

# Biomass-fired combined heating, cooling, and power for small scale applications – A review

Moritz Wegener<sup>a,b,\*</sup>, Anders Malmquist<sup>a</sup>, Antonio Isalgué<sup>b</sup>, Andrew Martin<sup>a</sup>

<sup>a</sup>Heat and Power Technology, Department of Energy Technology, KTH Royal Institute of Technology, Brinellvägen 68, 100 44 Stockholm, Sweden

<sup>b</sup>Architecture & Energy, School of Architecture of Barcelona, UPC. Av. Diagonal, 649, 6th Floor, 08028 Barcelona, Spain

\*Corresponding Author:

Tel.: +46 8 790 60 00

E-mail: [mbgw@kth.se](mailto:mbgw@kth.se)

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## Abstract

The growing demand for energy and the accelerating threats from climate change call for innovative and sustainable solutions to decrease dependency on fossil fuels. Biomass-based, small-scale Combined Cooling, Heating and Power (CCHP) systems are one of these solutions, because they can satisfy the energy demands of the consumer with enhanced flexibility, lower losses, less costs and less environmental pollution as compared to centralized facilities. Due to recent advances in several scientific subfields with relevance to small-scale CCHP, a rapidly increasing amount of literature is now available. Therefore, a structural overview is essential for engineers and researchers. This paper presents a review of the current investigations in small-scale CCHP systems covering biomass-fired concepts and solar extensions. To this end, critical system components are described and analysed according to their specific advantages and drawbacks. Recent case studies have been collected and key findings are highlighted according to each type of prime mover. The results indicate a scientific bias towards the economic viability of such systems and the need for real-life and experiment system data. However, the potential of biomass-fired CCHP systems and of such systems with solar extensions has clearly been recognised. Based on the results, future policy implementations should focus on fostering such systems in areas with high energy costs and to increase energy resilience in developed regions. Additionally research and industry applying novel prime mover technologies should be financially supported.

## Keywords

Small-scale CCHP, Trigeneration, biomass, bio-solar

## 1 Introduction

To fuel the world's rising demand for energy while also to slow down emissions of greenhouse gases, more efficient and more sustainable energy systems are necessary [1]. Combined Cooling, Heating and Power (CCHP) is a technology that aims to raise the energy efficiency of an energy system by using the electric as well as the thermal output for practical applications [2,3]. Most deployed CCHP systems involve centralized facilities with extensive heating and cooling networks supplying hundreds or thousands of industrial and residential consumers. However, the disadvantages of centralized energy systems are losses due to longer transfer distances, the inability to reply to the immediate demands of individual consumers and higher security risks should unexpected shutdowns occur [4]. Therefore smaller decentralized units, which serve the local demand for heat as well as for electricity, can be a more profitable and more efficient alternative to centralized facilities [5].

While small-scale systems providing cooling, heat and/or power driven by fossil fuels have been successfully developed and constructed for decades, the implementation of renewable options is relatively new and successful mass-scale commercialization still has to be proven [6,7]. Amongst renewable energies, biomass seems to be the most promising energy source for CCHP systems as other renewable energies are either not generating enough heat in normal operation modes (wind, photovoltaic, hydro), are too locally limited (geothermal) or are too volatile (solar thermal) [8–11]. Hence, the development of small-scale, biomass-fired CCHP systems is becoming increasingly important for climate politics, economics and research [12–14]. Such systems can be especially cost-efficient solutions in remote areas and islands with adequate sources of renewable energies [15,16]. Extensions involving solar electric energy can greatly augment the sustainability and viability of this approach, considering the vast solar potential and falling photovoltaic (PV) prices [17].

Historically CCHP is linked to the more well-known Combined Heat and Power (CHP) concept: a cooling unit is integrated to the CHP system, leading to more choices for energy outputs and higher operating times, especially in comparison to conventional power plants [12,18]. Several synonyms of CCHP can be found in literature and the following list defines their meaning for this paper [19]:

- Trigeneration: essentially equivalent to CCHP [19]
- Polygeneration/Multigeneration: Any system which produces more than two energy services; this can be a CCHP system but may also be a system producing chemicals or other products [19,]
- MCCHP/  $\mu$ CCHP: Micro CCHP (with less than 20 kW electric power) [20,21]
- CHP with Cooling or Cogeneration with Cooling: Essentially the same as CCHP [22]
- BCHP: Building Cooling Heating and Power [23]
- Biorefinery: Any system, which produces chemical products out of biomass [19]

Several studies indicate significant potential for biomass-fired CCHP systems, but so far only medium-scale (1 MW-10 MW) and large scale (>10 MW) systems have been commercialised successfully, while micro-scale (<20 kW) and small-scale (20 kW – 1 MW) systems are still in an experimental phase [21,24]. To design a CCHP system for optimal environmental and economic performance, component type and size have to be evaluated and chosen carefully according to the electricity, heating and cooling demand [2,5]. For this, many authors argue that the prime mover is the heart of such systems with the biggest impact on system economics and environment [5,21,25]. Another possibility to optimize small-scale CCHP systems is to use operation strategies adjusted to the electric or the thermal load [20]. These loads depend heavily on the energy consumer, which can be a household, an office building, a hospital, or any similar buildings [26]. Several studies investigate the optimal behaviour for CCHP systems and highlight the benefits of their flexibility for energy generation [19,27,28].

The previously mentioned studies review certain aspects of CCHP systems, but none of them focus on the growing amount of literature on biomass-fired options [14]. Hence, the aim of this paper is to summarize and structure the constantly increasing amount of scientific literature on small-scale (< 1 MW<sub>el</sub>), biomass-fired CCHP systems. For this, currently used technologies are presented as shown in Figure 1 and their specific benefits as well as drawbacks are identified. For each different prime mover technology, the key findings of the most recent case studies from 2010 to 2017 are highlighted and their key characteristics (maximal output, type of biomass, prime mover type, refrigeration technology, model software/experiment location) are assembled.

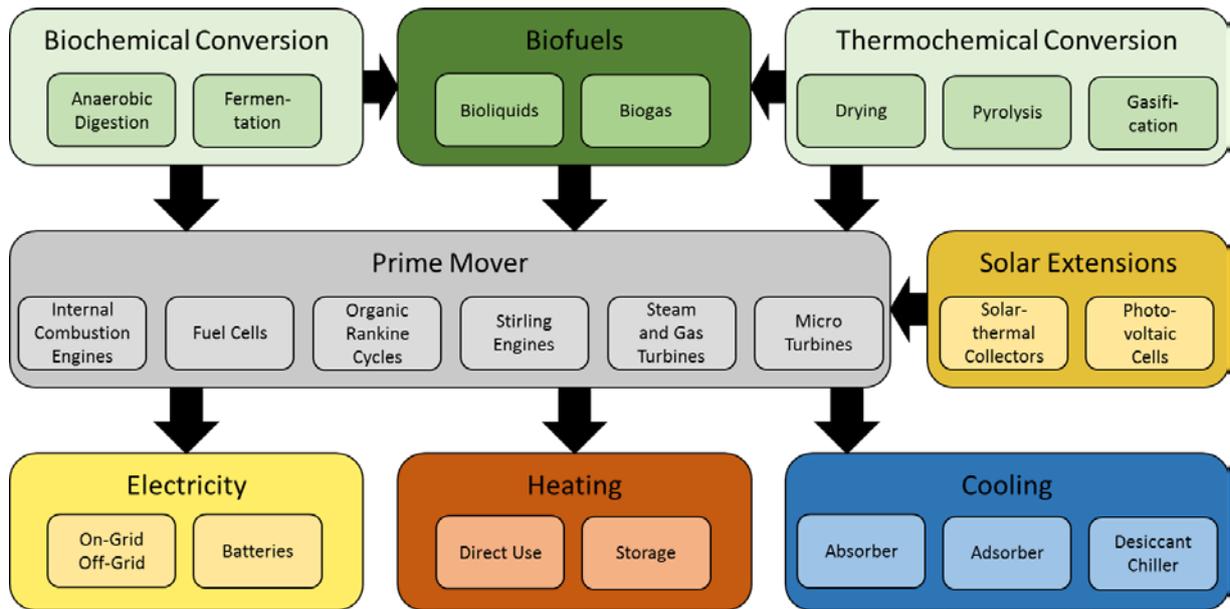


Figure 1 Key components in biomass-fired and solar assisted small-scale CCHP systems

After this introduction, internal and external factors that affect the technological and economic development of CCHP systems will be listed in chapter 2. In chapter 3, the different ways to obtain biofuel for small-scale CCHP systems are presented. The studies investigating small-scale biomass-fired CCHP systems are summarized and listed according to their prime mover in chapter 4. Therefore, the focus of the review has been laid on CCHP systems based on these various prime movers. Chapter 5 presents the most common cooling and storage technologies. The findings are discussed in chapter 6 and finally conclusions are drawn in chapter 7, where also future policy implementations are suggested.

