

## APPENDIX A

The advective mass transport occurs due to the groundwater movement and its real velocity is calculated from Darcy velocity and effective porosity as

$$V_i = \frac{u_i}{n_e} \quad (\text{A.1})$$

where  $V_i$  is the real velocity,  $u_i$  is the Darcy velocity and  $n_e$  is the effective porosity.

The advective mass transport in a small cube is considered (Figure A.1). If the change of volumetric concentration  $\Delta C_{\text{adv}}$  occurs in the small cube during an increment of time  $\Delta t$ , the stored mass inside of the small cube during the increment of time  $\Delta t$  is expressed as  $(\rho\theta\Delta C_{\text{adv}})\Delta x\Delta y\Delta z$ ,

$$(\rho\theta\Delta C_{\text{adv}})\Delta x\Delta y\Delta z = \Delta t \left\{ \frac{\partial(\rho\theta V_x c)}{\partial x} + \frac{\partial(\rho\theta V_y c)}{\partial y} + \frac{\partial(\rho\theta V_z c)}{\partial z} \right\} \Delta x\Delta y\Delta z \quad (\text{A.2})$$

where  $\rho$  is the fluid density,  $\theta$  is the volume water content and  $c$  is the volumetric concentration.

Dividing both side of Eq. (A.1) by  $\Delta x\Delta y\Delta z$  and considering  $\Delta t \rightarrow 0$  and  $\Delta x, \Delta y, \Delta z \rightarrow 0$ , the following equation is obtained.

$$\frac{\partial(\rho\theta C_{\text{adv}})}{\partial t} = \frac{\partial}{\partial x_i}(\rho\theta V_i c) \quad (i=1, 2, 3) \quad (\text{A.3})$$

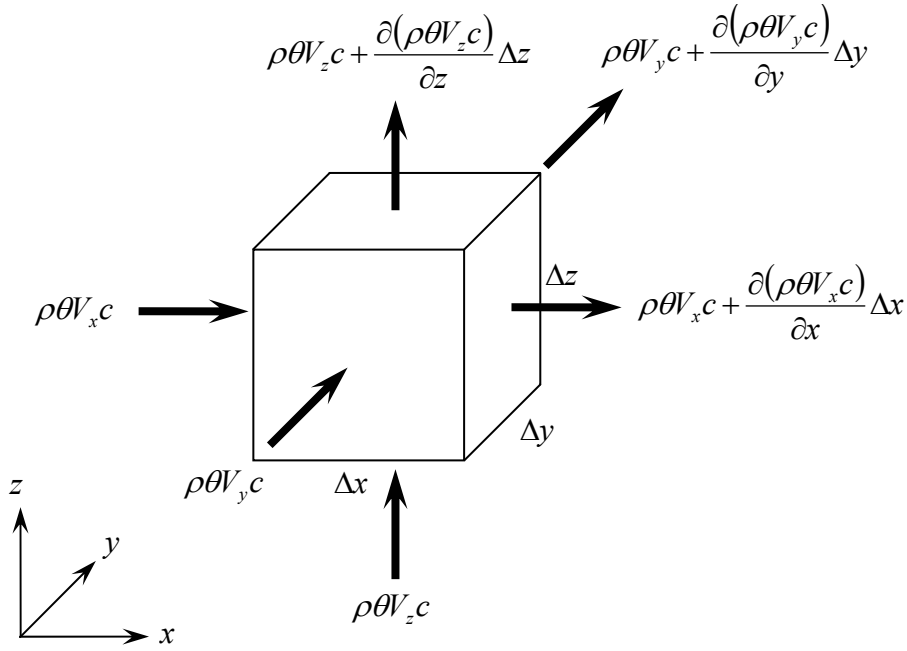


Figure A.1. The mass balance in a small cube due to advective mass transport.

The dispersive mass transport in the small cubic volume is also considered in the same way (Figure A.2).

$$\begin{aligned}
 & (\rho\theta\Delta C_{\text{dis}})\Delta x\Delta y\Delta z \\
 & = \Delta t \left\{ \frac{\partial}{\partial x} \left( \rho\theta D_x \frac{\partial c}{\partial x} \right) + \frac{\partial}{\partial y} \left( \rho\theta D_y \frac{\partial c}{\partial y} \right) + \frac{\partial}{\partial z} \left( \rho\theta D_z \frac{\partial c}{\partial z} \right) \right\} \Delta x\Delta y\Delta z \quad (\text{A.4})
 \end{aligned}$$

where  $D$  is the dispersivity tensor.

