao, *ACS Catalysis* 2013, 3, 2627-2639; c) S. Colussi, A. Gayen, M. Boaro, J. Llorca, A. Trovarelli, *Chemcatchem* 2015, 7, 2222-2229.
- [5] a) T. P. Senftle, A. C. T. van Duin, M. J. Janik, *ACS Catalysis* 2015, 5, 6187-6199; b) T. P. Senftle, A. C. T. van Duin, M. J. Janik, *ACS Catalysis* 2017, 7, 327-332.
- [6] S. Colussi, A. Gayen, M. F. Camellone, M. Boaro, J. Llorca, S. Fabris, A. Trovarelli, *Angewandte Chemie-International Edition* 2009, 48, 8481-8484.
- [7] E. Aneggi, V. Rico-Perez, C. de Leitenburg, S. Maschio, L. Soler, J. Llorca, A. Trovarelli, *Angewandte Chemie-International Edition* 2015, 54, 14040-14043.
- [8] R. Gholami, M. Alyani, K. J. Smith, *Catalysts* 2015, 5, 561-594.
- [9] N. Kamiuchi, H. Muroyama, T. Matsui, R. Kikuchi, K. Eguchi, *Appl Catal A-Gen* 2010, 379, 148-154.
- [10] M. H. Enayati, F. A. Mohamed, *Int Mater Rev* 2014, 59, 394-416.
- [11] R. B. Schwarz, C. C. Koch, *Appl Phys Lett* 1986, 49, 146-148.
- [12] a) Z. Yang, L. A. Zhansheng, G. Luo, K. Hermansson, *Phys Lett A* 2007, 369, 132-139; b) B. Liu, J. Liu, T. Li, Z. Zhao, X. Q. Gong, Y. Chen, A. J. Duan, G. Y. Jiang, Y. C. Wei, *J Phys Chem C* 2015, 119, 12923-12934; c) E. M. Slavinskaya, T. Y. Kardash, O. A. Stonkus, R. V. Gulyaev, I. N. Lapin, V. A. Svetlichnyi, A. I. Boronin, *Catal Sci Technol* 2016, 6, 6650-6666.
- [13] a) Y. Maeda, T. Akita, M. Kohyama, *Catal Lett* 2014, 144, 2086-2090; b) Y. Yang, S. Z. Zhang, S. W. Wang, K. L. Zhang, H. Z. Wang, J. Huang, S. B. Deng, B. Wang, Y. J. Wang, G. Yu, *Environ Sci Technol* 2015, 49, 4473-4480; c) C. Borchers, M. L. Martin, G. A. Vorobjeva, O. S. Morozova, A. A. Firsova, A. V. Leonov, E. Z. Kurmaev, A. I. Kukharensko, I. S. Zhidkov, S. O. Cholakh, *J Nanopart Res* 2016, 18; d) C. J. Tang, B. W. Sun, J. F. Sun, X. Hong, Y. Deng, F. Gao, L. Dong, *Catalysis Today* 2017, 281, 575-582.
- [14] a) T. X. T. Sayle, M. Cantoni, U. M. Bhatta, S. C. Parker, S. R. Hall, G. Mobus, M. Molinari, D. Reid, S. Seal, D. C. Sayle, *Chemistry of Materials* 2012, 24, 1811-1821; b) C. Munnings, S. P. S. Badwal, D. Fini, *Ionics* 2014, 20, 1117-1126.
- [15] a) J. E. Spanier, R. D. Robinson, F. Zheng, S. W. Chan, I. P. Herman, *Phys Rev B* 2001, 64; b) A. Filtschew, K. Hofmann, C. Hess, *J Phys Chem C* 2016, 120, 6694-6703.

- [16] a) S. Maschio, O. Sbaizero, S. Meriani, *Journal of the European Ceramic Society* 1992, 9, 127-132; b) G. V. Samsonov, in *Handbook of the Physicochemical Properties of the Elements* (Ed.: G. V. Samsonov), Springer US, Boston, MA, 1968, pp. 387-446.
- [17] H. Krupp, *Advances in Colloid and Interface Science* 1967, 1, 111-239.
- [18] W. C. Zhan, S. Z. Yang, P. F. Zhang, Y. L. Guo, G. Z. Lu, M. F. Chisholm, S. Dai, *Chemistry of Materials* 2017, 29, 7323-7329.