## 2 Internal and external factors driving CCHP development

To seize the potential of small-scale CCHP systems internal as well as external factors will influence the development in the coming years. One external factor for the viability of small-scale CHP and CCHP systems are government policies for support and subsidies [19]. It was noted that governments from developed and developing countries like the USA, China, the EU, Brazil, Russia and Japan use different mechanisms to promote the use of CCHP systems [20,21]. This implies, that the huge potential has been acknowledged also politically, but until today the total share of electricity and heat generated through CHP and CCHP systems still remains low with for example less than 6% of heat generated by CHP or CCHP systems in the EU in 2016 [20,29]. However, other external factors like biomass prices, oil prices or carbon dioxide taxes also effect the economics of small-scale CCHP systems greatly [30].

There are several parameters to measure the performance of internal factors of energy systems, for which a good overview can be found in [31]. One of the most commonly used energetic performance parameters is the Primary Energy Saving Ratio (PESR), which describes the ratio of primary energy saved in the new system compared to a conventional stand-alone energy generation system [12,31]. Many small-scale CHP and CCHP systems achieve a PESR of 20-30%, which indicates favourable ecologic and economic performances [9,27,32]. However, especially in the case of biomass-fired and biomass-fired solar-assisted CCHP systems, the PESR can be misleading, because even if more energy is needed in biomass systems than in conventional systems, they might still perform ecologically better. Hence, other methodologies like Life Cycle Assessments or CO<sub>2</sub>-equivalence should also be taken into account [2,31].

## 3 Fuel Supply

Apart from using simple mechanical preparation, biomass can be transformed into a gaseous, liquid or solid fuel through either biochemical conversion or through thermochemical conversion [33]. These

products can either be used for fueling a CCHP system directly or can be stored and then transported to the CCHP system.

### 3.1 Biochemical Conversion

The most popular biochemical conversion technology is anaerobic digestion, which describes a chain process of biological reactions in a low-oxygen environment transforming organic biomass into biogas [10,34]. The main contents of biogas are methane with 55-80% and carbon dioxide with 20-45%, while other gases as impurities and the remains of the anaerobic biomass are also produced [33,35]. Biomass used for anaerobic digestion is usually waste from agricultural enterprises or manure from animals and/or humans. This type of biomass has usually a high moisture content and features high ash contents [36].

Another technology for the biochemical conversion of biomass is fermentation, which describes the conversion of biomass firstly to sugars and finally to alcohols, mainly bio-ethanol. Mostly sugar or starch crops are used, however the process can also be applied to lignocellulose biomass, but with less efficiency [36]. Fermentation is usually applied in large-scale factories and is one of the most commonly used processes for the production of high-quality biofuels [37].

### 3.2 Thermochemical Conversion

The first process for preparing biomass for thermochemical conversion is drying, because this way, even for direct combustion, the efficiency can easily be increased by 5-10% and air emissions can be lowered. For micro-scale CCHP systems, the biomass can be dried before insertion into the system by using direct solar irradiation or other heat sources. Alternatively, some part of the exhaust heat from the CCHP system can be used to dry the biomass rapidly [38].

Pyrolysis describes the process of breaking down long hydrocarbon chains into smaller pieces by applying heat at temperatures, normally between 450-600 °C with low-oxygen supply [36]. Apart from temperature and heat supply time, other factors like chemical composition or surface area of the biomass have significant impact on the process and the products [35,39]. Gaseous products of biomass pyrolysis are mostly H<sub>2</sub>, CO, CO<sub>2</sub>, and CH<sub>4</sub>, but also higher hydrocarbons like C<sub>2</sub>H<sub>6</sub>, C<sub>2</sub>H<sub>4</sub>, and C<sub>3</sub>H<sub>8</sub> in small amounts. Additionally liquid oils are produced, which consist of even higher hydrocarbon chains, and solid charcoal remains, which can be used for combustion or fertilizing [39]. The produced oils can be transformed into transportation fuels or they can be further broken down by applying more heat [10,35].

This process of applying even more heat to biomass, usually at temperatures between 750-1,000 °C degrees, is referred to as gasification. At this temperature level, almost all carbohydrates are cracked down to H<sub>2</sub> and CO and the produced gas is often referred to as synthesis gas (syngas), producer gas, or wood gas. This is not a full combustion because the process occurs in a low oxygen environment [35]. Fixed bed type gasifiers represent the simplest category of gasifiers, where solid fuel particles are placed in a cylinder and gasifying agents (e.g. air, oxygen, steam) pass through the solid particles. After leaving the gasification chamber, the syngas usually undergoes a cleaning process by sending it through a cyclone for removal of solid particles and through filters. Another category of gasifiers is fluidized bed gasifiers [40]. Here the fluidizing agents enter from below into a mixture of biomass and inert bed materials like silica or sand, which are working as catalysts for the gasification process.

### 3.3 Bioliquids and Biogases

Based on the previous processes, medium to large-scale biofuel plants can provide biofuels used in many small-scale CCHP systems. For the sake of a complete picture of possible biofuel sources, a few other processes for the generation of biofuels will be listed shortly:

- Jatropha oil produced mechanically from Jatropha plants holds high potential for an easy-to-produce supply of biodiesel [41]. Several other so called energy plants are also currently under investigation for efficient generation of biofuels, e.g. Switch grass, Bermuda grass, Silver grass, Alamo [42].

- For the production of methane, seaweed (macroalgae) is currently being investigated and several pilot projects have proven successful implementation for biofuel production [42].
- Microalgae, which are used mainly in urban wastewaters, have been shown to be feasible for biofuel production [43].

## 4 Prime Mover

For the various types of biofuels, different prime movers can be selected, which greatly influence the energetic and economic performance of a CCHP plant [21,25,44]. An assessment of key characteristics of prime movers presented in this study is shown in Table 1 (No publications could be found that considered steam engines in this context, thus this prime mover is omitted). The assessment of the potential for a given prime mover estimates the ability for biomass-fired CCHP market penetration in the near future. It is based on findings from different sources as well as on the authors' judgement.

Table 1 Assessment of Prime Movers for small-scale biomass-fired CCHP systems

<b>Prime Mover</b>	<b>Internal Combustion Engines</b>	<b>Fuel Cells</b>	<b>Stirling Engines</b>	<b>Organic Rankine Cycles</b>	<b>Micro Turbines</b>
<b>Size</b>	Up to near 100 MW [25]	Up to 2 MW [25]	Up to 150 kW [2]	up to 2 MW [2]	Up to 1,000 kW [21]
<b>Advantages</b>	Very high reliability (with clean fuels) [21,45] Rapid start-up [21] Low investment costs [21]	Excellent partial load performance [25] Very high electric efficiency [5,21] Low noise [45] Low emissions [5,21]	Can use low quality fuels due to external combustion [21,25,32] Good partial load performance [12,25,32] Potentially low maintenance requirements/ less moving parts [21,46] High thermal efficiency [5] Low emissions [5,32]	Can run with low grade heat [12] High reliability [12,47] Low maintenance costs [5,48] Good partial load behaviour [47]	Low quality fuels can be used for externally driven units [21] Very few moving parts [21] Very compact sizes [21] High temperature exhaust [45] Low emissions [45]
<b>Disadvantages</b>	Short maintenance intervals [21,45] Instability with bio- and syngas/ limited fuel flexibility [21,48,49] High noise [45] High NO <sub>x</sub> -emissions [5,21] Using waste heat difficult [45]	Very high investment costs [5] SOFCs have long start-up times [25] Requires very high quality, energy intensive fuels [21] Low heat recovery [5]	Still high investment costs [21] Low electric efficiency [5,32] Technology not fully developed [32,45] Difficult to control power output [32]	Still high investment costs [5] Low maximal electric efficiency [5] Low heat recovery for low-grade heat applications [2]	Still high investment costs [21] Difficult Start-up [5,21] Delicate mechanical design [9] Low electric efficiency [18]
<b>Commonness in the reviewed cases</b>	Most common 19/41	Rare 3/41	Rare 2/41	Common 12/41	Rare 5/41
<b>Assessment of potential</b>	Remains stable	High [45]	Very High [2]	High [2]	Very high [21,50]

#### **4.1 Internal Combustion Engines**

Due to their advanced technological development, low initial investment costs and widespread distribution, internal combustion engines (ICEs) represent the most often applied and most researched prime mover. The nominal electric loads of ICEs can range from 3 kW to up to 100 MW, making them applicable for all sizes of small-scale CCHP system. In addition, the electric efficiency of ICEs can reach up to 45%, but the thermal losses are comparatively high, so that the overall efficiency of ICE systems is generally equal or lower compared to other prime movers. In small-scale CCHP systems the amount of chemical energy converted into electric energy is found to be a bit lower, usually in the range of 30-35% [51]. Especially in the context of syngas usage, ICEs are quickly damaged by low quality gases (i.e. sticky tar can clog injection nozzles) and hence their efficiency is lowered significantly [48,49]. Therefore, bigger CCHP systems using ICEs and direct gasification generally include more sophisticated cleaning systems [52]. All described systems of small-scale bio-fired CCHP systems with ICEs are summarized in Table 2-Table 5. Cases of small-scale bio-fired CCHP systems using ICEs in combination with solar extensions are summarized in Table 8.