If the change of volumetric concentration  $\Delta C_{\text{dis}}$  occurs in the small cube during the increment of time  $\Delta t$ , the stored mass inside of the small cube during the time  $\Delta t$  is expressed as  $(\rho\theta\Delta C_{\text{dis}})\Delta x\Delta y\Delta z$ .

Dividing both side of Eq. (A.4) by  $\Delta x\Delta y\Delta z$  and considering  $\Delta t \rightarrow 0$  and  $\Delta x, \Delta y, \Delta z \rightarrow 0$ , the following equation is obtained.

$$\frac{\partial(\rho\theta\Delta C_{\text{dis}})}{\partial t} = \frac{\partial}{\partial x_i} \left( \rho\theta D_i \frac{\partial c}{\partial x_i} \right) \quad (i=1, 2, 3) \quad (\text{A.5})$$

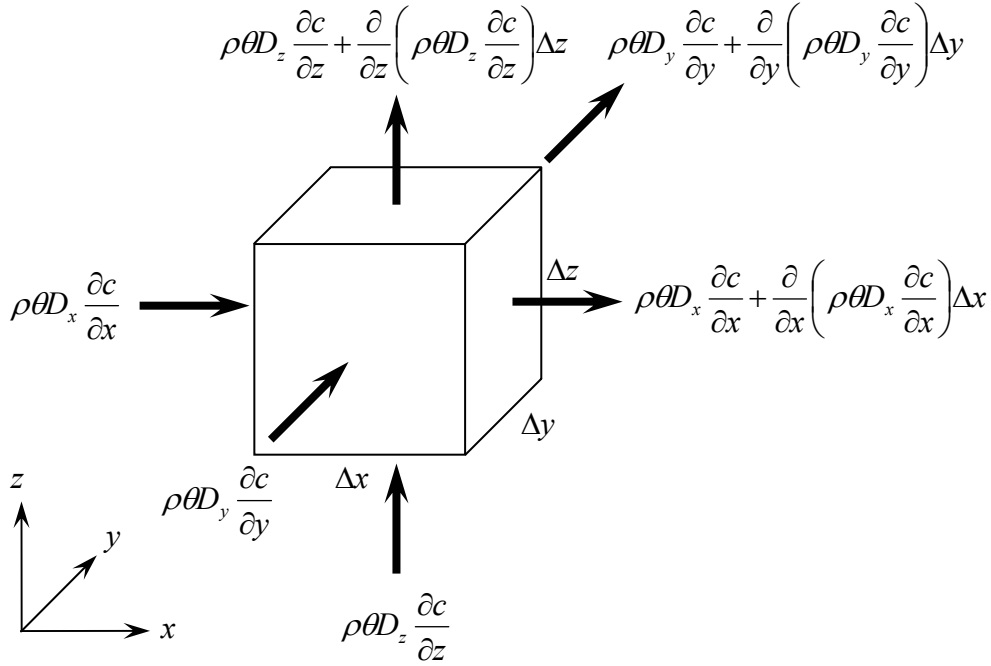


Figure A.2. The mass valance in a small cube due to dispersive mass transport.

Combining Eqs. (A.3) and (A.5), the general form of the advection-dispersion equation can be obtained as follows,

$$\frac{\partial(\rho\theta c)}{\partial t} = \frac{\partial}{\partial x_i} \left( \rho\theta D_{ij} \frac{\partial c}{\partial x_j} \right) - \frac{\partial}{\partial x_i} (\rho\theta V_i c) + Q_c \quad (\text{A.6})$$

where  $\theta$  is volume water content,  $\rho$  is fluid density,  $D_{ij}$  is dispersivity tensor,  $c$  is volumetric concentration,  $V_i$  is real velocity and  $Q_c$  is source/sink term.

Here the left hand side of Eq. (A.6) is

$$\frac{\partial(\rho\theta c)}{\partial t} = c \frac{\partial(\rho\theta)}{\partial t} + \rho\theta \frac{\partial c}{\partial t} \quad (\text{A.7})$$

and the second term of right hand side of Eq. (A.6) becomes

$$-\frac{\partial}{\partial x_i} (\rho\theta V_i c) = - \left( c \frac{\partial}{\partial x_i} (\rho\theta V_i) + \rho\theta V_i \frac{\partial c}{\partial x_i} \right) \quad (\text{A.8})$$