Table 2 Cases of small-scale biomass-fired CCHP systems with ICEs with 100-300 kW nominal power

Ref.	Max. Outputs	Biomass	Prime mover	Refrigeration	Software/ Location	Key Findings
[53]	<p>Electricity : 250kW - 1,974 kW</p> <p>Heating: 2,057 kW - 5,217 kW</p> <p>Cooling: 151 kW- no limit specified</p>	Wood chips and almond shells (gasified)	ICE (in the reference system with 767 kW nominal power)	AC	EES Model for a district heating and cooling network	<p>Analysis of 5 different configurations:</p> <ul style="list-style-type: none"> <li>• single vs. double AC</li> <li>• Heat recovery after air preheating vs. only engine exhaust gases</li> </ul> <p>Double effect AC with both heat recover inputs is the most efficient solution</p> <p>Overall system energy efficiency: 60% Electric efficiency: 37%</p>
[54]	<p>Electricity: 250kW</p> <p>Heating: 320 kW (in trigeneration)</p> <p>Cooling: 92.2 kW</p>	<p>Gasification:</p> <ul style="list-style-type: none"> <li>• willow chips</li> <li>• Miscanthus</li> <li>• rice husk</li> </ul>	ICE	Ammonia absorption	Model in Eclipse	<p>Energetic Efficiencies: CHP 61.4-66.5% Trigeneration: 53.5%-58.6%</p> <p>Cogeneration produces least amount of CO<sub>2</sub>-emissions</p> <p>Difference in biomass inputs affects technical performance marginally, but has great impact on economics due to biomass cost</p> <p>Use of Miscanthus leads to highest efficiencies</p> <p>All three biomasses economically feasible in the proposed trigeneration system</p>
[55]	<p>Electricity: 240 kW</p> <p>Heating: 225 kW</p> <p>Cooling: 13 kW</p>	Jatropha Oil	ICE	Ammonia AC	Model in ECLIPSE for households in GB	<p>Efficiencies of Jatropha oil fueled system lower than diesel fueled</p> <p>If emissions of the Jatropha oil were not considered as net zero the CO<sub>2</sub> emissions were found to be higher compared to diesel/CO<sub>2</sub> emissions (kg/kWh) less than half compared to power-only mode</p>
[56]	<p>Electricity: 120 kW</p> <p>Heating: up to 200 kW</p> <p>Cooling: 25.6 kW</p>	Biogas through anaerobic digestion of cow manure and brewers waste	Lister-Petter diesel engine assisted by dual-fuel boiler	Gas-fired ammonia-water AC	Eclipse software for a micro-brewery in England	<p>CHP system feasible under national funding scheme</p> <p>Trigeneration system calculated to have a payback period of 5.4 years and the highest additional income over 20 years</p>
[57]	<p>Electricity: designed for 100kW</p> <p>Heating: ~131 kW</p> <p>Cooling: ~76 kW</p>	Wood chips (gasified) + natural gas	ICE	AC	Model for a Chinese region supported by EES	<p>Combined use of natural gas and wood chips for a CCHP system</p> <p>Cofiring syngas and natural gas has higher efficiency than just combusting syngas</p> <p>Energetic efficiency 70-79.5%</p> <p>Exergetic efficiency: 22-35.6%</p> <p>Costs heavily affected by biomass and natural gas price</p>

Table 3 Cases of small-scale biomass-fired CCHP systems with ICEs with 300-1000 kW nominal power

Ref.	Max. Outputs	Biomass	Prime mover	Refrigerat ion	Software/ Location	Key Findings
[58] [59]	Electricity: 446 kW  Chilled Water: 1,804 kW  Heating: 595 kW  Hot Water: 335 kW	Gasification: Straw (0.297 kg/s)	ICE	Two-Stage LiBr-H <sub>2</sub> O Absorption chiller (AC)	DEST software	Efficiencies: Summer/ Winter/ Transition: Energy: 50%/ 37.8%/ 37% Exergy: 6.23%/ 12.51%/ 13.79%  Biomass costs greatly influence unit costs of outputs  Greatest exergy destruction in gasification system (~ 70%)
[60] [61]	Electricity: 1,000 kW  Heating: ~2,000 kW  Cooling: 2,800 kW (rated refrigerating capacity)	Anaerobic digestion: • straw • guano • kitchen waste • sludge  Gasification • Wood • Coconut • straw	ICE (gas)	AC	Model	More CH <sub>4</sub> in anaerobic digested gases, more H <sub>2</sub> in gasified gases  Anaerobic digested gases generates more electricity and less heat  For both gasification and anaerobic digestion optimal values were calculated for output work of engine, compression ratio, PESR and exergy efficiency with different temperature ratio and exhaust gas energy level
[23]	Electricity: 346 kW  Heating: 1,063 kW  Cooling: 1,010 kW	Wood chips (gasified)	Not specified	AC	MATLAB model for a travel hotel in Harbin, China	Compared to separated production:  • 90.4% CO <sub>2</sub> saved • 17.7% higher primary energy consumption due to lower energetic efficiency • Annual total cost saving: 45.4 %

Table 4 Cases of small-scale biomass-fired CCHP systems with ICEs with less than 40 kW nominal power

Ref.	Max. Outputs	Biomass	Prime mover	Refrigeration	Software/ Location	Key Findings
[62]	<p>Electricity: 9.9 kW</p> <p>Heating: 4.5 kW</p> <p>Ice: 40 kg/h = 4 kW</p> <p>Clean water</p>	Jatropha and Pongamia oils (3L/h)	ICE (Diesel – Lister Petter CI Engine)	Adsorption refrigerator	Experiment	<p>Thermal efficiency: 63%</p> <p>Payback: 1.7 – 3.2 years</p> <p>Low GHG emissions but also low COP with adsorption refrigerator</p> <p>Clean water produced through multiple-effect distillation</p>
[63]	<p>Electricity: 6.5 kW</p> <p>Hot Water: ~12.3 kW</p> <p>Cooling: 15 W</p>	Croton megalocarpus oil	Dual-use ICE (compression ignition)	AC + PCM storage	Experiment	<p>Overall efficiency: 76% with bio oil (compared to 88% with diesel)</p> <p>Electric efficiency: 25-30%</p> <p>Higher specific fuel consumption with bio oil compared to diesel due to maladjusted injection settings</p> <p>More heat recovery with biooil due to longer injection duration</p> <p>Preheating could lead to higher efficiency and less particulate emission</p>
[64]	<p>Electricity: 15 kW</p> <p>Heating: ~17 kW</p> <p>Cooling: ~4 kW (in trigeneration mode)</p>	Ligno-celulosic/ eucaliptus wood (20 to 30 kg/h) gasified in a downdraft gasifier	ICE	LiBr-AC	Analysis based on experiments in Zaragoza, Spain	<p>Highest energy efficiency achieved: 51.42%</p> <p>Feasible as alternative for rural areas with shortage of petroleum and abundance of biomass</p> <p>Electric efficiency of 21.42%</p>
[65]	<p>Reference system (summer mode):</p> <p>Electricity: 1.5 kW</p> <p>Heating: 19.6 kW</p> <p>Cooling: 9.1 kW</p>	B-100 biodiesel	ICE	Vapour compression chiller	Thermo-dynamic model based on data from experiments and literature	<p>Comparison between conventional diesel and biodiesel:</p> <ul style="list-style-type: none"> <li>• Primary energy consumption decreased by ~ 50%</li> <li>• CO<sub>2</sub> emissions by ~ 95%</li> </ul> <p>Case study for a commercial building complex in Hong Kong suggest a switch to heat-driven chillers</p>

Table 5 Cases of small-scale biomass-fired CCHP systems with ICEs with 40-100 kW nominal power

Ref.	Max. Outputs	Biomass	Prime mover	Refrigeration	Software/ Location	Key Findings
[66]	Electricity: ~40 kW  Heating: ~60 kW  Cooling: not specified	Biomass-derived gases (gasification vs. pyrolysis vs. anaerobic digestion) mixed with LPG	ICE (gas)	Mixed effect AC	Mathematical Model	Addition of LPG to all three types of gases increases exergy and energy efficiency and decreases CO <sub>2</sub> emissions for gases from gasification and pyrolysis, but from anaerobic digestion  Lower heating value and air fuel ratio of the biomass-derived gas affects the impact of LPG the most
[67] [68]	Electricity: 50 kW  Heating: 120 kW  Cooling: 20 kW (in optimized case)	Wood chips (gasified by fixed bed gasifier)	ICE	AC (COP: 0.8)	Matlab model for Italian building cluster	Electrical efficiency: 20.6% Thermal efficiency: 40.5%  Upgrade of a CHP system  Thermal energy storage (of not specified type) considered, but has a negligent effect on economic performance  Size of AC is the most important factor for feasible investment
[69]	Electricity: 56 kW (shaft power)  Heating: ~110 kW  Cooling: ~ 60 kW	LPG mixed with biomass-derived gases: <ul style="list-style-type: none"><li>• Gasification</li><li>• Pyrolysis</li><li>• Anaerobic digestion</li></ul>	ICE	Mixed effect absorption chiller (COP: up to 0.94)	Mathematical model (no software mentioned)	Electrical efficiency: 30%  Simulating the effects of adding LPG to biomass-derived gases: <ul style="list-style-type: none"><li>• better energetic and exergetic performance for gasification and pyrolysis derived gases</li><li>• worse energetic and exergetic performance for gases from anaerobic digestion</li></ul>

Table 6 Cases of small-scale biomass-fired and solar-assisted CCHP systems with ICEs

Ref.	Max. Outputs	Biomass	Prime mover	Refrigeration	Software/ Location	Key Findings
[70] [71]	Electricity: 987 kW  Hot water: 1,988 kW  Cooled Water: 843 kW  Dry Air: 482 kW	Rice husk (1,400 kg/h – gasified)	Gas ICE + solar collectors connected to gasification	LiBr-H <sub>2</sub> O AC + liquid desiccant cooler	Aspen plus	Most exergy destroyed in gasifier and engine  Exergy efficiency: 19.21%  Energy efficiency: 77.4% (when only considering positive influence of solar energy)  Electric efficiency: 15%  Air equivalence ratio, steam/biomass ratio and air preheating have significant effects on gasification  Solar thermal energy can decrease biomass consumption by 29%  Annual cost savings of up to 25.9% compared to separate systems
[72] [73]	Electricity: 1,000 kW  Heating: 580.2 kW  Cooling: 67.9 kW	Biogas from cattle and pig manure	ICE (750 kWe) + PV cells (255 kWe)	Adsorption Chiller	Model (example given for an agricultural process facility)	Thermoeconomic analysis (TEA) and thermos-ecological analysis (TEC)  Exergy efficiency of adsorption chiller considerably low  Electric efficiency of ICE: 47.9%  ICE provides 64.7% and PV panels 8.9% of consumer's electricity demand, rest is provided by electric grid
[74]	Electricity: 100 kW  Hot water: 102.7 kW  Cooled water: 197.2 kW	Wood chips (gasified)	ICE (gas) + solar- evacuated thermal collectors	Mixed effect LiBr- AC (using engine air exhaust and solar hot water) (~COP 1)	EES Model	Solar collectors to heat up waste stream after ICE for absorption chilling  Using a higher biomass to solar energy ratio leads to higher efficiency but also to more carbon emissions  Exergetic efficiency mostly influenced by biomass subsystem  Overall system energy efficiency: 57.9%  Solar subsystem energy efficiency: 47%  Bio subsystem energy efficiency: 61%
[75]	Electricity: 95 kW  Heating: unspecified  Cooling: 325 kW	Vegetable oil (rapeseed oil)	ICE + parabolic through collectors	LiBr-H <sub>2</sub> O double- stage AC (~COP 1.4)	Model in TRNSYS	Solar collectors to heat up waste stream after ICE for absorption chilling  PESR: 93%  Discounted payback period of around 9 years, highly dependent on pure plant oil price

## 4.2 Fuel Cells

With no moving parts and no combustion, fuel cells (FCs) are a completely different type of prime mover from their mechanical counterparts, excelling in environmental impact and load flexibility [45]. However, the environmental benefit is rapidly equalized when considering the energy consumption and GHG emissions for producing hydrogen or methane as fuel. FCs generally have a high electric efficiency and thus a lower heat recovery and bio-fueled CCHP systems using FCs which can serve loads from less than 1 kW to more than 1,000 kW have been demonstrated [5,21,76,77]. A huge disadvantage for FCs is the need of very high fuel purity levels. Research is therefore being conducted in techniques to remove

sulphur, halogens, alkali and siloxanes from biogas, while for gasification systems, an efficient technology to remove tar is still the main obstacle for commercialization with investigations still ongoing [78–81]. Table 7 shows a summary of the investigated small-scale biomass-fired and solar-assisted CCHP systems. There is also a case of system with an Organic Rankine Cycle (ORC) enhanced by a FC (see Table 11).

Table 7 Cases of small-scale biomass-fired and solar-assisted CCHP systems with fuel cells

Ref.	Max. Outputs	Biomass	Prime mover	Refrigeration	Software/ Location	Key Findings
[82]	Electricity: ~220 kW Heating: 69.9 kW Cooling: 22.1 kW	Not specified (gasification)	SOFC + ORC turbine (with toluene)	LiBr-AC (~COP 0.7-0.8)	EES software	Energy : 78.8% Exergy efficiency: 50.6%  Comparing various gaseous fuels from different gasifier systems:  1. Bubbling fluidized bed 2. Circulating fluidized bed 3. Dual fluidized bed  Syngas from bubbling fluidized bed gasifier shows highest thermodynamic performance with a net system energy efficiency of 60%
[83] [84] [85]	Electricity: ~329 kW SOFC + ~89 kW ORC Heating: ~646 kW Cooling: ~51 kW	Syngas from gasification (no more specification)	SOFC and ORC with two turbines + parabolic through solar collectors super-heating ORC circuit	LiBr- AC	EES software	Highest system energy efficiency: 85.1% Highest system exergy efficiency: 32.62%  Highest exergetic losses in SOFC, ORC evaporator and solar panels  Solar assistance increases efficiency by up to 16% and adds 89 kW electricity generation  SOFC input parameters (fuel utilization ratio, recirculation ratio, stack temperature) influence system significantly  Exergetic efficiency up to 25% higher compared to power-only cycle
[86]	Electricity: 630 kW Heating: 1185 kW Cooling: 320 kW	Downdraft gasification from lignocellulosic biomass (pine wood residues)	SOFC + Solar thermal collectors for heating	Silica-Gel Adsorption chiller (and electric chiller)	ASPEN model with TRNSYS environment	Total energy efficiency: 56% Electric efficiency: 23%  Three different system configurations: SOFC + adsorption chiller SOFC + electric chiller SOFC + electric chiller + solar collectors  Hot water storage considered in all cases  Adsorption chiller based on 10 kW commercial unit  Low efficiency due to cold gas efficiency in gasifier  PSER: 50% CO <sub>2</sub> -emissions savings: 5000 t/y

### 4.3 Stirling Engines

Compared to the previously mentioned ICs, Stirling engines (SEs) have the potential to operate more quietly, with better partial load performance and low maintenance costs due to less moving parts [12,48,87]. They can satisfy electric loads from a few kW up to 150 kW, while also being able to provide high temperature heat exhausts with high thermal efficiency [2,21,88]. Especially in the context of

biomass usage, SEs show great fuel flexibility being able to be driven by direct combustion of biomass or by combustion of syn- or biogas, because the heat can be applied externally [89]. Uncertainties in operating SEs and high investment costs hinder further use of SE technology [89]. A summary of the investigated small-scale bio CCHP systems with Stirling engines is given in Table 8.

There are few cases using SEs as prime movers in the context of small-scale CHP and CCHP systems, which however report promising results for reducing GHG emissions due to high energetic efficiencies [89–97]. However only few cases of such systems fueled explicitly with biomass could be found within the literature of scientific journals, which are summarized in Table 8.

Table 8 Cases of small-scale biomass-fired CCHP systems with Stirling engines

Ref.	Max. Outputs	Biomass	Prime mover	Refrigeration	Software/ Location	Key Findings
[98]	SE: Electricity: 3.2 kW  Heating: 10.9 kW  Cooling: 4.4 kW  Compared with an ICE: Electricity: 5.2 kW  Heating: 7.6 kW  Cooling: 2.2 kW	Option 1: Wood pellets SE  Option 2: willow chips SE  Option 3: biodiesel ICE	SE vs. ICE	LiBr-AC	Model in Eclipse	SE: Overall efficiency 67% (electric efficiency 20%)  ICE: Overall efficiency 60.1% (but higher electric efficiency with 30%)  Potential of saving 6.1 to 8.9 tonnes of CO <sub>2</sub> per year  Batteries with a storage capacity of 13 kWh were also modelled into the system  SE option more feasible when electricity/heat demand ration is low, otherwise ICE option more feasible
[88]	Electricity: 0-15 kW  Heating: not specified  Cooling: not specified	Wood chips	SE	AC	EnergyPlus software using data for a small office in Atlanta, GA, USA	Reference case with 7 kW SE  Analysis of primary energy consumption and operational costs compared to the reference system  Identifying SE size, heat exchanger, AC, and fuel costs as most important variables for economy

#### 4.4 Organic Rankine Cycles

Compared to ICE and conventional turbines, Organic Rankine Cycles (ORCs) perform better when run under partial load, although there can be significant losses [48]. ORCs are a potential key technology for achieving successful commercialization of small-scale CCHP systems [87]. ORCs have been proven to successfully satisfy loads from 100 kW up to 2 MW, while even smaller systems are currently researched in a pre-commercial status [47,99]. Larger systems can reach electric efficiencies of up to 35% and overall energetic efficiencies of around 85%, but systems smaller than 100 kW reach only lower electric efficiencies of about 15% [100]. A key decision for designing an ORC system is the choice of the organic working fluid, where several characteristics have to be considered: heat transfer properties, environmental impact, safety issues, chemical stability, pressure requirements, costs and availability, molecular weight, freezing point, curve of saturation, thermodynamic performance, corrosiveness [47,99,101]. A detailed overview of working fluids for low-temperature organic Rankine cycles can be found in Saleh et al. [102]. As mentioned before, several studies tested the combination of ORC with FCs (s. chapter 4.2), but there are also numerous studies on small-scale CCHP systems relying solely on ORCs. In Table 9-Table 11, the cases of small-scale biomass-fired and solar-assisted CCHP systems using ORCs are summarized.