Substituting Eqs. (A.7) and (A.8) into Eq. (A.6), the following equation is obtained

$$c \frac{\partial(\rho\theta)}{\partial t} + \rho\theta \frac{\partial c}{\partial t} = \frac{\partial}{\partial x_i} \left( \rho\theta D_{ij} \frac{\partial c}{\partial x_j} \right) - \left( c \frac{\partial}{\partial x_i} (\rho\theta V_i) + \rho\theta V \frac{\partial c}{\partial x_i} \right) + Q_c \quad (\text{A.9})$$

On the other hand, the continuity equation is expressed as

$$\frac{\partial(\rho\theta)}{\partial t} = - \frac{\partial(\rho\theta V_i)}{\partial x_i} \quad (\text{A.10})$$

Introducing Eq. (A.10) in Eq. (A.9), the latter becomes

$$\rho\theta \frac{\partial c}{\partial t} = \frac{\partial}{\partial x_i} \left( \rho\theta D_{ij} \frac{\partial c}{\partial x_j} \right) - \rho\theta V \frac{\partial c}{\partial x_i} + Q_c \quad (\text{A.11})$$

If retardation effect and decay are considered, Eq. (A.11) becomes as follows using retardation coefficient  $R$  and decay rate  $\lambda$ ,

$$R\rho\theta \frac{\partial c}{\partial t} = \frac{\partial}{\partial x_i} \left( \rho\theta D_{ij} \frac{\partial c}{\partial x_j} \right) - \rho\theta V \frac{\partial c}{\partial x_i} - R\rho\theta\lambda c + Q_c \quad (\text{A.12})$$

Introducing the following Lagrangian description in Eq. (A.12),

$$\frac{d}{dt} = \frac{\partial}{\partial t} + \frac{V_i}{R} \frac{\partial}{\partial x_i} \quad (\text{A.13})$$

it becomes,

$$R\rho\theta \left( \frac{dc}{dt} - \frac{V_i}{R} \frac{\partial c}{\partial x_i} \right) = \frac{\partial}{\partial x_i} \left( \rho\theta D_{ij} \frac{\partial c}{\partial x_j} \right) - \rho\theta V \frac{\partial c}{\partial x_i} - R\rho\theta\lambda c + Q_c \quad (\text{A.14})$$

Since the second terms in both sides are the same, Eq. (A.14) becomes

$$R\rho\theta \frac{dc}{dt} = \frac{\partial}{\partial x_i} \left( \rho\theta D_{ij} \frac{\partial c}{\partial x_j} \right) - R\rho\theta\lambda c + Q_c \quad (\text{A.15})$$

Now it is assumed that the volumetric concentration  $c$  can be divided into two parts related to advection  $\bar{c}$  and dispersion  $\tilde{c}$  as follows.

$$c(x_i, t) = \bar{c}(x_i, t) + \tilde{c}(x_i, t) \quad (\text{A.16})$$

Substituting Eq. (A.16) into Eq. (A.17), the following equation is obtained,

$$R\rho\theta \frac{d(\bar{c} + \tilde{c})}{dt} = \frac{\partial}{\partial x_i} \left( \rho\theta D_{ij} \frac{\partial c}{\partial x_j} \right) - R\rho\theta\lambda(\bar{c} + \tilde{c}) + Q_c \quad (\text{A.17})$$

or

$$R\rho\theta \frac{d\bar{c}}{dt} + R\rho\theta \frac{d\tilde{c}}{dt} = \frac{\partial}{\partial x_i} \left( \rho\theta D_{ij} \frac{\partial c}{\partial x_j} \right) - R\rho\theta\lambda\bar{c} - R\rho\theta\lambda\tilde{c} + Q_c \quad (\text{A.18})$$

If the advective transport is focused on, the following governing equation can be obtained,

$$\frac{d\bar{c}}{dt} = -\lambda\bar{c} \quad (\text{A.19})$$

On the other hand, the governing equation for dispersive transport can be obtained by subtracting advection part from Eq. (A.18)

$$R\rho\theta \left( \frac{dc}{dt} - \frac{d\bar{c}}{dt} \right) = \frac{\partial}{\partial x_i} \left( \rho\theta D_{ij} \frac{\partial c}{\partial x_j} \right) - R\rho\theta\lambda(c - \bar{c}) + Q_c \quad (\text{A.20})$$

or

$$R\rho\theta \frac{d\tilde{c}}{dt} = \frac{\partial}{\partial x_i} \left( \rho\theta D_{ij} \frac{\partial(\bar{c} + \tilde{c})}{\partial x_j} \right) - R\rho\theta\lambda\tilde{c} + Q_c \quad (\text{A.21})$$

Eqs. (A.19) and (A.20) are two independent problems that can be solved separately.