*Table 9 Cases of small-scale biomass-fired and solar-assisted CCHP systems with ORCs with less than 50 kW nominal power*

<b>Ref.</b>	<b>Max. Outputs</b>	<b>Biomass</b>	<b>Prime mover</b>	<b>Refrigeration</b>	<b>Software/ Location</b>	<b>Key Findings</b>
[103]	<p><i>Electricity: 0.5 kW</i></p> <p><i>Heating: 9.6 kW</i></p> <p><i>Cooling: 6.5 kW</i></p>	<p><i>Wood pellets (direct combustion)</i></p>	<p><i>ORC turbine</i></p>	<p><i>Liquid desiccant cooler (Potassium formate - HCOOK)</i></p>	<p><i>Experiment</i></p>	<p><i>Overall energetic efficiency of CHP: 83%</i></p> <p><i>Overall energetic efficiency of trigeneration: 84.4%</i></p> <p><i>Thermal/electric COP of cooler: 0.86/7.7</i></p> <p><i>Working fluid: HFE7100 (non-flammable, non-toxic, low GHG potential)</i></p>
[104]	<p><i>Electricity: 1,42 kW</i></p> <p><i>Heating: 53,5 kW</i></p> <p><i>Cooling: 5 kW</i></p>	<p><i>SRC willow pellet (direct combustion)</i></p>	<p><i>ORC expander (R245fa) + parabolic-through collectors (super-heating after reactor)</i></p>	<p><i>Vapour compression chiller</i></p>	<p><i>EES Model for a household</i></p>	<p><i>Payback: 7 years (average case)</i></p> <p><i>Estimated exergy efficiency of about 7%</i></p> <p><i>Energetic and economic analysis distinguishing between summer and winter mode</i></p>
[105]	<p><i>Electricity: 27.5 kW</i></p> <p><i>Heating: 180 kW</i></p> <p><i>Cooling: 5 kW</i></p>	<p><i>Not specified</i></p>	<p><i>ORC</i></p>	<p><i>AC</i></p>	<p><i>Calculations for a supermarket in Vitoria, Spain, based on experiments</i></p>	<p><i>Based on a commercial ORC unit by Rank® with HFC-245fa as working fluid</i></p> <p><i>CO<sub>2</sub>-emissions savings: 285 t/y</i></p>
[106]	<p><i>Restaurant case demand:</i></p> <p><i>Electricity: 35 kW</i></p> <p><i>Hot water: 50 kW</i></p> <p><i>Cooling: 10 kW</i></p> <p><i>Orange processing case demand:</i></p> <p><i>Electricity: 110 kW</i></p> <p><i>Hot water: 115 kW</i></p> <p><i>Cooling: 135 kW</i></p>	<p><i>Wood-beech (direct combustion)</i></p>	<p><i>Two ORC-expanders</i></p>	<p><i>Ammonia-water AC</i></p>	<p><i>RefProp 9.0 model</i></p>	<p><i>R134a and R407f selected as working fluids</i></p> <p><i>Trigeneration system with two expanders and two compressors allows for more flexible control of thermal and electric services</i></p> <p><i>The configuration is profitable in the smaller restaurant case, but unprofitable for the larger orange processing case</i></p>

Table 10 Cases of small-scale biomass-fired CCHP systems with ORCs with 50-400 kW nominal power

Ref.	Max. Outputs	Biomass	Prime mover	Refrigeration	Software/ Location	Key Findings
[107]	<p>Electricity: 204 kW</p> <p>Heating: 972 kW</p> <p>Cooling: 226 kW</p>	<p>Direct combustion:</p> <ul style="list-style-type: none"> <li>Willow chips</li> <li>Straw</li> <li>Rice husks</li> </ul>	ORC Turbine (R245fa)	AC	Eclipse Model	<p>Comparing three different biomass inputs with the result that all three fuels are feasible</p> <p>Cogeneration has higher efficiency than trigeneration</p> <p>Payback period of trigeneration slightly lower than for cogeneration but much lower than for only power</p> <p>Fuel cost is an important factor</p> <p>Similar study with ICE engine is shown in Table 2</p>
[108]	<p>Electricity: 280 kW</p> <p>Heating: 1,500 kW</p> <p>Cooling: 500 kW</p>	Combustion: Oil tree residues	ORC (fluid: MDM)	AC	Model for an airport in Bari, Italy	<p>Energetic efficiency for heat and power: 71.8%</p> <p>Energetic efficiency for cooling and power: 31.2%</p> <p>Payback period of 6 years</p> <p>Yearly CO<sub>2</sub>-savings: 1,176 t/year</p>
[109]	<p>Electricity: 315 kW</p> <p>Heating: not specified</p> <p>Cooling: 780 kW</p>	Pine Chips (direct combustion)	ORC	AC	SimaPro7.1 Model for the WALQA Technology park in Huesca	<p>Energetic, economic and environmental investigation of different trigeneration configurations:</p> <ul style="list-style-type: none"> <li>Parallel (boiler connected to ORC, AC and heat-exchanger)</li> <li>Cascade (boiler only connected to ORC)</li> <li>Separate energy service production</li> </ul> <p>Cascade configuration leads to highest energetic efficiencies.</p> <p>Using the Life Cycle Assessment methodology for environmental impact</p>
[110]	<p>Electricity: 350 kW</p> <p>Heating: 1,644 kW</p> <p>Hot Water: 0.52 kg/h</p> <p>Cooling: 2,000 kW</p> <p>Hydrogen: 1.2-1.5 kg/h</p> <p>Fresh Water: 1-1.4 kg/h</p>	Pine Saw Dust (0.2-0.4 kg/s – direct combustion)	ORC Turbine	Double-effect AC	Model using genetic algorithm optimization	<p>Exergetic efficiency: 32-34%</p> <p>Increase in biomass flow -&gt; decrease in exergy efficiency</p>

*Table 11 Cases of small-scale biomass-fired and solar-assisted CCHP systems with ORCs with 400-1000 kW nominal power*

<b>Ref.</b>	<b>Max. Outputs</b>	<b>Biomass</b>	<b>Prime mover</b>	<b>Refrigeration</b>	<b>Software/ Location</b>	<b>Key Findings</b>
[111] [112]	Electricity: 600 kW  Heating: 3,750 kW  Cooling: 300 kW	Pine Saw Dust (direct combustion)	ORC turbine	Single-effect AC	Proposed System modelled in EES	Most exergy destroyed in biomass burner (55%) and ORC evaporator (38%)  System sensitive to ORC evaporator temperature and pump inlet temperature  System insensitive to turbine inlet pressure  Maximum trigeneration exergy efficiency 28%  Maximum trigeneration energetic efficiency: 89%
[113]	Electricity: 671 kW  Hot water: 2,617 kW  Cooling: 611 kW  Hydrogen: 3.14 kg/day	Pine sawdust (0.3 kg/s – direct combustion)	ORC Turbine (n-octane)	LiBr-AC	Model and Simulation	Exergetic efficiency: 22.2%  Exergy destruction highest in combustor and ORC evaporator  System affected mostly by pinch point temperature, ORC inlet pressure and ORC inlet temperature
[114] [115] [116]	Electricity: 400-800 kW  Heating: not specified  Cooling: not specified	Pine sawdust (direct combustion)	ORC Turbine (in some cases after SOFC)	Single-effect AC	EES	Comparing three different configurations: <ul style="list-style-type: none"> <li>• Methane-fueled SOFC before ORC</li> <li>• Biomass-boiler before ORC</li> <li>• Solar-thermal boiler before ORC</li> </ul> Electrical efficiency of SOFC-system highest with 19%,  Trigeneration energetic efficiency highest in biomass and solar system with both 90%  Solar trigeneration system performs best in terms of thermoeconomics and ecology
[117]	Electricity: 1000 kW  Hot water: not specified  Cooling: not specified	Mixture of agricultural and forest biomass (direct combustion)	ORC	AC (single- effect)	GIS-Data from BIORAISE	Max. electrical efficiency: 15% Max. thermal efficiency: 74%  Studying the potential of such an ORC-system in various regions of Spain for villages of around 10,000 inhabitants  Apart from regional climate, fuel ability dictates profitability  CCHP profitable in warm climates, CHP in cold climates

#### 4.5 Steam and Gas Turbines

Conventional steam and gas turbines can serve electric loads of several hundreds of MW, but internally fired gas turbines are rarely smaller than 500 kW while steam turbines are rarely smaller than 50 kW [21]. Both types of turbines suffer significant losses in efficiency when used in partial load mode, so steam and gas turbines are an inconvenient choice for flexible small-scale CCHP systems [26].

However, the high temperature of exhaust gases holds high potential for further usage for heating and cooling applications. Studies suggest that small-scale gas turbines with 100-600 kW electric output are economically disadvantageous compared to internal combustion gas engines, but future technologies could change this status [118]. A summary of the two previous cases is given in Table 12.

There are certain studies that investigate the use of considerably small steam and gas turbines in CCHP systems, providing useful insights for other small-scale systems, especially run with micro-turbines as a prime mover. It can be found that for smaller systems (2 – 3.5 MW) the highest exergy losses occur in the furnace [119] and that the values of energy efficiency of steam and gas turbines are similar for CHP systems [120]. One case where a gas turbine cycle of unspecified nominal power is combined with two ORC cycles has been mentioned in chapter 4.4.

#### **4.6 Micro Turbines**

Micro-turbines are another promising technology on the brink of mass-scale commercialization for CHP and CCHP systems [121]. Micro-turbine sizes range from a few kW to several hundreds of kW, while even smaller capacities are being investigated. Apart from the disadvantages mentioned in Table 1, there is also the need for high quality fuels when run on bio- or syngas [21]. A solution to this problem could be externally fired micro-turbines, where studies suggest that syngas containing more tar can lead to higher electric efficiencies [122]. Simulations of a biomass CHP system comparing an internally fired micro-turbine fueled with syngas to an externally fired micro-turbine driven by direct combustion could show that the latter reaches higher electric efficiency and higher overall efficiency with less biomass consumption [123]. In a case study for a polygeneration system, a 100 kW micro turbine was driven externally using direct combustion of biomass and natural gas [124]. It could be shown that with a mixture of 70/30 for bio/natural gas fuel, an electric efficiency of 21.8% could be reached, but a further increase of biomass would lower efficiency. Two cases of a trigeneration system using a micro gas turbine are presented in Table 12.

Table 12 Cases of small-scale biomass-fired CCHP systems with steam, gas and micro turbines

Ref.	Max. Outputs	Biomass	Prime mover	Refrigeration	Software/ Location	Key Findings
[125]	<p>Electricity: 1.1 MW</p> <p>Cooling: 0.26 MW</p> <p>Net utility Heating: 0.22 MW</p> <p>Ethanol: 3.38 t/h</p>	<p>Fluidized Bed gasifier (1 t/h):</p> <ul style="list-style-type: none"> <li>Rice straw</li> <li>Sugarcane</li> <li>Coconut fibres</li> </ul>	Gas Turbine + Steam Turbines	Vapour absorption refrigeration	Aspen Plus	<p>Polygeneration system for Ethanol production plant</p> <p>Comparison of different Biomass inputs and outputs:</p> <ol style="list-style-type: none"> <li>Rice straw</li> <li>Sugarcane bagasse</li> <li>Coconut fibre dust (highest output)</li> </ol> <p>Fuel energy saving ratio between 16-27%</p> <p>Payback period: 5.25 years</p> <p>Also CO<sub>2</sub> capture technologies proposed</p>
[126]	<p>Electricity: 172.28 kW</p> <p>Heating: 488.51 kW</p> <p>Cooling: 256.21 kW</p>	Corn Stover (gasified) + Coal	Two Gas Turbines in cascade utilization	Double-effect Li-Br AC (COE:1.1)	Aspen Plus Software	<p>Chemical looping of coal and biomass in the same gasifier</p> <p>When co-firing with a ratio of 50/50, an energy efficiency of 60.16% and 57.46% can be reached in summer and winter, respectively</p> <p>An increase in biomass firing leads to a decrease in energy output, but an increase in PESR</p>
[127]	<p>For one MGT:</p> <p>Electricity: 30 kW</p> <p>Heating: 57 kW</p> <p>Cooling: 40 kW</p>	Biogas (supported by natural gas)	Micro Gas Turbine	<p>Single and double-effect AC,</p> <p>Ammonia-water chiller</p> <p>Compression chiller</p>	Hysys Process Software	<p>Case study for sewage treatment plant with comparison of several configurations using various refrigeration technologies</p> <p>Double-effect AC best economic and energetic performance</p> <p>Several micro turbines can be stacked for higher electricity generation</p>
[128]	<p>Electricity: 100 kW</p> <p>Heating: 333 kW</p> <p>Cooling: 110 kW</p>	Not mentioned (Co-firing natural gas – direct combustion)	Micro turbine	LiBr-H <sub>2</sub> O single-effect AC	Gate-Cycle®	<p>Thermal efficiency 46-38%</p> <p>Electric efficiency 30-19%</p> <p>Global energy efficiency of 30-40% unsatisfactory for Italian high efficiency system requirements</p> <p>Trigeneration only viable in high-cooling demand areas (hot areas)</p> <p>Mix of 50/50 biomass gas/natural gas shows best results considering energy conversion efficiency, investment and fuel costs</p>
[129]	<p>Electricity: 131 kW</p> <p>Heating: 230 kW</p> <p>Cooling: 187 kW</p>	Corn Stover gasified with coal	Steam turbine after gasifier and gas turbine using syngas	Double-effect LiBr- AC	Aspen Plus	<p>Energy efficiency (winter/summer): 63%/67%</p> <p>Exergy efficiency (winter/summer): 26%/24%</p> <p>Increasing the share of biomass from 0 to 50% leads to efficiency losses of around 25%, but leads to CO<sub>2</sub> reduction of 300% by using carbon capture technology</p>

#### 4.7 Solar Extensions

In comparison to bioenergy, solar energy has an even bigger potential with negligible operational costs as there are no fuel costs [130]. With the costs for PV cells plummeting from \$76.67 per Watt in 1977 to \$0.36 per Watt in 2014 and the use of solar thermal energy always having been simple and cheap, solar energy becomes more and more competitive [17]. The key findings and characteristics of a solar-driven CCHP system with an auxiliary biomass boiler are shown in Table 13. Another study considering a purely solar-driven CCHP system based on an ORC was mentioned in Table 11.

Table 13 Cases of small-scale solar-driven CCHP systems with auxiliary biomass boiler

Ref.	Max. Outputs	Biomass	Prime mover	Refrigeration	Software/ Location	Key Findings
[16] [131]	Electricity: variable with solar input  Heating: variable with solar input  Cooling: variable with solar input  Potable water	Wood chips (direct combustion)	Solar thermic and PV system with auxiliary biomass boiler	LiBr-H <sub>2</sub> O AC	TRNSYS for a system placed in Naples, Italy	Electric Efficiency: up to 23%  Thermal Efficiency: up to 60%  Payback time of 13.6 years saving 0.26 million €/year  Very effective in summer, but very ineffective in winter  The models prove that such a system is not economically sensible except on disadvantaged areas like small islands

In direct comparison with bioenergy or fossil fuels, solar energy is disqualified for fueling CHP or CCHP systems on its own [114]. It is therefore necessary to combine solar energy with either advanced electric and/or thermal storages or with other energy sources like biofuels [17,20]. Using solar energy this way in a CCHP system can lead to significant reductions of CO<sub>2</sub> emissions and to higher energy utilization compared to stand-alone as well as CHP systems [132]. For solar extensions in bio-driven small-scale CCHP systems, there are five main configurations in which the solar energy can enhance the performance of the whole system (as illustrated in Figure 2):

1. Solar thermal energy can enhance the biochemical or thermochemical conversion of biomass into fuel for the prime mover to reduce biomass consumption (example case [133]).
2. Solar thermal energy can be used to preheat the air intake of the prime mover, which then will increase the efficiency of a combustion process (example case [134]). This is quite common for gas turbines and bigger systems.
3. Solar thermal energy can be used to produce steam directly and to temporarily run the prime mover without any usage of biomass (example case [114,133]). This configuration is often applied in systems using ORCs.
4. Solar thermal energy can be used to reheat any stream after the exhaust for enhancing the heat supply or the thermally activated cooling process. This way, when electricity demand is low, the heat and cooling demand can still be satisfied in partial mode and biomass can be saved (example case [83]).
5. PV cells can provide electric energy and thus the prime mover has to satisfy less electric demand, so that biomass can be saved (example case [135]).

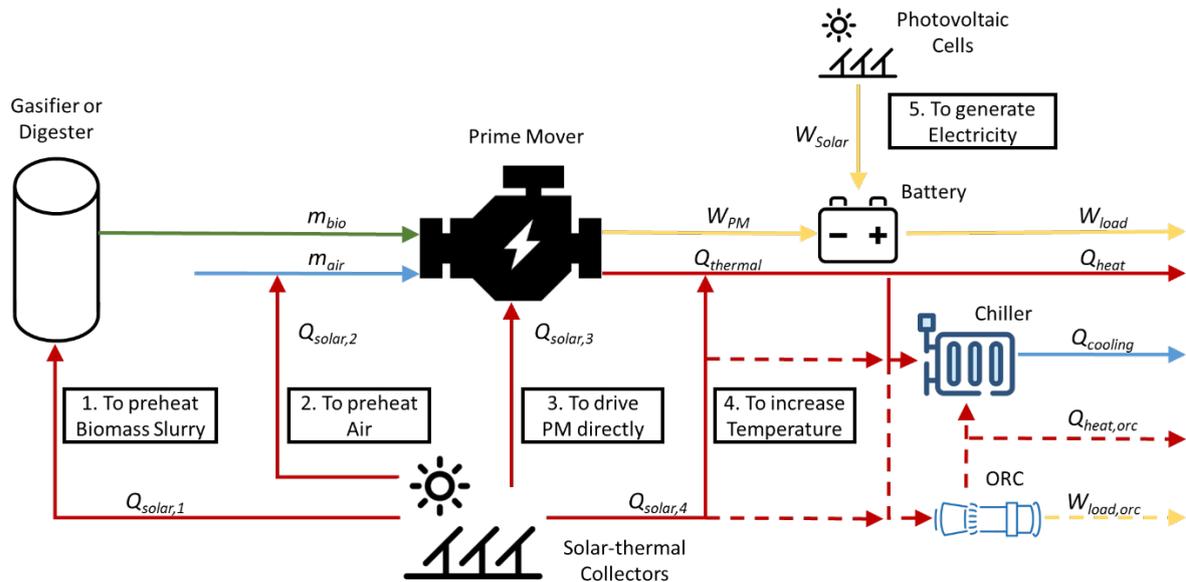


Figure 2 Possible solar extensions in biomass-fired small-scale CCHP systems

This figure does not represent PV/thermal (PVT) components, which are essentially a combination of PV and solar thermal technology. Such PVT collectors are still not reliable and cost-effective enough for market penetration, but are promised to have huge potential in the near future [136]. As for Figure 2, the application of PVT collectors in a small-scale CCHP system would be a combination of any of the options 1-4 with option 5.

Essentially all five configurations imply a temporary decrease in biomass consumption. This has several advantages for the system:

- Operational costs can be lowered as there will be less costs for the biomass itself and the biomass transport to the system [24].
- It leads to a better short-term CO<sub>2</sub> balance, because the combusted biomass needs several years to be reincorporated into the biomass cycle, as well as to a better long-term CO<sub>2</sub> balance, because less energy will be used in transport vehicles.
- In some cases, the possibility to run systems only on solar energy can be a fallback option for stand-alone systems in case of a shortage of biomass supply.

However, there are also certain drawbacks to be considered:

- The installation of additional solar units leads to higher capital costs.
- The installation of additional solar units leads to higher complexity for the design and operation of the CCHP.

## 5 Cooling Units and Storage Systems

Seizing the exhaust heat from a prime mover by connecting it with a cooling unit can lead to higher profitability [137]. Similarly energy storage technologies improve the economic viability of small-scale CCHP systems [138]. It is therefore imperative for a clear picture of small-scale CCHP systems to know about the most important thermally activated cooling technologies and storage technologies.

### 5.1 Thermally Activated Cooling Technologies

Although CHP systems have been in use since the installation of the first commercial power plant, CCHP systems have only experienced very slow development until the oil crisis in 1979 [139]. Since then the commercialisation of thermally activated cooling units accelerated and with it the development of CCHP systems. A commonly used parameter to describe the efficiency of refrigeration units is the coefficient of performance (COP), which is the cooling capacity of the unit divided by its heat or electricity consumption [74].

Three different thermal refrigeration technologies can be applied in CCHP systems [140]:

- Absorption chillers (ACs)
- Adsorption chillers
- Desiccant chillers

ACs are the most commonly used type of thermally activated chillers, especially Lithium Bromide–Water (LiBr) and Water-Ammonia chillers [12,20,140]. In LiBr-chillers evaporating a low pressure, working fluid (water) in an evaporator “draws” heat and hence cools the surrounding. The gaseous water is then absorbed by the LiBr-salt solution in the absorber, the mixture reheated to evaporate the water and the water then condensed. The process scheme of a single-effect absorption refrigerator is illustrated in Figure 3.

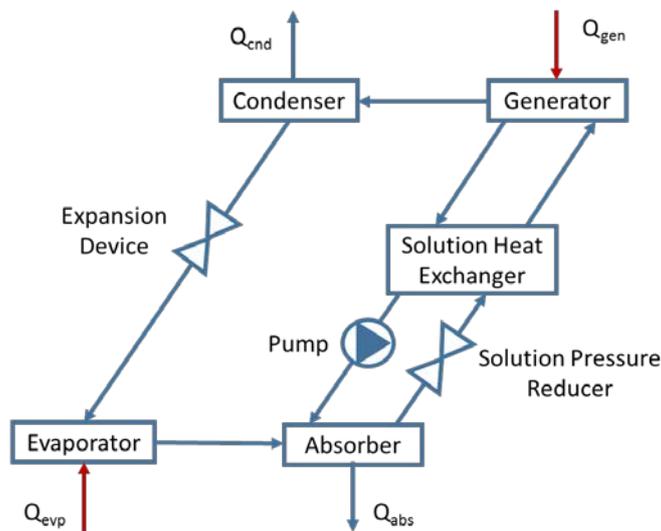


Figure 3 Simplified process of Single-Effect Absorption Refrigeration (based on [149])

LiBr-ACs can be driven by pressurized hot water with more than 120 °C or gases with more than 400°C. Their advantages are the familiarity with the technology, the low investment costs and the high COP. Ammonia-water chillers work under the same basic principle as LiBr-chillers, but due to the lower evaporation temperature of ammonia, they can be used for lower temperature applications and in smaller sizes [12,139,140].

Another technology, which can be applied to low-heat sources and which is more environmentally friendly, is adsorption chilling. The basic working principle is similar ACs; however, the working fluid is only adsorbed to the surface of the adsorbent. The most common adsorption chillers use silica gel, as this type has been successfully commercialized [140]. Drawbacks of adsorption chillers are higher investment costs [12] and lower COP [139]. Nonetheless, they are sometimes chosen for small-scale CCHP systems (see Table 4, Table 7 and Figure 4).

A novel technology emerging on the market is desiccant cooling, where either a desiccant wheel or a liquid desiccant dries and heats up an incoming air stream, which can then be cooled down by surrounding air. In an evaporator the air then is rehumidified while its temperature is lowered immensely [141]. Desiccant cooling can be advantageous in small-scale residential systems due to its low maintenance costs and combined control of humidity and temperature [140]. Two cases using desiccant cooling could be found (see Table 6 and Table 9). Apart from thermally driven refrigeration systems, vapour compression chillers driven by electric or mechanical energy are often chosen in CCHP systems [5]. The advantages of vapour compression chillers are high COP and higher reliability due to independence from the thermal heat of the system, but they are less environmentally friendly, emit more noise and require more maintenance [2,32].

## 5.2 Storage Units

In the context of solar energy, batteries are often identified as the means to enable versatility of solar energy sources, hence making solar energy a feasible alternative to conventional energy sources [142]. The worldwide energy capacity of batteries for utility-scale energy storage applications is predicted to rise from 412 MWh in 2014 to 51,200 MWh in 2023, which implies an annual growth rate of more than 71% [143]. A plurality of battery technologies is currently investigated and a review of all of these is beyond the scope of this paper. Hence, it is here referred to recent reviews of battery technologies for further information [144,145].

Concerning thermal storages, simple water tanks are the most common and simplest solution, as water has a high specific capacity and the installation of a water tank is an easy and cheap task. A more compact way to store thermal energy can be provided by phase change materials (PCM). These materials use the energy needed for a phase change to either store or absorb heat [146]. Apart from storing energy for direct heating or cooling purposes, the heat can also be stored to preheat biofuels at a constant temperature and hence help with the start-up of an engine as well as to increase its efficiency [147].

## 6 Results and Discussion

As can be seen in Figure 4, most studies were simulation models, which themselves were often based on synthetic data or data collected from subsystems. Although there are some experimental studies, it seems that there is a general lack of real-life data in this area [148]. This may be due to an underestimation from researches of increased maintenance works and complexity, as operators may value the simplicity of a system highly. Additionally, as with every new technology, the overall lifetime of the components as well as their decay over time cannot be determined based on operation experience. There might be more real-life examples outside of scientific literature whose insights have not been documented for the scientific community. It was also found that nearly one out of four cases considers solar-assistance to enhance the biomass-fired systems. The potential of combining these two energy sources has thus been recognised.

In the cases of biomass-fired CCHP systems investigated in this paper, downdraft gasifiers seem to be the most practical choice for gasification due to the high quality of the syngas [40]. These gasification systems are mostly below 500 kW nominal power, as smaller gasification systems are generally more cost-effective than larger ones due to lower maintenance costs [10]. In the case studies investigated in this paper, anaerobic digestion is also an often-used technology. While for off-grid CCHP systems thermal and electric storage units are usually indispensable, for on-grid systems they are often overlooked in models despite their potentially high impact on economics [18]. If the use of a thermal storage system was stated at all, it was usually water tanks and only in one case PCM.

It could be found that LiBr-absorption is the most often used technology in the investigated cases of biomass-fired and solar-assisted CCHP systems. Ammonia-water chillers have also been proposed often, while for some models the concrete working pair for the AC has not been specified. As shown in Figure 4, AC technology is used significantly more often than other technologies.

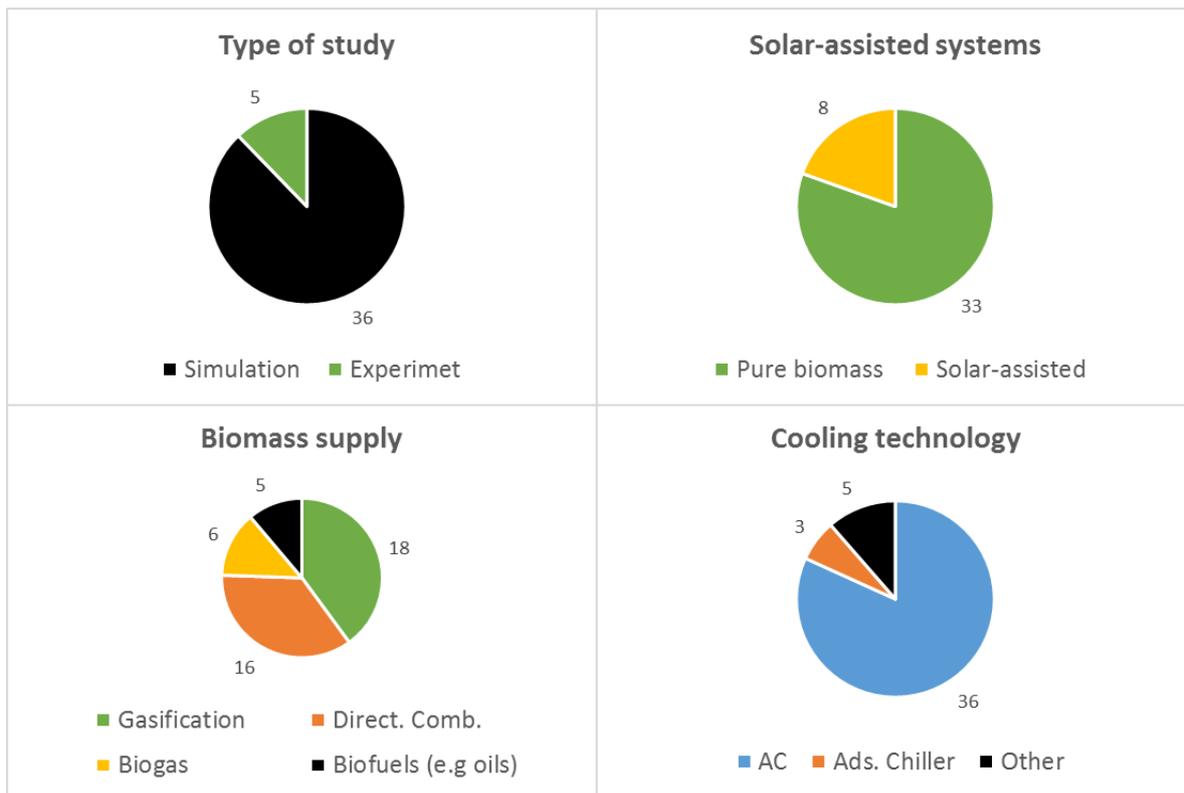


Figure 4 Meta-data results of the 41 different systems studied (multiple component application possible)

Payback time was chosen as the most convenient economic variable, but it is difficult to compare the economic viability of different systems based on this variable, because some studies include subsidies while some do not. It is remarkable that almost every model achieved economic viability, at least when subsidised. Together with the lack of studies on real-life, successful systems, this suggests a certain economic bias within the scientific community towards such renewable energy systems and their efficiencies (see also [149,150]). To promote small-scale biomass systems in rural and off-grid areas, where the benefits may be strongest, it is necessary to inform the population about the benefits and to educate the system owner and operators in technical training institutes [151].

Most case studies identify the prime mover as the most important unit of the CCHP system, because it has the biggest impact on energetic, ecologic and economic performance. Future research in the fields of SEs, FCs and micro turbines can lead to considerable competitiveness of these technologies compared to ICEs, while ORCs are already penetrating the market successfully [12,21,25,48]. Despite of the instability with bio- and syngas and the regular maintenance requirements of ICEs, until today they still seem to be the preferred choice for investors. But due to the external combustion SEs or Micro turbines can be used in combination with gasification for greater robustness [89,122]. Additionally, these technologies could surpass the performance of ICE driven systems and can lead to small-scale CCHP systems with even higher ecologic and economic benefits. However, other technologies concerning heat exchangers, cooling units, gasifiers or digesters will also develop further due to new materials and better simulation programs [18,152–155].

This study concentrated on systems which produce electricity, heating and cooling, but there are several polygeneration systems which produce other energy products like biofuels (e.g. hydrogen, methane), chemicals for production processes, purified water or food [156,157]. These technologies offer a huge variety of different system configurations for more efficient, more flexible and more environmentally friendly biomass usage, but they also increase the complexity of such systems. While some studies explicitly concentrate on storage possibilities, especially for off-grid systems, other studies completely ignore the possible benefits of storing electric and/or thermal energy. Nonetheless, on-

going advances in fields like phase-change materials or solid-state batteries will enter the energy market and increase the economic feasibility of small-scale CCHP systems, especially for off-grid systems and for solar-assisted systems [138,158–160]. For grid-connected systems data optimization, which will enable better synchronization of various interconnected CCHP systems, and load shifting techniques will improve their energetic and economic efficiency [138,161,162]. Other promising technologies emerging on the market are carbon capture and storage (CCS), where the CO<sub>2</sub> is stored away, and carbon capture and utilisation (CCU), where the CO<sub>2</sub> is used for chemical products. CCS and CCU can push the carbon balance of biomass-fired CCHP systems into negative areas [5,163].

Overall, the CCHP market is currently experiencing enormous growth and several technologies are competing with each other while also opening up new possibilities [14,21]. The same can be said for the research in various subfields; several technologies now passed the experimental stage and can be applied and investigated in CCHP systems, while unripe technologies will enter this stage soon. Hence, the amount of studies in this field is growing rapidly [25].

## 7 Conclusion

In this study, the most important components for biomass-fired, small-scale CCHP systems have been presented and described according to their most current development. Furthermore, for each prime mover, the most recent case studies and their key characteristics have been presented. The results of these findings have been discussed and put into the context of current and future technology development.

Although the field of small-scale biomass-fired and biomass-fired solar-assisted CCHP systems gains rising interest in the scientific community, most studies are based on simulation models instead of experimental data. This leads to a gap between theoretical and practical feasibility of such systems. Models often show very cost-effective and feasible systems, but investors seem to be reluctant due to the uncertainty involved. This suggests an economic bias within the scientific field towards such systems. Future policy implementations should therefore consider the need for extra maintenance in combination with the increased complexity of such systems. Flexible and fast responding systems should be promoted. Especially regions with high energy prices, like islands or off-grid, rural areas, should be targeted for financial support. However, also in regions with good electric infrastructure, these small systems may help with the goal of decentralization and lead to higher energy resilience of communities and individuals. Research and finance projects should not just monitor the design and construction of such systems, but also observe long-term technical and socio-economic effects.

Additionally, it was found, that many studies consider ICEs and ORCs as prime mover, but only few investigate the possibilities of other upcoming prime mover technologies like SEs, FCs or micro turbines. Especially in the context of biomass gasification prime movers need to show robustness and fuel flexibility, which ICEs often lack. Therefore, the chances for other prime movers to gain greater shares in the market are very high. To accelerate this development, policy implementations should promote the use of alternative prime movers, especially in combination with innovative biomass pre-treatment technologies. Governments could finance such projects directly or give incentives to companies investing in such technologies through tax reductions or establishing knowledge transfer networks.

Moreover, stricter execution of already established policies like CO<sub>2</sub>-taxes may accelerate the transition towards renewable CCHP systems. Nonetheless, all of the systems investigated require a stable supply of raw biomass or processed biofuels. Policy implementations should therefore consider that a higher biomass consumption for such systems may endanger entire ecosystems and may lead to competition with areas for food production.

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